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# **Nitrous Oxide (N<sub>2</sub>O) Transfer Velocity and the Effect of Ammonium on N<sub>2</sub>O fluxes from an Agricultural Drain**

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A thesis  
submitted in partial fulfilment  
of the requirements for the Master of Science Degree of  
Agriculture and Life Sciences

at  
Lincoln University  
by  
Manjula Premaratne

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Lincoln University  
2016

To

Retired Associate Professor Rob Sherlock

who taught me how to solve the problems analytically

Abstract of a thesis submitted in partial fulfilment of the  
requirements for the Master of Science Degree of Agriculture and Life Sciences

Nitrous Oxide ( $\text{N}_2\text{O}$ ) Transfer Velocity and the Effect of Ammonium on  $\text{N}_2\text{O}$   
fluxes from an Agricultural Drain

by

Manjula Premaratne

Indirect nitrous oxide ( $\text{N}_2\text{O}$ ) emissions from rivers and drains are poorly quantified and the uncertainty surrounding the emission factor for dissolved  $\text{N}_2\text{O}$  in rivers (EF5-r) is high. Scaling the exchange of  $\text{N}_2\text{O}$  across the water – air interface is important in order to estimate the indirect  $\text{N}_2\text{O}$  emissions from rivers and drains. Therefore, this study was designed to measure the drain water  $\text{N}_2\text{O}$  emission transfer velocity ( $k_{\text{N}_2\text{O}}$ ) and the effect of ammonium ( $\text{NH}_4^+$ ) on drain water  $\text{N}_2\text{O}$  yield. The field experiment released  $^{15}\text{N}\text{-NH}_4^+$ , with Bromide ( $\text{Br}^-$ ) as a conservative tracer, Rhodamine<sup>WT</sup> as a visual tracer, and propane ( $\text{C}_3\text{H}_8$ ) as a conservative tracer gas, into a drain. Visual tracer and conservative tracers allowed the drain water velocity and dilution factor to be determined, respectively. The  $\text{C}_3\text{H}_8$  and  $\text{N}_2\text{O}$  gases were collected using headspace equilibrium and floating chamber methods. The rate of  $\text{C}_3\text{H}_8$  escape from water to air was used to measure the  $\text{N}_2\text{O}$  transfer velocity ( $k_{\text{N}_2\text{O}}$ ). The gas transfer velocity model which as explained by O'Connor and Dobbins (1958), equation 2.9 as interpreted by Wilcock (1982) was also used to measure  $k_{\text{N}_2\text{O}}$ . The  $^{15}\text{N}_2\text{O}$  fluxes allowed the  $\text{NH}_4^+$  contribution to the  $\text{N}_2\text{O}$  flux to be determined. The  $^{15}\text{N}$  enrichment in biofilms and aquatic plants also allowed nitrogen assimilation to be evaluated.

The measured  $k_{\text{N}_2\text{O}}$  using headspace equilibrium and the  $k_{\text{N}_2\text{O}}$  estimated from Wilcock (1982) were  $7.49 \pm 0.72 \text{ m day}^{-1}$  and  $8.65 \pm 1.23 \text{ m day}^{-1}$ , respectively. To measure the hydro physical variations in  $k_{\text{N}_2\text{O}}$ , the current study data and the data from other New Zealand studies were evaluated. The results showed that for shallow drains, water depth  $< 1 \text{ m}$ , the value of  $k_{\text{N}_2\text{O}}$  increased with decreasing water depth.

There was an inverse relationship between  $^{15}\text{N}\text{-NH}_4^+\text{-N}$  enrichment and the  $^{15}\text{N}$  enrichment of the  $\text{N}_2\text{O}$  evolved. However, there was no relationship between  $^{15}\text{N}\text{-NO}_3^-$  enrichment with  $^{15}\text{N}\text{-N}_2\text{O}$  enrichment indicating  $\text{N}_2\text{O}$  was produced due to nitrification of added  $\text{NH}_4^+\text{-N}$ . Following  $^{15}\text{N}$  tracer

addition, biotic components of the drain ecosystem were highly enriched but returned to near background levels after 10 days, demonstrating that  $\text{NH}_4^+$ -N assimilation and mineralization occurred.

The calculated EF5-r values were significantly lower than the IPCC default EF5-r value; 0.0025 kg (2.5 g)  $\text{N}_2\text{O}$ -N per kg  $\text{NO}_3^-$ -N. The measured EF5-r values, derived using the surface  $\text{C}_3\text{H}_8$  flux measurements and the headspace  $\text{C}_3\text{H}_8$  equilibrium concentrations, were  $7.66\text{E-}6$  (7.66 mg) and  $8.20\text{E-}6$  (8.20 mg) kg  $\text{N}_2\text{O}$ -N per kg  $\text{NO}_3^-$ -N, respectively. However, the EF5-r values derived using floating chambers were significantly lower ( $3.92\text{E-}11$  kg; (0.0004 mg)  $\text{N}_2\text{O}$ -N per kg  $\text{NO}_3^-$ -N) and showed chamber methodology as an inefficient technique for gas flux measurements on flowing water surfaces. In contrast, the  $k_{\text{N}_2\text{O}}$  measured using the Wilcock (1982) model, that used drain water speed and depth produced higher EF5-r;  $9.48\text{E-}6$  kg (9.48 mg)  $\text{N}_2\text{O}$ -N per kg  $\text{NO}_3^-$ -N.

Thus, this study demonstrated; (1) the tracer gas addition technique is a reliable and accurate method for  $\text{N}_2\text{O}$  flux determinations from drains, (2) in shallow drains (water depth < 1 m) the  $k_{\text{N}_2\text{O}}$  value was inversely correlated with the water depths, (3) the added  $^{15}\text{N}$  tracer permitted the role of  $\text{NH}_4^+$  in  $\text{N}_2\text{O}$  production to be assessed and (4) the IPCC EF5-r default value overestimated  $\text{N}_2\text{O}$  emissions from agricultural drains.

**Keywords:** Nitrogen (N), Nitrous oxide ( $\text{N}_2\text{O}$ ),  $\text{N}_2\text{O}$  flux, ammonium ( $\text{NH}_4^+$ ), Nitrate ( $\text{NO}_3^-$ ), propane ( $\text{C}_3\text{H}_8$ ), Bromide ( $\text{Br}^-$ ) Rhodamine<sup>WT</sup>,  $\text{N}_2\text{O}$  transfer velocity ( $k_{\text{N}_2\text{O}}$ ),  $^{15}\text{N}$  enrichment, EF5-r, Headspace equilibrium and Floating Chambers.

## Acknowledgements

First of all I express my gratitude to my supervisor, Professor Tim Clough for his guidance, support, and encouragement throughout my study period and reading drafts and providing valuable comments that improved the content of the thesis enormously.

Next, I would like to thank my associate supervisor, Professor Frank Kelliher for helping me to understand the kinetic principles of the gas transfer between water and air and giving valuable comments to improve the thesis content.

Many thanks to my colleagues Teresa Symon, Rebecca D'Souza, Shiv Prasad Pokhrel, Barry Anderson, Neil Smith, Nigel Beale, Joy Jiao and Emily Huang who helped me with sampling, solution preparations, apparatus making and sample analysis. Without them, it was impossible to carry out all the tasks at once efficiently and effectively.

Special thanks to Jen Owens for providing much information about data analysis and collecting water samples. Sincerely thank Miriam Hodge and Jennifer Bufford for providing insight into how to find the effect of sampling time on data.

Many thanks to Analytical Service Manager Roger Cresswell for his support through out this study. I acknowledge and thank the Head of Soil Department, Associate Professor Peter Almond, Department Secretary, Amal Torky and Project Manager Gail Harkerss for their support for this study. Sincere thanks to Leanne Hassall and Lynne Clucas for supplying equipments and materials for the experiments.

To fellow students friends and colleagues at Soil Science Department, Soil Science Students Society and elsewhere thank you for your support, in many ways; Jason Breitmeyer, Roshean Woods, Amy Whitely, Dharini Paramachivam, Anna Carlton, Monica Giona Bucci, Veronica Penny, Tihana Vujanovic, Camilla Gardiner, Gustavo Boitt, Peter Carey, Obed Lense, Daniel Martin-Hendrie, Sally Seyedalikhani, Minakshi Mishra and Shamim Maumun.

Last, but not least, I thank my wife Aruni, daughter Malshi and son Jayavi for their support, encouragement and love.

# Table of Contents

<b>Abstract .....</b>	<b>iii</b>
<b>Acknowledgements .....</b>	<b>v</b>
<b>Table of Contents .....</b>	<b>vi</b>
<b>List of Tables .....</b>	<b>ix</b>
<b>List of Figures .....</b>	<b>x</b>
 <b>Chapter 1 Introduction .....</b>	 <b>1</b>
 <b>Chapter 2 Literature Review.....</b>	 <b>4</b>
2.1 Introduction .....	4
2.2 Determination of N <sub>2</sub> O exchange rates.....	4
2.3 Gas transfer rate measurements .....	6
2.3.1 Measurement methods .....	6
2.3.2 Tracer gases .....	6
2.3.3 Tracer gas injection methods.....	7
2.3.4 Tracer gas measurement methods .....	7
2.3.5 Gas Transfer measurement models.....	8
2.4 Indirect N <sub>2</sub> O emissions.....	11
2.4.1 Measurement methods .....	11
2.4.2 Nitrous oxide production and pathways.....	12
2.4.3 Nitrous oxide production in river systems .....	14
2.4.4 Nitrous oxide from leaching and runoff.....	15
2.4.5 EF5-g: N <sub>2</sub> O emissions from groundwater.....	17
2.4.6 EF5-r: N <sub>2</sub> O emissions from rivers .....	17
2.4.7 Conditions affecting N <sub>2</sub> O emissions .....	19
2.4.8 EF5-r measurements in New Zealand .....	20
 <b>Chapter 3 Measuring the nitrous oxide transfer velocity (<math>k_{N2O}</math>) in an agricultural drain .....</b>	 <b>22</b>
3.1 Introduction .....	22
3.2 Method .....	22
3.2.1 Field site .....	22
3.2.2 Hydrological and geophysical measurements .....	23
3.2.3 Mixed tracer solution .....	24
3.2.4 Sampling time, stations and collection .....	25
3.2.5 Dissolved propane measurements .....	27
3.2.6 Floating chamber gas collection and measurements .....	27
3.2.7 Gas analysis .....	28
3.2.8 Dissolved gas concentrations and gas transfer rate calculations .....	29
3.2.9 Statistical analysis .....	32
3.3 Results.....	33
3.3.1 Micro-metrological conditions.....	33
3.3.2 Drain water hydro physical measurements .....	33
3.3.3 Drain water Bromide (Br <sup>-</sup> ) measurements.....	34
3.3.4 Drain water steady state measurements – correction from Br <sup>-</sup> concentration.....	36
3.3.5 Drain water velocity .....	37

3.3.6	Nitrous oxide transfer velocity ( $k_{N_2O}$ ) measurement using propane ( $C_3H_8$ ) as a tracer gas .....	38
3.3.7	Nitrous oxide transfer velocity ( $k_{N_2O}$ ) measurement using the Wilcock (1982) transfer velocity model .....	41
3.3.8	Direct $k_{N_2O}$ measurement from floating chambers .....	42
3.3.9	Comparisons of $N_2O$ transfer velocity ( $k_{N_2O}$ ) estimations .....	43
<b>Chapter 4 Nitrous Oxide Transfer Velocity (<math>k_{N_2O}</math>) .....</b>		<b>45</b>
4.1	Evaluation of methods used to establish $k_{N_2O}$ .....	45
4.2	Gas transfer velocity in small rivers .....	49
4.3	Summary and suggestion for future research .....	50
<b>Chapter 5 Effect of Ammonium (<math>NH_4^+-N</math>) on <math>N_2O</math> emissions from an agricultural drain .....</b>		<b>51</b>
5.1	Introduction .....	51
5.2	Methods .....	52
5.2.1	Mixed tracer solution .....	52
5.2.2	Sampling time, stations and collection .....	52
5.2.3	Dissolved $N_2O$ measurements .....	53
5.2.4	Gas sample analyses on GC and TGII-IRMS .....	54
5.2.5	Dissolved $N_2O$ and $N_2O$ flux calculation .....	54
5.2.6	Inorganic $-N$ analysis .....	54
5.2.7	Plants, biofilms and sediments .....	55
5.2.8	Plants, biofilms, sediments and diffusions analysis in EA-CF IRMS .....	56
5.2.9	Inorganic- $N$ $^{15}N$ enrichment .....	57
5.2.10	$^{15}N$ enrichment and recovery calculations .....	58
5.2.11	Statistical analysis .....	58
5.3	Results .....	60
5.3.1	Dissolved oxygen (DO) and water temperature .....	60
5.3.2	Drain water pH and electrical conductivity .....	61
5.3.3	Distribution of $NH_4^+-N$ .....	62
5.3.4	Half-life of $NH_4^+-N$ .....	63
5.3.5	$^{15}N-NH_4^+$ atom percentage .....	64
5.3.6	$NH_4^+-N$ concentration versus $^{15}N-NH_4^+$ atom % .....	65
5.3.7	$^{15}N-NH_4^+$ recovery .....	66
5.3.8	Distribution of $NO_3^--N$ .....	67
5.3.9	$NH_4^+-N$ concentration versus $NO_3^--N$ concentration .....	68
5.3.10	Doubling time of $NO_3^--N$ .....	69
5.3.11	$^{15}N-NO_3^-$ atom percentage .....	70
5.3.12	$NO_3^--N$ concentration versus $^{15}N-NO_3^-$ atom % .....	71
5.3.13	$^{15}N-NO_3^-$ recovery .....	72
5.3.14	Distribution of $N_2O-N$ .....	73
5.3.15	Effect of DO, pH and temperature on $N_2O$ production .....	74
5.3.16	Inorganic- $N$ ( $NH_4^+-N$ & $NO_3^--N$ ) versus $N_2O$ production .....	75
5.3.17	$^{15}N-N_2O$ atom % .....	76
5.3.18	$NH_4^+-N$ & $NO_3^--N$ atom % vs versus $N_2O$ atom % .....	77
5.3.19	$^{15}N-N_2O$ recovery .....	78
5.3.20	Relationships of $^{15}N$ recoveries between $^{15}N-NH_4^+$ & $^{15}N-NO_3^-$ and $^{15}N-N_2O$ .....	79
5.3.21	Surface $N_2O$ and $^{15}N-N_2O$ flux measurements .....	79
5.3.22	$^{15}N-N_2O$ atom% from floating chambers .....	80
5.3.23	$^{15}N-N_2O$ recovery from floating chambers .....	81
5.3.24	Nitrogen uptake by river components .....	81



<b>Chapter 6 Drain water N dynamics and EF5-r measurements .....</b>	<b>83</b>
6.1 $\text{NH}_4^+$ -N versus $\text{NO}_3^-$ -N as a source of $\text{N}_2\text{O}$ .....	83
6.2 $\text{N}_2\text{O}$ -N flux estimations.....	84
6.3    EF5-r estimations .....	85
6.3.1    EF5-r measurements using the estimated $\text{N}_2\text{O}$ -N fluxes and $\text{NO}_3^-$ -N flux.....	86
6.3.2    EF5-r measurements from $\text{N}_2\text{O}$ -N flux and dissolved $\text{NO}_3^-$ -N .....	87
6.3.3    Comparison of total $\text{N}_2\text{O}$ -N flux from EF5-r values .....	88
6.4    Summary and suggestions for future research.....	88
 <b>Appendix A Abbreviations .....</b>	 <b>89</b>
 <b>Appendix B Equations.....</b>	 <b>91</b>
<b>References .....</b>	<b>93</b>

## List of Tables

Table 2.1	Published gas transfer coefficient ( $k'$ ) values in small rivers and streams (< 100 m wide) are employed to estimate the N <sub>2</sub> O transfer-coefficient ( $k'_{N_2O}$ ) using equation 2.1. Adopted from Wanninkhof et al. (1990), Murphy (2003) and Alin et al. (2011)..	10
Table 2.2	Summary of EF5-r studies in New Zealand .....	21
Table 3.1	Experiment 1; the drain water chemistry and physical measurements. (Temperature and dissolved oxygen errors = $\pm$ standard deviations of three samples).....	33
Table 3.2	Experiment 2; the drain water chemistry and physical measurements. (Temperature and dissolved oxygen errors = $\pm$ standard deviations of three samples).....	34
Table 3.3	Headspace N <sub>2</sub> O transfer velocity ( $k_{N_2O}$ ) calculations from experiment 1 (20/01/2015) and experiment 2 (12/08/2015). .....	40
Table 3.4	Nitrous oxide transfer velocity ( $k_{N_2O}$ ) values derived from C <sub>3</sub> H <sub>8</sub> surface flux measurements.....	41
Table 3.5	N <sub>2</sub> O transfer velocity ( $k_{N_2O}$ ) determined using the model of Wilcock (1982) for data from experiment 1 (20/01/2015) and experiment 2 (12/08/2015). .....	42
Table 3.6	Nitrous oxide transfer velocity ( $k_{N_2O}$ ) values derived from floating chamber N <sub>2</sub> O surface flux measurements. ....	42
Table 3.7	Comparisons between experimentally observed $k_{N_2O}$ (m day <sup>-1</sup> ) using propane as a tracer gas at each site from headspace equilibrium (HS) and floating chamber (FC) methods, Wilcock (1982) model and N <sub>2</sub> O flux measurements. ....	43
Table 4.1	Comparisons between $k_{N_2O}$ obtained at each site (m day <sup>-1</sup> ) from equation 2.10 (multiplier 3.74), and the modified model (multiplier 2.70) measured $k_{N_2O}$ .....	47
Table 6.1	Nitrous oxide (N <sub>2</sub> O-N) flux estimations from the measured $k_{N_2O}$ using different methods.....	85
Table 6.2	EF5-r estimations from the calculated N <sub>2</sub> O-N flux using different $k_{N_2O}$ .....	86
Table 6.3	EF5-r estimations from the chamber N <sub>2</sub> O-N flux measurements at sites 1, 3 and 5. ..	87

## List of Figures

Figure 2-1	Schematic of the nitrification pathway showing $N_2O$ production as a result of ammonia oxidation which occurs under aerobic conditions (Wrage, 2001).....	12
Figure 2-2	Schematic diagram of the denitrification pathway showing $N_2O$ production as a result of nitrate respiration which occurs under anaerobic conditions (Wrage et al., 2001).....	13
Figure 2-3	Schematic of the nitrifier-denitrification pathway where $N_2O$ production occurs as a result of nitrate respiration by nitrifiers, when the oxygen status is declining but not totally anaerobic (Wrage, 2001).....	14
Figure 2-4	A model of $N_2O$ production in streams (modified from Mulholland et al., 2004) ( $k'$ = water to air $N_2O$ exchange rate, $K_n$ = $N_2O$ production rate from nitrification/denitrification and $K_u$ = assimilative N uptake and release rate).....	15
Figure 2-5	The relation between $N_2O$ flux and the stream order in south-eastern Minnesota (Turner et al., 2015).....	20
Figure 3-1	Rainey's Road drain .....	23
Figure 3-2	Topographical map showing measurement sites of the Rainey's road drain. Direction of the water flow is shown by the arrow. (Scale 1.0 cm: 0.25 Km) .....	26
Figure 3-3	Dissolved gas extractions by headspace method .....	27
Figure 3-4	Floating chamber headspace gas sampling .....	28
Figure 3-5	Experiment 1: Drain water $Br^-$ concentration over distance and sampling time following commencement of tracer solution injection at time zero. Error bars = stdev, (n = 4) of mean $Br^-$ concentrations over all sampling times.....	35
Figure 3-6	Experiment 2: Drain water $Br^-$ concentration over distance and sampling time following commencement of tracer solution injection at time zero. Error bars = Stdev, (n = 5) of mean $Br^-$ concentrations over all sampling times.....	35
Figure 3-7	Mean water velocity obtained from the slope of graph for both experiment 1 and 2. Travel time is determined using breakthrough concentrations of Rhodamine <sup>WT</sup> dye.....	37
Figure 3-8	Experiment 1, results of the natural log of $C_3H_8/Br^-$ over time. The data points are individual sample values. The area between the green lines represents the 95% confidence interval and the brown line is the best-fit line. The area between the purple lines represents the prediction interval, and the slope of the best-fit line is the propane transfer coefficient ( $k'_{C_3H_8}$ ).....	38
Figure 3-9	Experiment 2, results of the natural log of $C_3H_8/Br^-$ over time. The data points are individual sample values. The area between the green lines represents the 95% confidence interval and the brown line is the best-fit line. The area between the purple lines represents the prediction interval. The slope of the best-fit line is the propane transfer coefficient ( $k'_{C_3H_8}$ ).....	39
Figure 3-10	The interquartile box plot comparisons of experiment #1 $N_2O$ transfer velocity ( $k_{N_2O}$ ) determined using $C_3H_8$ as a tracer gas between HS (Headspace equilibrium) and Wilcock (1982) model. The box represents the interquartile range (25% to 75%) for each group, the middle line is median, the symbol is the mean value and the upper (> 75%) and lower (< 25%) whiskers are the outside values of interquartile range.....	44
Figure 3-11	The interquartile box plot comparisons of experiment #2 $N_2O$ transfer velocity ( $k_{N_2O}$ ) determined using $C_3H_8$ as a tracer gas between HS (Headspace equilibrium), Floating chambers (FC) and Wilcock (1982). The determined $k_{N_2O}$ from surface flux is based on $N_2O$ flux measured in chambers. The box represents the interquartile range (25% to 75%) for each group, the middle line is median, the symbol is the mean value of the group and the upper (> 75%) and lower whiskers (< 25%) are the outside values of the interquartile range. ....	44
Figure 4-1	The modified model predicted $k_{N_2O}$ ( $m\ day^{-1}$ ) in Rainey's Road sites depth (m).....	47
Figure 4-2	The modified model predicted $k_{N_2O}$ ( $m\ day^{-1}$ ) vs. sampling site depth (m) of Wilcock (1984), Young, and Huryn (1999) and Rainey's Road drain (2015). ....	48

Figure 5-1	A photo of biofilm and soil sediment. ....	55
Figure 5-2	A photo of aquatic plant species; (a) <i>Rununculus sp.</i> (b) Aquatic grass – <i>Carex sp.</i> (c) Duckweed – <i>Lemnoideae sp.</i> ....	56
Figure 5-3	Samples undergoing $^{15}\text{N}$ diffusion to determine inorganic-N $^{15}\text{N}$ enrichment.....	57
Figure 5-4	Change in (a) dissolved oxygen (DO) concentrations, (b) DO saturation and (c) water temperature over distance. Each data point denotes a single measurement at 10 cm depth (n = 15). ....	60
Figure 5-5	Change in water pH over distance. Data points are means, n= 9 (3 samples X 3 times) and error bars are $\pm$ Stdev. ....	61
Figure 5-6	Drain water EC over distance. Data points are means, n=9 (3 samples X 3 sampling times) and error bars are $\pm$ Stdev. ....	61
Figure 5-7	Drain water $\text{NH}_4^+$ -N concentration versus distance (a) and time (b). The best-fit exponential regression lines are black, the 95% confidence intervals are between blue lines and predicted intervals are between red lines. Each data point denotes a single sample measurement (n = 45). ....	62
Figure 5-8	Drain water $\text{NH}_4^+$ -N concentration versus time. The brown line is the best-fit exponential curve ( $r^2 = 1.0$ ). The brown line is the best-fit line ( $r^2 = 1$ ), the area between the green lines represents the 95% confidence interval and the area between purple lines represents the prediction interval.....	63
Figure 5-9	Drain water $^{15}\text{N}$ - $\text{NH}_4^+$ atom % versus distance (a) and time (b). The black line is the best-fit regression curve, 95% confidence intervals are between blue lines and predicted intervals are between red lines. Each data point denotes a single sample measurement (n = 42). ....	64
Figure 5-10	Drain water $\text{NH}_4^+$ -N concentration versus $^{15}\text{N}$ - $\text{NH}_4^+$ atom %. The black line is the best-fit regression curve, 95% confidence intervals are between blue lines and predicted intervals are between red lines. Each data point denotes a single sample measurement (n = 42). ....	65
Figure 5-11	Drain water $^{15}\text{N}$ - $\text{NH}_4^+$ recovery versus distance (a) and time (b). The black line is the best-fit regression curve, 95% confidence intervals are between blue lines and predicted intervals are between red lines. Each data point denotes a single sample measurement (n = 42). ....	66
Figure 5-12	Drain water $\text{NO}_3^-$ -N concentration versus distance (a) and time (b) and the net change of $\text{NO}_3^-$ -N concentrations ( $\text{dNO}_3^-$ -N) versus distance (c) and time (d). Black lines are the best-fit regression lines, the area between blue lines is 95% confidence interval and the area between red lines is predicted interval. Each data point denotes a single sample measurement (n = 45).....	67
Figure 5-13	The $1/\text{dNH}_4^+$ -N concentration versus the $\text{dNO}_3^-$ -N concentration (n = 45). The black line is the best-fit linear regression curve, the area between blue lines is 95% confidence intervals and the area between red lines is the predicted interval. Each data point denotes a single sample measurement (n = 42). ....	68
Figure 5-14	Drain water $\text{dNO}_3^-$ -N concentration versus time. The brown line is the best-fit exponential curve ( $r^2 = 1.0$ ). The brown line is the best-fit line ( $r^2 = 1$ ), the area between the green lines represents the 95% confidence interval and the area between purple lines represents the prediction interval.....	69
Figure 5-15	Drain water $^{15}\text{N}$ - $\text{NO}_3^-$ atom % versus distance (a) and time (b). The black lines are the best-fit linear regression lines, the area between blue lines is 95% confidence interval and the area between red lines is the predicted interval. Each data point denotes a single sample measurement (n = 42). ....	70
Figure 5-16	Drain water $^{15}\text{N}$ - $\text{NO}_3^-$ atom % versus $\text{NO}_3^-$ -N concentration. The black lines are the best-fit linear regression lines, the area between blue lines is 95% confidence interval and the area between red lines is the predicted interval. Each data point denotes a single sample measurement (n = 42). ....	71
Figure 5-17	Drain water $^{15}\text{N}$ - $\text{NO}_3^-$ recovery versus distance (a) and time (b). The black lines are the best-fit linear regression lines, the area between blue lines is 95% confidence	

	interval and the area between red lines is the predicted interval. Each data point denotes a single sample measurement (n = 42).....	72
Figure 5-18	Drain water N <sub>2</sub> O-N concentration versus distance (a) and time (b) and the net change of N <sub>2</sub> O-N concentrations (dN <sub>2</sub> O-N) versus distance (c) and time (d). The best-fit exponential regression lines are black, the area between blue lines is 95% confidence interval and the area between red lines is the predicted interval. Each data point denotes a single sample measurement (n = 39).....	73
Figure 5-19	Change in N <sub>2</sub> O-N concentrations versus (a) DO, (b) pH and (c) water temperature. The performed trend lines represent linear regressions (n = 45). ....	74
Figure 5-20	The drain water dN <sub>2</sub> O-N changes versus (a) NH <sub>4</sub> <sup>+</sup> -N concentration and (b) dNO <sub>3</sub> <sup>-</sup> -N concentrations. The trend lines are simple linear regressions (n = 45). ....	75
Figure 5-21	Drain water <sup>15</sup> N- N <sub>2</sub> O atom % versus distance (a) and time (b). The black line are the best-fit regression lines, the area between blue lines are 95% confidence interval and the area between red lines are predicted interval. Each data point denotes a single sample measurement (n = 39).....	76
Figure 5-22	The drain water <sup>15</sup> N-NH <sub>4</sub> <sup>+</sup> atom % versus <sup>15</sup> N-NO <sub>3</sub> <sup>-</sup> atom % (a) and <sup>15</sup> N-N <sub>2</sub> O atom % (b).....	77
Figure 5-23	The drain water <sup>15</sup> N-NO <sub>3</sub> <sup>-</sup> atom % versus <sup>15</sup> N-N <sub>2</sub> O atom %. ....	77
Figure 5-24	Drain water <sup>15</sup> N- N <sub>2</sub> O recovery versus distance (a) and time (b). The best-fit regression lines are black, the 95% confidence intervals are between blue lines and the predicted intervals are between red lines. Each data point denotes a single sample measurement (n= 39).....	78
Figure 5-25	Interaction of the drain water <sup>15</sup> N-NH <sub>4</sub> <sup>+</sup> recovery % with <sup>15</sup> N-NO <sub>3</sub> <sup>-</sup> (a) and <sup>15</sup> N-N <sub>2</sub> O recovery % (b); (n=39). ....	79
Figure 5-26	Hourly average N <sub>2</sub> O flux at three sample sites (15 m, 65 m and 215 m; n = 3, error bars = ± stdev).....	80
Figure 5-27	Average <sup>15</sup> N-N <sub>2</sub> O atom percentage at three sample sites (15 m, 65 m and 215 m; n = 3, error bars = ± stdev). ....	80
Figure 5-28	Average <sup>15</sup> N recovery as N <sub>2</sub> O at three sample sites (15 m, 65 m and 215 m; n = 3, error bars = ± stdev). ....	81
Figure 5-29	Temporal changes in δ <sup>15</sup> N vs air (prior to tracer solution addition, 24 hrs after and 10 days later) in drain components (Biofilms n = 5, soil sediments n = 5, Duckweed n = 5, Aquatic grass n = 4 and <i>Rununculus sp</i> , n = 2; Error bars = ± stdev). ....	82
Figure 5-30	Spatial variances of δ <sup>15</sup> N vs. air in drain components 24 hrs after tracer solution injection (n = 1). ....	82

# Chapter 1

## Introduction

As a consequence of nitrous oxide ( $\text{N}_2\text{O}$ ) being a greenhouse gas (IPCC, 2007) and impacting on stratospheric ozone depletion (Crutzen, 1981) it has received significant scientific attention. Nitrous oxide results from the microbial transformation of nitrogen (N) in soils, sediments or water bodies, (Wrage et al., 2001). When agricultural N inputs are out of balance with agroecosystem demands, the excess N may be lost. Ruminant cattle return 60 – 90% of their ingested N to the pasture as urine with loading rates of up to  $1200 \text{ kg N ha}^{-1}$  (Di & Cameron, 2002b). The pasture utilizes only a small proportion of this N and the remainder is at risk of being leached as nitrate ( $\text{NO}_3^-$ ) or lost via gaseous forms. The direct gaseous loss pathways occur at the site of N deposition and include gaseous fluxes such as dinitrogen ( $\text{N}_2$ ) and  $\text{N}_2\text{O}$ . The N leached from pasture soils can also, in turn, result in indirect emissions of  $\text{N}_2\text{O}$  from drains, rivers and estuaries.

New Zealand signed the Kyoto Protocol in 1998 under the auspices of the United Nations Framework Conventions on Climate change (UNFCCC). Therefore, New Zealand is legally obliged to provide annual inventories of its agricultural greenhouse gas (GHG) emissions, and must reduce its GHG emissions to 1990 levels or take responsibility for the excess emissions (Ward, 1998). Animal agriculture is responsible for 97% of the  $\text{N}_2\text{O}$  emissions in New Zealand (Ministry of Agriculture and Forestry, 2006). The established IPCC (Intergovernmental Panel on Climate Change) methodology provides default emission factors to calculate  $\text{N}_2\text{O}$  sources from anthropogenic N inputs to agroecosystems. The methodology also allows the use of country specific emission factors. In New Zealand, most of the research to date has focused on refining direct emission factors, not indirect emissions.

Fertilizers and animal excreta are the main sources of agricultural  $\text{N}_2\text{O}$  emissions, and they dominate global anthropogenic emissions accounting for  $4.1 \text{ Tg N}_2\text{O-N yr}^{-1}$  of a total  $6.1 \text{ Tg N}_2\text{O-N yr}^{-1}$  of direct emissions. Indirect emissions account for  $0.6 \text{ Tg N}_2\text{O-N yr}^{-1}$ , however, estimated indirect emissions are highly uncertain ( $0.02\text{--}1.20 \text{ Tg N}_2\text{O-N yr}^{-1}$ ). The revised 1996 IPCC guidelines stated that the indirect  $\text{N}_2\text{O}$  emissions accounted for 1/3 of the global agricultural  $\text{N}_2\text{O}$  sources with 2/3 of the total uncertainty (Mosier et al., 1998). Obtaining more accurate indirect  $\text{N}_2\text{O}$  emissions data, especially for emissions resulting from leaching and runoff remains a high priority.

The N leached through soil profiles may resurface in agricultural drains. The magnitude of indirect  $\text{N}_2\text{O}$  emissions from such N contaminated water bodies may differ with agricultural ecosystem type (cropping systems, pastoral farms etc.), and over spatial and temporal scales. However, current

indirect emission factors used in NZ for leaching and run off make no distinction based on catchment use or water-body class (e.g. drain, stream, or river). Under the IPCC's 2006 guidelines, the current default emission factor for riverine N<sub>2</sub>O production (EF5-r) has a value of 0.0025 kg N<sub>2</sub>O-N per kg of N leached. However, data reporting N<sub>2</sub>O emissions from agricultural drains and the N<sub>2</sub>O exchange rate from drain water to air are scarce.

The rate of N<sub>2</sub>O dissipation from water to air is an essential measurement for determining a loss of N<sub>2</sub>O from waterbodies. The exchange of dissolved gasses between water and air is governed by the relative partial pressure differences of both phases. The measurement of N<sub>2</sub>O concentrations in air and water are straightforward. However, determining the N<sub>2</sub>O transfer coefficient ( $k'$  –emissions per unit time) is neither simple nor direct. Water velocity, gradient, roughness of the bottom surface, water depth and the area of the waterway exposed to air, control the value of  $k'$ .

1. Thus, the first objective of this study was to measure the N<sub>2</sub>O transfer coefficient ( $k'$ ) from water to air in an agricultural drain using a tracer gas.

Propane (C<sub>3</sub>H<sub>8</sub>) was used as a tracer gas in this study. Both floating chambers and headspace equilibrium methods were employed to measure the C<sub>3</sub>H<sub>8</sub> emitted from the water surface and the dissolved C<sub>3</sub>H<sub>8</sub> concentrations, respectively. The slope of the log of C<sub>3</sub>H<sub>8</sub> concentration versus time was considered as the C<sub>3</sub>H<sub>8</sub> gas transfer coefficient ( $k'_{C_3H_8}$ , hr<sup>-1</sup> or day<sup>-1</sup>). This was then normalised to a value at 20°C using the Schmidt number of 600 ( $Sc_{600}$ ) and then used to estimate the N<sub>2</sub>O fluxes from the drain water surface (Jähne et al., 1987).

No previous research has examined the effect of NH<sub>4</sub><sup>+</sup> on N<sub>2</sub>O fluxes from drains. The N leached from farm lands into drains may be assimilated in aquatic plants and algae as organic matter. When the organic matter decomposes, biological N is released as ammonia (NH<sub>4</sub><sup>+</sup> or NH<sub>3</sub>). Such ammonia may also undergo nitrification resulting in N<sub>2</sub>O emissions. It is stated that 0.0025 kg N<sub>2</sub>O-N is emitted from drains per kg of N leached (IPCC, 2006).

2. Thus, the second objective of this study was to assess the N<sub>2</sub>O yield due to nitrification of ammonium (NH<sub>4</sub><sup>+</sup>). This was achieved by adding <sup>15</sup>N tracer (<sup>15</sup>NH<sub>4</sub><sup>+</sup>) into the drain and measuring the <sup>15</sup>N<sub>2</sub>O and <sup>15</sup>NO<sub>3</sub><sup>-</sup> produced over the drain's distance.

This experiment released a tracer solution into the drain that comprised of <sup>15</sup>N enriched ammonium ((<sup>15</sup>NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>), a conservative bromide (Br<sup>-</sup>) tracer, a visual tracer, Rhodamine<sup>WT</sup> (visual tracer) and a conservative gas tracer, C<sub>3</sub>H<sub>8</sub>. The Br<sup>-</sup> and Rhodamine<sup>WT</sup> tracers assisted to measure the water discharge rate and the drainage water velocity, respectively. The water samples and gas samples were collected along longitudinal transects of the drain and analysed for <sup>15</sup>NH<sub>4</sub><sup>+</sup>, <sup>15</sup>NO<sub>3</sub><sup>-</sup> and the

tracers. Gas samples were collected to measure  $^{15}\text{N}_2\text{O}$  and  $^{15}\text{N}_2$  every 15 minutes using both floating chambers and headspace equilibrium methods. The drain geophysical (temperature, width, depth and velocity) and chemical (pH and DO) parameters were also measured.

This thesis is structured into six chapters. The introductory chapter is presented here. Chapter two summarises the current state of knowledge on gas transfer rate measurements, indirect emissions, EF5-r estimates and N dynamics in flowing waters. Chapter three describes objective one, the field trials that were carried out to measure  $\text{N}_2\text{O}$  transfer velocity ( $k_{\text{N}_2\text{O}}$ ) from water to air. Chapter four addresses the measured  $k_{\text{N}_2\text{O}}$  measurements, comparison of methods used to establish  $k_{\text{N}_2\text{O}}$ . Chapter five explains  $\text{N}_2\text{O}$  yield due to  $\text{NH}_4^+$  addition. Chapter six concludes the thesis by summarising the findings with respect to  $\text{N}_2\text{O}$  yield and the effect of  $^{15}\text{N}$  tracer on  $\text{N}_2\text{O}$  emissions and EF5-r. In addition, the recommendations for future work are also discussed with the limitations and implications of the study.



## Chapter 2

### Literature Review

#### 2.1 Introduction

The purpose of this review was to evaluate and summarise literature related to the measurement of nitrous oxide ( $\text{N}_2\text{O}$ ) transfer velocity measurements ( $k_{\text{N}_2\text{O}}$ ) and  $\text{N}_2\text{O}$  production in surface waters, published  $\text{N}_2\text{O}$  yields and fluxes from river systems, with respect to the indirect emission factor (EF5-r).

Thus, this review covers:

- Procedures and methods to measure gas exchange rates
- Data used to determine the  $\text{N}_2\text{O}$  transfer rates and the effect of hydro-physical measurements on gas exchange
- Indirect  $\text{N}_2\text{O}$  emissions
- Nitrogen transformations and pathways
- IPCC guidelines for estimating the indirect emission factor EF5 (EF5-g, EF5-r & EF5-e)
- Nitrous oxide fluxes from flowing waters (rivers, streams and drains)

#### 2.2 Determination of $\text{N}_2\text{O}$ exchange rates

Nitrous oxide exchange at the water-air interface is central to  $\text{N}_2\text{O}$  flux measurements, in order to establish a credible N budget. Significant effort has gone into assessing carbon dioxide ( $\text{CO}_2$ ) and oxygen ( $\text{O}_2$ ) transfer rates from surface waters, but very few studies have measured  $\text{N}_2\text{O}$  transfer rates. The gas transfer rates from flowing waters depend on weather conditions (temperature and wind speeds that may vary seasonally) and hydro-physical conditions (exposed water surface area to water volume ratio, speed of water and gradient and roughness of the bottom surface).

Nitrous oxide is a sparingly soluble and a non-reactive gas, and the primary mechanism of gas removal from water is atmospheric exchange. The gas transfer rate from water to air is governed by two mechanisms, identified as advection and diffusion. Advection is a transport mechanism that carries dissolved substances within the water body as a result of fluid motion, which depends on the

surface water depth and roughness of the bottom surfaces of the water body (Zappa et al., 2007). Diffusion of gas from water to air depends on the solubility of the gas which is affected by water temperature and salinity as described by the Henry's Law function (Weiss, 1974).

In addition, wind also plays a role in determining the magnitude of the gas transfer rate from water to air (Wanninkhof, 1992). As reviewed by Alin et al. (2011), many studies have investigated the interaction between water and wind speed with respect to gas exchange rates in flowing waters. If drains are sheltered from wind, the main effect on gas exchange is likely to be water turbulence. However, in open and relatively still waters such as lakes and oceans, wind is the main factor governing gas exchange (Cole & Caraco, 1998).

The loss rates of added tracer gases have been used to determine the loss rates of CO<sub>2</sub> and O<sub>2</sub>. According to Graham's law the diffusion rate of gas is inversely proportional with its molar mass. Different gasses have different molecular diffusion coefficients; as a result, loss rates also differ. Thus, the rate of loss of a given gas can be related to the rate of loss of a second gas when it escapes into the atmosphere. The gas transfer rate from water to air is a first-order mechanism, thus the measurement of tracer gas loss rate allows the gas transfer rate of any gas to be determined using Schmidt number ratios (Jähne et al., 1987). The Schmidt number is a unitless ratio of the kinematic viscosity to the diffusion coefficient of the gas of interest which is sensitive to temperature. The gas loss rate is determined by plotting the log of the tracer gas concentration in the water body versus time. The slope of the graph is equivalent to the tracer gas transfer coefficient ( $k'_{Tracer\ gas}$ ).

The  $k'_{Tracer\ gas}$  can be employed to determine the N<sub>2</sub>O transfer coefficient ( $k'_{N2O}$ ) according to:

$$k'_{N2O} = k'_{Tracer\ gas} * (Sc_{N2O} / Sc_{Tracer\ gas})^{-n} \quad 2.1$$

where,  $Sc_{Tracer\ gas}$  and  $Sc_{N2O}$  are the Schmidt numbers for the tracer gas and N<sub>2</sub>O respectively, and n is the Schmidt number coefficient ( $\frac{1}{2}$  for rough bottom surfaces and  $\frac{3}{4}$  for smooth bottom surfaces of the water body concerned).

Assuming the water column is well mixed, the water to air N<sub>2</sub>O flux ( $F_{N2O}$ ) is determined according to:

$$F_{N2O} = h * k'_{N2O} (X_{aq} - X_g) \quad 2.2$$

where,  $F_{N2O}$  is the N<sub>2</sub>O flux from water to air (mol m<sup>-2</sup> hr<sup>-1</sup>), h is the depth of the water (m),  $k'$  is the N<sub>2</sub>O transfer coefficient (hr<sup>-1</sup>),  $X_{aq}$  is the N<sub>2</sub>O concentration in the aqueous phase (mol m<sup>-3</sup>) and  $X_g$  is the equilibrium N<sub>2</sub>O concentration in the aqueous phase (mol m<sup>-3</sup>) for a given atmospheric gas concentration and water temperature (Jähne et al., 1987; MacIntyre et al., 2001; Raymond et al., 2012).

The product of the water depth ( $h$ ) and  $N_2O$  transfer coefficient ( $k'_{N_2O}$ ) is defined as the  $N_2O$  transfer velocity ( $k_{N_2O}$ ) of the source water (Equation 2.3).

$$k_{N_2O} = h * k'_{N_2O} \quad 2.3$$

where,  $k_{N_2O}$  has units of distance per unit time ( $cm\ hr^{-1}$  or  $m\ day^{-1}$ ).

Substituting  $k_{N_2O}$  to 2.2, the  $N_2O$  flux from water to air can be written as:

$$F_{N_2O} = k_{N_2O} * (X_{aq} - X_g) \quad 2.4$$

Rearranging equation 2.4,  $k_{N_2O}$  can be estimated using a flux measured with floating chambers and by knowing the equilibrium gas concentration in waters using:

$$k_{N_2O} = F_{N_2O} / (X_{aq} - X_g) \quad 2.5$$

The diffusive  $N_2O$  fluxes from waters can either be measured directly or calculated from the dissolved equilibrium concentrations as per equation 2.4, if the  $N_2O$  transfer velocity ( $k_{N_2O}$ ) is known.

## 2.3 Gas transfer rate measurements

### 2.3.1 Measurement methods

To measure water-air gas exchange rates, two methods are generally considered: either a tracer gas addition method or a natural gas dissipation method. In the tracer gas addition method, non-reactive trace gases are purposely added to the water and the gas dissipation rates are calculated by measuring changes in the gas concentration over stream distance. In natural tracer studies, naturally available dissolved gasses are used to determine the water-air gas exchange rates.

### 2.3.2 Tracer gases

Gases used in tracer gas addition studies include propane, hexa-fluoro sulphide ( $SF_6$ ), methyl chloride ( $CHCl_3$ ) and krypton (Kr), in aquatic ecosystems such as, lakes (Cole & Caraco, 1998), oceans (Wanninkhof, 1992), estuaries (Clark et al., 1994) rivers (Caplow & Schlosser, 2004) and small streams (Wanninkhof et al., 1990); Melching and Flores (2007). Propane ( $C_3H_8$ ) has been previously validated as a least-affected gas in a range of water conditions and has been used in many air-water gas exchange studies (Boumansour & Vassel, 1998).

In natural gas dissipation measurement studies, dissolved gases such as oxygen (Hall et al., 2012; Melching & Flores, 2007), carbon dioxide (Borges et al., 2004), methane (Jones Jr & Mulholland, 1998) and  $N_2O$  (Lal & Patra, 1998) have been measured to estimate the air water gas transfer coefficients.

Previously,  $N_2O$  fluxes determined flowing water studies have generally used direct measurements and have not employed  $N_2O$  transfer coefficients for their calculations. However, three studies have used tracer gasses to determine  $N_2O$  transfer coefficients in rivers. Hemond and Duran (1989) applied di-chloro-methyl-fluorine (Freon-12) as a tracer to directly measure the  $N_2O$  transfer coefficient in an N enriched river. Harrison and Matson (2003) employed a pulse of dissolved hexa fluoro sulphide ( $SF_6$ ) as a volatile tracer to measure the patterns and controls on  $N_2O$  emissions from the Yaqui Valley agricultural drains of Sonora, Mexico. Wilcock and Sorrell (2008) used their previously derived methyl chloride ( $CHCl_3$ ) transfer coefficients data to measure  $N_2O$  emissions from three agricultural drains in the North Island, New Zealand.

### **2.3.3 Tracer gas injection methods**

Three tracer gas injection methods have been previously described; steady state injection (tracer gas injected as a continuous steady flow), single-slug gas injection and multi-slug gas injection (Hwa-Seong et al., 2012). The steady state injection method has been widely used and produced consistent results (Marzolf et al., 1994). However, steady injection requires significant resources in terms of consumables and labour (Hwa-Seong et al., 2012). The single slug injection is a simple method, but sample gas collections can be problematic with inconsistent results as a consequence. Multi-slug, the repeated injection of single slugs, uses less resource than the steady state injection method.

### **2.3.4 Tracer gas measurement methods**

Both the headspace equilibrium and the floating chamber techniques may be employed to measure the dissolved tracer gas equilibrium concentrations.

The headspace equilibrium method is a separation technique where dissolved gases are extracted from the liquid phase into a headspace volume. The dissolved gas concentrations ( $X_{aq}$ ) are determined following phase equilibrium at a known equilibrium temperature. Mackay et al. (1979) showed the dissolved concentration of a gas in water depends on the air-water gas distribution ratio which is approximated by the Henry's law constant ( $K_H$ ). The, Henry's law constant is defined according to:

$$K_H = P_{X(g)} / X_{(aq)} \quad 2.6$$

where,  $K_H$  is the Henry's law constant ( $\text{atm m}^3 \text{mol}^{-1}$ ) which is the ratio of  $P_{X(g)}$ , the partial pressure of the dissolved gas X in the gaseous phase, and  $X_{(aq)}$ , the molar concentration of gas X in the aqueous phase ( $\text{mol m}^{-3}$ ). The value of  $K_H$  is a function of both temperature and salinity (Wanninkhof, 1992).

Rearranging equation 2.4, the molar concentration of gas X in the aqueous phase can be estimated as,

$$X_{(aq)} = F_{(g)} / K_H \quad 2.7$$

In the floating chamber method, a chamber floats on the water and gas accumulates in the chamber headspace. The gas flux is determined by measuring the change in the headspace gas concentration over a known time per unit area. This is performed using a best-fit regression model of the gas concentration change over time (Hutchinson and Moiser, 1981; Stolk et al., 2009).

Rearranging equation 2.6, the molar concentration of gas  $X_{(aq)}$  in the aqueous phase can be estimated as,

$$X_{(aq)} = F / k \quad 2.8$$

where,  $X_{(aq)}$ , is the molar concentration of gas X in the aqueous phase ( $\text{mol m}^{-3}$ ),  $F$  is the gas flux measured in the chamber headspace ( $\text{mol m}^{-2} \text{hr}^{-1}$ ) and  $k$  is the gas transfer velocity ( $\text{m hr}^{-1}$ ).

### 2.3.5 Gas transfer measurement models

The predictive equations/models that are used for gas transfer coefficient estimations are mainly based on the hydrophysical characteristics of the rivers. Most of the models are mathematically complex requiring much more than general routine measurements and typically involve many assumptions. In addition, empirically derived gas transfer coefficient models are specific to the experimental river condition and are not appropriate for all waterways. An empirical model to measure the water turbulence velocity ( $k_{water}$ ) was introduced by O'Connor and Dobbins (1958) as follows.

$$k_{water} = (D * U / h)^{0.5} \quad 2.9$$

where,  $U$  is the river velocity ( $\text{m s}^{-1}$ ),  $h$  is the average river depth (m), and  $D$  is the diffusion coefficient in water ( $\text{m}^2 \text{s}^{-1}$ ) estimated by extrapolating data contained in Wise and Houghton (1968).

Equation 2.9 has been widely used to predict the gas transfer coefficient and laboratory derived data with isotropic water condition. O'Connor and Dobbins (1958) justified their model with river data. After a survey of New Zealand river aeration data and considering frequently cited predictive models, such as O'Connor and Dobbins (1958), Churchill et al., (1962), Owens et al., (1964), Langbein and Durum (1967), Isaacs and Guady (1968), Wilcock (1982) introduced a simple predictive equation for gas transfer coefficient determination. It was interpreted using equation (38) from O'Connor and Dobbins (1958) and adapted for the temperature range 10-30°C by Elmore and West (1961) as follows.

$$k = k_{(20)} * [1.0241]^{T-20} * 3.74 * [U^{0.5}/h^{1.5}] \quad 2.10$$

where,  $T$  is mean water temperature (°C),  $k_{(20)}$  is  $k$  when  $T$  is 20°C,  $U$  is water velocity ( $m\ s^{-1}$ ) and  $h$  is water depth (m). The equation has been used for reaeration measurements in streams and rivers by local government and other authorities for many years.

According to the established models, the gas transfer coefficient correlates with water velocity and inversely correlates with water depth. However, applying these models to measure the  $N_2O$  transfer coefficient in an agricultural drain could be biased due to drain characteristics, water quality and hydro-physical variations. Therefore, to understand the real time  $N_2O$  emissions from the study site, a tracer addition experiment is required.

Many studies have measured  $k'_{Tracer\ gas}$  (unit of  $time^{-1}$ ;  $s^{-1}$  or  $hr^{-1}$ ) in a wide range of rivers and streams. Employing equation 2.1,  $k_{N_2O}$  values were calculated from the published data for small rivers and streams (< 100 m wide) and are summarised in Table 2.1.

**Table 2.1** Published gas transfer coefficient ( $k'$ ) values in small rivers and streams (< 100 m wide) are employed to estimate the N<sub>2</sub>O transfer-coefficient ( $k'_{N_2O}$ ) using equation 2.1. Adopted from Wanninkhof et al. (1990), Murphy (2003) and Alin et al. (2011).

Location	Water type	Volatile tracer/Method	Reference	Discharge volume (L s <sup>-1</sup> )	Water Velocity (cm s <sup>-1</sup> )	Water depth (cm)	Transfer coefficient $k'$ at 20°C (hr <sup>-1</sup> ) for reference gas	Estimated N <sub>2</sub> O transfer co-efficient at 20°C (hr <sup>-1</sup> )
Lakes District, UK	Stream	Disturbed Equilibrium	Owens et al. (1964)	396 ± 196 (77-612)	29 ± 15 (4 - 55)	N/A	18.5 ± 10.5 (1.1 – 46.2)	NA
Jackson river St 7 – 8 North river	Stream	<sup>85</sup> Kr	Tsivoglou (1967)	620	13	69	2.4	2.08
	Stream	Ethylene			23	45	9.5	8.25
Bonner reach 1-2	Stream	Propane	Grant and Skavroneck (1980)	48	30	30	6.2	4.05
Waitoa, NZ	Stream	Methyl chloride	Wilcock, (1984)	700	19	40	16.4	15.5
Waipa, NZ	Small river	Methyl chloride	Wilcock, (1984)	36000	24	410	0.4	3.8
Waiotapu, NZ	Large stream	Methyl chloride	Wilcock (1984)	3500	38-40	79	7.7	7.31
					40-46	77	8.0	7.60
					33-46	70	3.9	3.70
Walker Branch, Tennessee, USA	1 <sup>st</sup> order stream	SF <sub>6</sub>	Wanninkhof et al. (1990)	20	6	10	NA	NA
Walker Branch, Tennessee, USA	1 <sup>st</sup> order stream	Propane	(Roberts, 2007)	5-57	NA	6-9	102 - 67	66.8–43.8
Grand Teton National Park, Wyoming	Stream	SF <sub>6</sub>	Hall & Tank, 2013	78 ± 74 (4-231)	18 ± 9 (5-33)	10 ± 4 (4-15)	81 -35.5 (41.4 – 135.2)	51.2 ± 22.4 (26.16 -85.4)
Amazon and Mekong rivers	Small rivers	Floating chambers	Alin et al. (2011)	9015 ± 13117 (70-38017)	39 ± 28 (5 - 100)	120 ± 90 (10 - 300)	10.9 ± 14.4 (1.4 - 60.2)	9.3 ± 12.3 (1.0 - 51.1)
River Lagan UK	Stream	<sup>85</sup> Kr	(Murphy, 2003)	28800	36	50	28.4	24.2

## 2.4 Indirect N<sub>2</sub>O emissions

### 2.4.1 Measurement methods

The loss of N from farmlands leads to a loss of soil fertility and potential productivity, but also poses a considerable threat to the environment (Cameron et al., 2013). New Zealand's pastoral agriculture has undergone rapid intensification since 1990 with increased stocking rates, N fertilizer usage, excreta N inputs and the use of imported N feed (Parfitt et al., 2012). Excess inputs of N followed by irrigation and rain events, may lead to large losses of N from agricultural lands (Riley et al., 2001). Accumulation of N in ground and surface waters increases eutrophication of streams, lakes and estuaries, and emissions of N<sub>2</sub>O from surface waters (Sutton et al., 2011).

The established IPCC (Intergovernmental Panel on Climate Change) methodology provides default emission factors to calculate N<sub>2</sub>O sources from anthropogenic N inputs to agro ecosystems under three categories: direct emissions from agricultural lands, animal waste systems and indirect (Wilcock, 1984) emissions that are associated with volatilized, leached or exported N from farmlands (Mosier, 1998). Many of these default emission factors have been updated and replaced with New Zealand specific factors. However, most of the research to date to refine these emission factors has been performed to assess direct emissions, not indirect emissions.

Globally, anthropogenic and natural sources are responsible for total N<sub>2</sub>O emissions of 17.9 Tg N<sub>2</sub>O-N yr<sup>-1</sup>, with a range of 8.1 – 30.7 Tg N<sub>2</sub>O-N yr<sup>-1</sup>, accumulating in the atmosphere at a rate of 3.6 Tg N<sub>2</sub>O-N yr<sup>-1</sup> (Ciais et al., 2013). The main anthropogenic sources for N<sub>2</sub>O emissions are synthetic N fertilizers and animal excreta which account for 4.1 Tg N<sub>2</sub>O-N yr<sup>-1</sup> of direct emissions. Indirect emissions partially result from N leaching and runoff from agricultural inputs of N and account for 0.9 Tg N<sub>2</sub>O-N yr<sup>-1</sup> with a high uncertainty (0.02 – 0.12 Tg N<sub>2</sub>O-N yr<sup>-1</sup>). Recent studies describe riverine N<sub>2</sub>O emissions as being the most uncertain in terms of magnitude, both spatially and temporally (Ivens et al., 2011).

According to past studies global indirect N<sub>2</sub>O emissions are as large as the direct emissions (Mosier et al., 1998). Seitzinger and Kroeze (1998) predicted N inputs to rivers would triple N<sub>2</sub>O production by 2050. Uncertainty surrounding indirect N sources and subsequent indirect N<sub>2</sub>O emissions is large and ranges over 1.5 orders of magnitude. This arises because there is a lack of understanding of the off-site N transport mechanisms and the ensuing N<sub>2</sub>O emissions (de Klein et al., 2001). Therefore, the quantification of the contribution of waterways to total annual N<sub>2</sub>O emissions is a high priority.



## 2.4.2 Nitrous oxide production and pathways

Nitrous oxide is produced in the natural environment by both biological and non-biological processes. However, the biological processes are responsible for more than 95% of global  $\text{N}_2\text{O}$  production (Muller and Sherlock, 2004; Cias et al., 2013). Nitrification and denitrification are the main biological processes responsible for  $\text{N}_2\text{O}$  production in soil environments (Beaulieu et al., 2010). In addition, heterotrophic nitrification and nitrifier-denitrification are also biological processes producing  $\text{N}_2\text{O}$  emissions. While these processes are relatively well characterised in terrestrial ecosystems, there is less known with respect to aquatic ecosystems (Beaulieu et al., 2011).

### 2.4.2.1 Nitrification

Nitrifying organisms conserve energy via the oxidation of inorganic N compounds such as ammonia ( $\text{NH}_3$ ) and derive carbon for growth from carbon dioxide ( $\text{CO}_2$ ). Nitrification is generally thought to be an aerobic two-step N oxidation process, where ammonia ( $\text{NH}_3$ ) is oxidised to nitrite ( $\text{NO}_2^-$ ) by ammonia oxidising bacteria and/or archaea and thereafter to nitrate ( $\text{NO}_3^-$ ) by nitrite oxidising bacteria (Delwiche, 1981). Both steps require several enzymes, and intermediates are formed (Figure 2.2). In the first step of nitrification, hydroxylamine ( $\text{NH}_2\text{OH}$ ) is produced as an intermediate product during  $\text{NH}_3$  to  $\text{NO}_2^-$  oxidation (Bremner, 1997). In the second step of nitrification,  $\text{NH}_2\text{OH}$  is oxidised to  $\text{NO}_2^-$  and  $\text{NO}_3^-$ . During both steps, nitrifying organisms release  $\text{N}_2\text{O}$  as a by-product. However, more recently, (Maartje et al., 2015) found two *Nitrospira* species that could encode all the enzymes for complete nitrification (comammox) and which performed both nitrification steps.

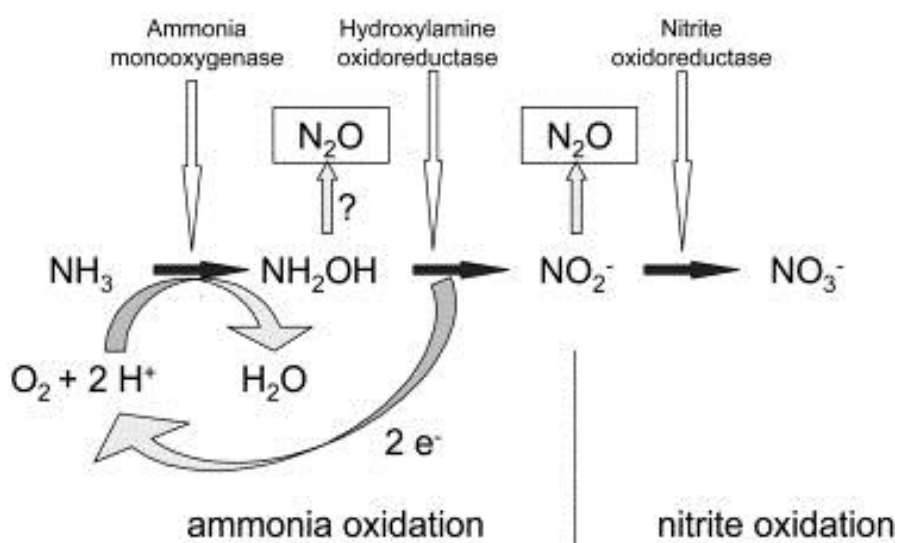


Figure 2-1 Schematic of the nitrification pathway showing  $\text{N}_2\text{O}$  production as a result of ammonia oxidation which occurs under aerobic conditions (Wrage, 2001).

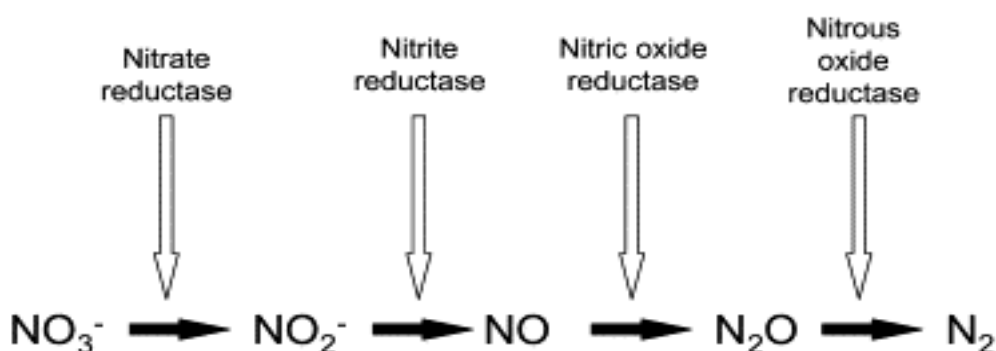
Nitrification may be a significant  $\text{N}_2\text{O}$  production mechanism in river waters where organic N mineralises, leading to  $\text{NH}_4^+$  production. There appear to be no studies that have examined the effect of  $\text{NH}_4^+$  on river  $\text{N}_2\text{O}$  emissions, and this process remains to be investigated (Beaulieu, 2010).

#### 2.4.2.2 Heterotrophic- nitrification

Nitrification is not limited to being an autotrophic process. In heterotrophic nitrification, organisms use carbon from organic matter for growth. Although the process of heterotrophic nitrification is similar to nitrification, different enzymes are responsible for  $\text{NH}_3$  oxidation to hydroxylamine, and then  $\text{NO}_2^-$  and  $\text{NO}_3^-$  (Wrage et al., 2001). Heterotrophic nitrification is considered a relatively minor  $\text{N}_2\text{O}$  production process when compared to autotrophic nitrification (Wrage et al., 2001). Low pH, high amounts of oxygen and availability of organic matter favour heterotrophic nitrification (Wrage et al., 2001). Beaulieu et al. (2015) doubted heterotrophic nitrification is dominant in well oxygenated waterways.

#### 2.4.2.3 Denitrification

Denitrification is an anaerobic process where  $\text{NO}_3^-$  is reduced to dinitrogen ( $\text{N}_2$ ) under anoxic conditions and  $\text{N}_2\text{O}$  is produced as an intermediate product (Wrage et al., 2001). During the denitrification process, the activity of the denitrification enzymes is repressed by  $\text{O}_2$  (Figure 2.3). As a result, an environment lower in  $\text{O}_2$  tends to increase the role of the denitrification process. Zhu et al. (2013) found that denitrification increased from 34% to 66% as the  $\text{O}_2$  concentration decreased from 21% to 0% in soil. Availability of carbon,  $\text{NO}_3^-$ , high pH and temperature are also recognized as factors influencing denitrification (Seitzinger et al., 2006).

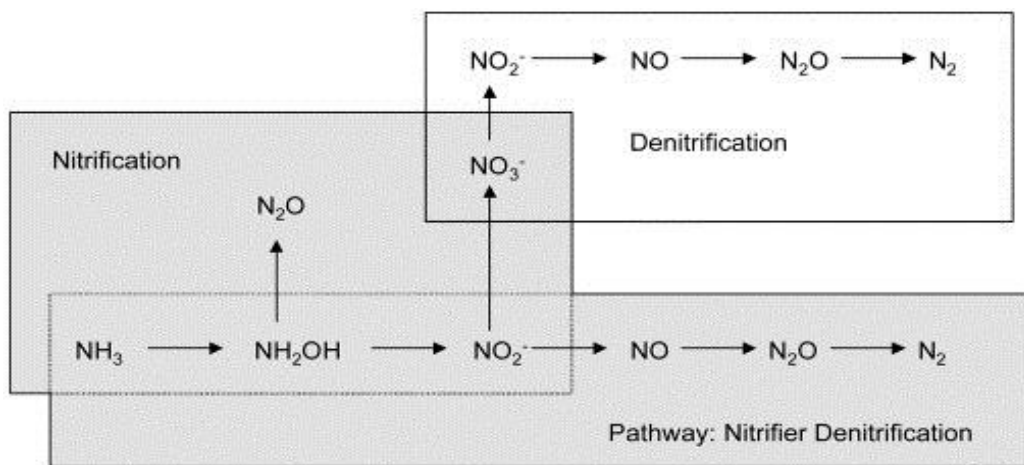


**Figure 2-2** Schematic diagram of the denitrification pathway showing  $\text{N}_2\text{O}$  production as a result of nitrate respiration which occurs under anaerobic conditions (Wrage et al., 2001).

#### 2.4.2.4 Denitrification

The nitrifier- denitrification process occurs when the  $O_2$  status declines in the environment but when it is not totally anaerobic (Wrage et al., 2001; Zhu et al., 2013). Webster and Hopkins (1996) revealed that nitrifier-denitrification was responsible for about 30% of  $N_2O$  emissions from soils.

Considering all of the  $N_2O$  emissions pathways, denitrification and  $NO_3^-$  have been recognized as the main process and the primary source for  $N_2O$  emissions in aquatic systems respectively (Baulch et al., 2011).



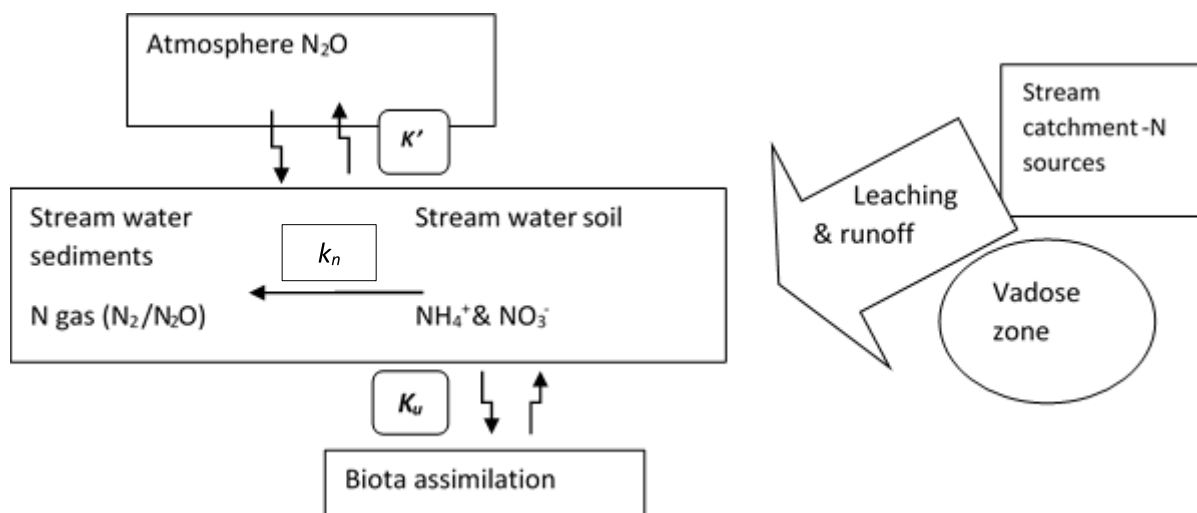
**Figure 2-3** Schematic of the nitrifier-denitrification pathway where  $N_2O$  production occurs as a result of nitrate respiration by nitrifiers, when the oxygen status is declining but not totally anaerobic (Wrage, 2001).

#### 2.4.3 Nitrous oxide production in river systems

Nitrous oxide emissions from ground and surface waters occurs either via  $N_2O$  leaching from the soil into ground or surface waters being released, or as a result of in-situ production (Reay et al., 2003).

The N input to river catchments is a consequence of leaching and runoff. As a main N component of these N inputs,  $NO_3^-$  plays an important role in  $N_2O$  emissions. However, the leached  $NO_3^-$ -N may also be assimilated in aquatic plants and algae as organic matter, a process known as biota assimilation. When the organic matter decomposes, biological N is released as ammonia ( $NH_4^+$  or  $NH_3$ ) and nitrified (Mosier, 1998). Such  $NH_4^+$  or  $NH_3$  may also undergo nitrification resulting in  $N_2O$  emissions.

Mullholand et al. (2004) explained stream denitrification and total N uptake using a schematic model. In terms of  $N_2O$  production, that model is modified for  $N_2O$  production in streams as follows.



**Figure 2-4 A model of N<sub>2</sub>O production in streams (modified from Mulholland et al., 2004)**  
**( $k'$ = water to air N<sub>2</sub>O exchange rate,  $k_n$ = N<sub>2</sub>O production rate from nitrification/denitrification and  $K_u$ = assimilative N uptake and release rate).**

The in-situ production of N<sub>2</sub>O in surface waters may vary with dissolved O<sub>2</sub> concentration (Clough et al., 2007; Harrison et al., 2005). During the day, due to photosynthesis, dissolved O<sub>2</sub> may increase and inhibit denitrification resulting in less N<sub>2</sub>O emissions. However, at night where respiration continues in the absence of O<sub>2</sub> inputs via photosynthesis, the dissolved O<sub>2</sub> may decrease, increasing N<sub>2</sub>O emissions.

Organic carbon may also increase the denitrification rate in waters, with high N<sub>2</sub>O emissions recorded in the presence of both carbon and NO<sub>3</sub><sup>-</sup>, an order of magnitude more than NO<sub>3</sub><sup>-</sup> alone (Harrison and Matson, 2003). Algae blooms also have the potential to create favourable conditions for rapid denitrification and N<sub>2</sub>O emissions in waterways by increasing organic carbon loads (An & Joye, 2001).

Nitrification and denitrification rates may be controlled by the surface water pH. For example, Watson et al. (1994) observed ammonium oxidisers were highly active when the pH ranged from 5.8 -8.5 with an optimum of 7.8. Knowles (1982) described denitrification as being positively related to water pH. Harrison and Matson (2003) also showed a positive correlation between N<sub>2</sub>O emissions and pH of drainage canals.

#### **2.4.4 Nitrous oxide from leaching and runoff**

The IPCC revised Guidelines were introduced in 1996 and 1998, in order to improve the methodology for estimating annual national N<sub>2</sub>O emission inventories. According to the IPCC Guidelines, the

national inventories use a default emission factor (EF5) for N<sub>2</sub>O emissions from N leaching and runoff. However, further developments were required to overcome deficiencies in national inventory calculations, especially the quantification of the anthropogenic N<sub>2</sub>O production following N leaching and runoff (Mosier et al., 1998). The second phase approach determined the direct emissions from agricultural fields, direct emissions from animal production systems and indirect emissions. The Guidelines were revised in 2006 and stated that a country has to follow the revised 1996 Guidelines and the 2000 IPCC Good Practice Guidance to measure the default emission factors, unless a country can fully justify why they have changed emission factors.

Indirect emissions partially result from N leaching and runoff (NLEACH) from agricultural systems. Agricultural inputs of N include fertiliser N (NFERT; kg N yr<sup>-1</sup>) and N derived from animal excretion (NEX; kg N yr<sup>-1</sup>). The fraction of N, from fertiliser and excreta that is leached (FRACLEACH), was estimated by Mosier et al., (1998) to range from 0.1- 0.8. In New Zealand a country specific value for FRACLEACH has been derived and equates to 0.07 kg (70 g) N leached from 1 kg of N input (Thomas et al., 2005).

Thus, the flux of N leached (NLEACH, kg N yr<sup>-1</sup>) is:

$$NLEACH = [NFERT+NEX]*FRACLEACH \quad 2.11$$

Production of N<sub>2</sub>O occurs when leached N moves into the aquatic environments; ground water and surface drainage, rivers, and estuaries. Emission factors for these three zones are designated as EF5-g, EF5-r and EF5-e, respectively (Mosier, 1998). The total indirect emissions are accounted for in the IPCC methodology using three separate emission factors based on dissolved NO<sub>3</sub><sup>-</sup> concentrations. The sum of these three components equates to the default value of EF5.

The N<sub>2</sub>O emissions due to agricultural N loss through leaching and runoff N<sub>2</sub>O (L) are calculated by multiplying NLEACH by the emission factor (EF5) for leaching and runoff,

$$N_2O (L) = NLEACH * EF5 \quad 2.12$$

The previously estimated default values used to derive the N losses from designated zones in the 1996 guidelines were;

1. EF5-g = Ground water and surface drainage (0.015 kg N<sub>2</sub>O-N per kg NLEACH)
2. EF5-r = River and flowing waters (0.0075 kg N<sub>2</sub>O-N per kg NLEACH)
3. EF5-e = Coastal and estuary surfaces (0.0025 kg N<sub>2</sub>O-N per kg NLEACH)

As a result, the EF5 value is assigned by taking the sum of the above default values and equates to 0.025 kg (25g) N<sub>2</sub>O-N per kg NLEACH.

In 2006, the estimated EF5 values were revised. Dong et al., 2004 and Clough et al., 2006 examined N<sub>2</sub>O emissions in rivers in Wales and England and lowland braided streams rivers in South Island New Zealand, respectively. These studies estimated EF5-r to equal between 0.0003 (0.3 g) and 0.0005 (0.5 g) kg N<sub>2</sub>O-N per kg NLEACH. As a result, in 2006, the EF5 was revised downwards from 0.025 to 0.0075 kg N<sub>2</sub>O-N/kg N leached/runoff reducing all EF5-g, EF5-r and EF5-e values to 0.0025 kg (2.5 g) N<sub>2</sub>O-N per kg NLEACH. However, the uncertainty in the revised value of EF5 remains large (de Klein, 2006).

#### **2.4.5 EF5-g: N<sub>2</sub>O emissions from groundwater**

Reay et al. (2003) observed N<sub>2</sub>O emissions from out gassing sites (tile drains) through soil profiles and obtained low EF5-g values of 0.0004-0.0006 with few samples reaching the IPCC default value of 0.0025. Hiscock et al. (2003) also found low N<sub>2</sub>O-N:NO<sub>3</sub><sup>-</sup>-N ratios of 0.0017 to 0.0019. Following these studies, Beaulieu et al. (2008) examined 12 agricultural river basins that had discharge rates ranging from 3.0 to 62.7 L s<sup>-1</sup> over 18 months period and found EF5-g equalled 0.0101. Reay et al. (2008) conducted a 17 month long study and found that, the value of EF5-g was 0.003 (range 0.00008 – 0.036) from an intensively grazed pasture catchment. These studies have observed lower EF5-g values than the current IPCC predicted values and supported the EF5-r downward revision to the new value of 0.0025. According to the IPCC methodology, NO<sub>3</sub><sup>-</sup> concentrations in stream water are considered as the best predictor of N<sub>2</sub>O emission rates.

#### **2.4.6 EF5-r: N<sub>2</sub>O emissions from rivers**

Measurements of N<sub>2</sub>O yields in rivers are limited. The IPCC guidelines assume the N<sub>2</sub>O yield is 0.5% for both denitrification and nitrification (Nevison, 2000). Cole and Caraco (2001) measured N<sub>2</sub>O fluxes from the Hudson River comparing their results with six previous river N<sub>2</sub>O flux measurement studies and found no significant effect of NO<sub>3</sub><sup>-</sup> concentrations on river N<sub>2</sub>O emissions. Many research

studies have observed lower EF5-r values than the current IPCC methodology default value. Clough et al. (2006) found  $\text{N}_2\text{O-N}:\text{NO}_3^- \text{-N}$  ratios were  $\leq 0.00067$  and the EF5-r value well below the current EF5-r default value of 0.0025. A potential artefact identified in this study was the degassing of  $\text{N}_2\text{O}$  in the river's upper reaches originating from groundwater sources at the springs.

Wilcock and Sorrell (2008) measured  $\text{N}_2\text{O}$  fluxes from three New Zealand spring-fed streams ( $\text{NO}_3^- \text{-N}$  was 0.3 to 4.0  $\text{mg L}^{-1}$ ; flow  $< 0.10$  to 0.97  $\text{m}^3 \text{s}^{-1}$ ) in the North Island. The mean fluxes of the study (taken from Table 2, Wilcock and Sorrell, 2008) averaged between  $4.5 \pm 4.0$  to  $17.2 \pm 21.2 \mu\text{mol N}_2\text{O m}^{-2} \text{h}^{-1}$  ( $125 \pm 112$  to  $483 \pm 594 \mu\text{g N}_2\text{O-N m}^{-2} \text{h}^{-1}$  ( $\pm$  stdev)). Their results were similar to those found by Clough et al. (2006) in a South Island lowland stream.

Baulch et al. (2011) studied 2 to 4 sites per stream on five streams for a 29 month period in southern Ontario, Canada. The estimated  $\text{N}_2\text{O}$  fluxes, derived using a gas exchange model, ranged from 5.8 to  $\mu\text{g m}^{-2} \text{h}^{-1}$  to 100  $\mu\text{g m}^{-2} \text{h}^{-1}$ . This study found a strong relationship between log-transformed  $\text{NO}_3^-$  concentrations and log-transformed  $\text{N}_2\text{O}$  fluxes. Clough et al. (2011) studied  $\text{N}_2\text{O}$  dynamics over a 397 day period in the braided Ashburton River, New Zealand, where  $\text{NO}_3^- \text{-N}$  concentrations averaged 0.57  $\text{mg L}^{-1}$  (range 0.02 - 1.36  $\text{mg L}^{-1}$ ) and increased as river distance increased. The  $\text{N}_2\text{O}$  saturation averaged 114% and correlated with  $\text{NO}_3^-$  concentration.

Beaulieu et al. (2011) carried out a comprehensive  $^{15}\text{N}$  tracer study in 72 headwater streams in the U.S.A. As a result of denitrification,  $^{15}\text{N}$  tracer was detected in  $\text{N}_2\text{O}$  evolved from 52 of the 73 streams. This is a key study of  $\text{N}_2\text{O}$  emissions from streams, and the stream  $\text{NO}_3^- \text{-N}$  concentrations correlated with  $\text{N}_2\text{O}$  emission rates. Following a modelling approach, Beaulieu et al. (2011) estimated that at the global scale, 0.75% of dissolved inorganic-N inputs were converted to  $\text{N}_2\text{O}$  via direct denitrification and nitrification. This is higher than the IPCC default.

Hinshaw and Dahlgren (2013) measured  $\text{N}_2\text{O-N}$  fluxes from the San Joaquin River in California using both floating chambers and headspace methods over a 13 month period. Nitrous oxide fluxes (9.5-352  $\mu\text{g N}_2\text{O-N m}^{-2} \text{h}^{-1}$ ) correlated linearly with dissolved  $\text{N}_2\text{O}$  concentrations and exponentially with  $\text{N}_2\text{O}$  saturation percentages. The calculated EF5-r value averaged 0.0028 (range 0.0012-0.0069). The highest values occurred during high flow events with low dissolved  $\text{NO}_3^-$  concentrations. Hinshaw and Dahlgren (2013) concluded that 'denitrification in anoxic sediments was the main mechanism for  $\text{N}_2\text{O}$  production.

Further research also queries the IPCC methodology. A study by Mulholland et al. (2004) found a nonlinear, positive relationship between  $\text{NO}_3^-$  loading and  $\text{N}_2\text{O}$  production. In this study, a 2-fold increase in the  $\text{NO}_3^-$  concentrations from 0.023 to 0.5  $\text{mg N L}^{-1}$  increased  $\text{N}_2\text{O}$  production 6-fold or more, per unit area. Another non-linear effect of  $\text{NO}_3^-$  vs.  $\text{N}_2\text{O-N}$  was found by Beaulieu et al. (2011).

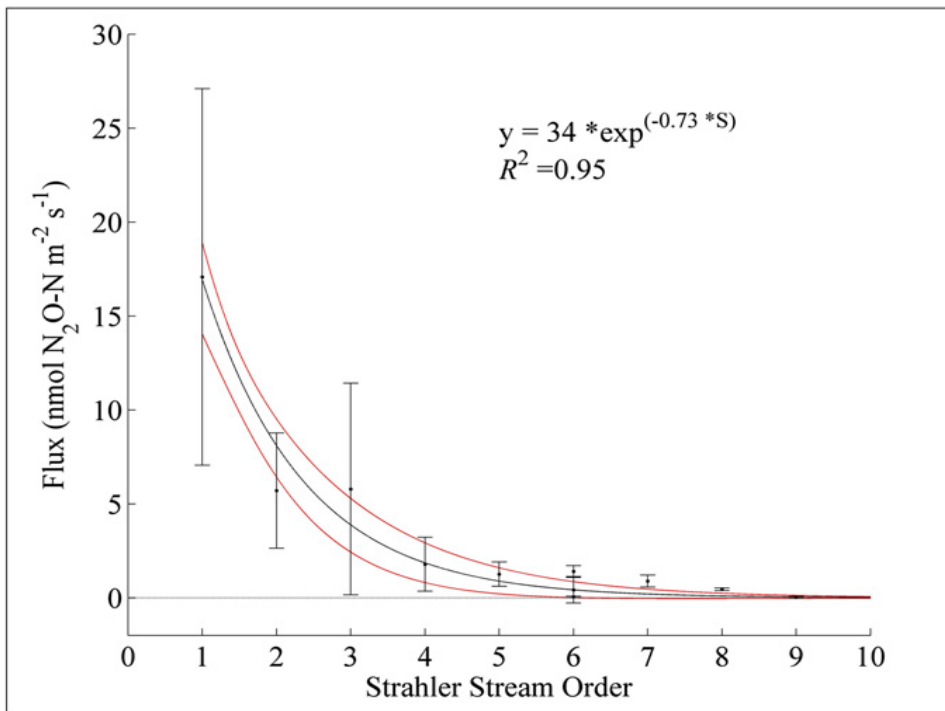
Following  $^{15}\text{N}$  tracer addition,  $\text{N}_2\text{O}$  production rates increased with increasing  $\text{NO}_3^-$  loading but only 1% of the denitrified N was produced as  $\text{N}_2\text{O}$ , and there was no relationship found between  $\text{N}_2\text{O}$  yield and stream  $\text{NO}_3^-$  loading rate. This study proved that  $\text{NO}_3^-$  loading stimulated the denitrification in streams producing  $^{15}\text{N}\text{-N}_2\text{O}$ , but the  $\text{N}_2\text{O}$  yield did not increase proportionally.

#### **2.4.7 Conditions affecting $\text{N}_2\text{O}$ emissions**

Hypoxia, low dissolved oxygen in rivers occurs when respiration exceeds the resupply of oxygen by photosynthesis and aeration. A study by Yu et al. (2013) found a correlation between higher  $\text{N}_2\text{O}$  saturation levels in the Shanghai river network that received sewage inputs. In this study,  $\text{NH}_4^+\text{-N}$  and dissolved oxygen were positively and negatively correlated to  $\text{N}_2\text{O}$  saturation respectively. A two year study on the Grand River, Canada (Rosamond et al., 2012) found that  $\text{N}_2\text{O}$  emissions were underestimated in dry seasons and overestimated in wet seasons with no relationship between  $\text{N}_2\text{O}$  emissions and dissolved  $\text{NO}_3^-$  concentrations, although there was a negative correlation with dissolved oxygen. They concluded that hypoxia was the main driver of  $\text{N}_2\text{O}$  emissions from river systems not the  $\text{NO}_3^-$  loading rate. A study on the Grand River by Venkiteswaran et al. (2014) also concluded that  $\text{N}_2\text{O}$  fluxes were higher during hypoxic conditions at low temperature conditions. Clough et al. (2007) and Wilcock and Chapra (2005) also described diel oxygen cycles and a lack of oxygen leading to an increase in  $\text{N}_2\text{O}$  emissions from New Zealand streams. It was suggested that  $\text{NO}_3^-$  was not the only limiting factor for  $\text{N}_2\text{O}$  production in rivers.

The current IPCC methodology for EF5-r calculations does not consider river geometry or water residence time. However, Peterson et al. (2001) reported the river morphology also influenced the processing of inorganic-N in streams. Turner et al. (2015) examined the  $\text{N}_2\text{O}$  emissions based on stream order and found  $\text{N}_2\text{O}$  fluxes from low order headwater streams often had higher fluxes than the higher order down-water streams (Figure 2-5). The studies of Clough et al. (2006) and Clough et al. (2007) also considered the water residence time in river systems as a factor that could influence the value of EF5-r for New Zealand where rivers have relatively short residence times, measured in hours. Beaulieu et al. (2011) hypothesised that the longer water-residence times in large rivers would result in a greater percentage of the  $\text{NO}_3^-$  being denitrified.





**Figure 2-5 The relation between N<sub>2</sub>O flux and the stream order in south-eastern Minnesota (Turner et al., 2015).**

Current methods to estimate riverine N<sub>2</sub>O emissions are based on the knowledge of N transformation pathways and hydrophysical conditions of waters. The effect of both nitrification and denitrification on N<sub>2</sub>O yield from surface waters may be smaller when compared with the terrestrial ecosystems (Beaulieu et al., 2011). Seasonal variances, N residence time, water quality and hydrophysical measurements may also affect the N<sub>2</sub>O yield from rivers. Due to variable N<sub>2</sub>O yields and the complexity of river systems, a simple relationship between N sources and N<sub>2</sub>O emissions from flowing waters may not exist.

#### **2.4.8 EF5-r measurements in New Zealand**

Few field studies have examined N<sub>2</sub>O fluxes from rivers in New Zealand. Those that have include: Wilcock and Sorrell (2008), Clough et al. (2006; 2007; 2011) and a scoping study Clough and Kelliher (2012) which was performed on the longest river in New Zealand, the Waikato River (Table 2.2).

**Table 2.2 Summary of EF5-r studies in New Zealand**

Reference	Water body	Method	N <sub>2</sub> O-N flux ( $\mu\text{g m}^{-2} \text{h}^{-1}$ )	NO <sub>3</sub> <sup>-</sup> -N ( $\text{mg L}^{-1}$ )	EF5-r <sup>a</sup> range
<b>Clough et al. 2006</b>	LII (lowland spring-fed stream)	Floating chambers	38-501	2.5 -5.3	0.00015-0.00067
<b>Clough et al. 2007</b>	LII (lowland spring-fed stream)	Floating chambers	52-140	3.0	0.00042-0.00065
<b>Clough et al. 2011</b>	Ashburton (Braided-gravel bed)	Head-space equilibrium <sup>b</sup>	16-30	0.02-1.36	0.0007-0.0169
<b>Wilcock &amp; Sorrell 2008</b>		Head-space equilibrium <sup>b</sup>			ND <sup>b</sup>
	Whakapipi		10-305	1.4 - 4.5	
	Toenepi		-1 – 770	0.1 – 3.4	
	Whangamaire		3 -2714	7.6 – 15.6	
<b>Clough and Kelliher 2012</b>	Waikato River, at 15 sites	Floating chambers	< 100	0.02 – 0.31	0.0010-0.0132

<sup>a</sup> Determined as the ratio of N<sub>2</sub>O-N: NO<sub>3</sub><sup>-</sup>-N; <sup>b</sup> Not Determined in this study (Clough et al. 2012).

There remains a need to examine New Zealand's indirect N<sub>2</sub>O emissions from headwater streams and field drains, in order to more accurately understand New Zealand's N<sub>2</sub>O inventory. There is also a lack of measurements for the N<sub>2</sub>O transfer rate from water to air and limited data available worldwide. Therefore, this study was performed to measure both N<sub>2</sub>O transfer rate and the effect of NH<sub>4</sub><sup>+</sup> on N<sub>2</sub>O emissions from an agricultural drain.

## Chapter 3

# Measuring the nitrous oxide transfer velocity ( $k_{N_2O}$ ) in an agricultural drain

### 3.1 Introduction

A fraction of the nitrogen nitrified within an agricultural drain may escape as  $N_2O$ , but the actual  $N_2O$  yield is unknown. One of the major reasons for this is the lack of data detailing the  $N_2O$  exchange rate between water to air. Scaling the water-air  $N_2O$  exchange in drains, streams and river systems is important when attempting to constrain indirect emissions of  $N_2O$  at temporal and spatial scales (Cole and Caraco, 2001). Knowing the  $N_2O$  transfer velocity ( $k_{N_2O}$ ), the diffusive  $N_2O$  fluxes from waters can either be measured directly or calculated from the dissolved equilibrium  $N_2O$  concentrations, using equation 2.4.

Two experiments were performed in the summer (January) and late winter (August) of 2015 to measure the  $N_2O$  exchange across the water- air interface in an agricultural drain. Following the continuous tracer addition method (2.3.3), the experiments were designed to measure the  $k_{N_2O}$ , in a given reach, using propane ( $C_3H_8$ ) as the tracer gas, while measuring the real time  $N_2O$  emissions from the drain. The experiment employed both headspace equilibrium and floating chamber methods and evaluated the consistency of the obtained values in the context of published gas transfer models and values.

### 3.2 Method

#### 3.2.1 Field site

The experiments were performed at a spring-fed drain site flowing north to south alongside Raineys Road (Figure. 3-1). The drain flows into the Halswell River (43°S and 172°E), which is one of the main waterways entering Lake Ellesmere. The chemical, physical and biological measurements, described below, were collected over a 200 m length of the drain where no other inlets, that could alter the volume and its chemical composition, occurred. Adjacent farmlands were predominantly dairy pasture. The bottom of the drain was covered in fine sediments (3 – 10 cm deep) and the water was clear. Giant-meadow buttercup (*Ranunculus sp.*), sedges (*Carex sp.*) and monkey musk (*Mimulus sp.*) were abundant on the sides of the drain with a small quantity of floating duck weed (*Lemna minor*) also present.



**Figure 3-1** Raineys Road drain

### 3.2.2 Hydrological and geophysical measurements

The drain had a gradient of 1:0.0019 (5.2 m fall over 2.7 km) which was determined using a Garmin™ GPS. Water velocity ( $V$ ) was determined using the Rhodamine<sup>WT</sup> dye method (Liang & Richardson, 1971). Water temperature and dissolved  $O_2$  were measured by placing the sensor of the YSI-DO™ (USA) meter at 10 cm depth on three consecutive times at each site. Drain water geo-physical measurements were determined with a measuring tape.

The discharge rate,  $Q$  ( $L\ s^{-1}$ ), was calculated using the bromide ( $Br^-$ ) dilution data as follows (Marzolf et al., 1994).

$$Q = \frac{Solution\ [Br^-] \times RR}{Site\ [Br^-]} \quad 3.1$$

where,  $Solution\ [Br^-]$  is the  $Br^-$  concentration of the added carboy solution ( $g\ L^{-1}$ ),  $RR$  is the solution release rate ( $L\ s^{-1}$ ) and the  $Site\ [Br^-]$  is the  $Br^-$  concentration at a given sampling site ( $g\ L^{-1}$ ).

The mean drain depth ( $D$ ), in metres, was calculated as (Alin et al., 2011);

$$D = \frac{Q}{U \times W} \quad 3.2$$

where,  $Q$  is the water discharge rate ( $\text{m}^3 \text{s}^{-1}$ ),  $U$  is the water velocity at measurement site ( $\text{m s}^{-1}$ ) and  $W$  is the drain width (m). Discharge rate -  $Q$  was determined from the  $\text{Br}^-$  dilutions (Equation 3.1).

Water velocity was estimated using the break-through concentration curves of the Rhodamine<sup>WT</sup> dye that was injected into the drain immediately after the tracer experiment concluded. Three water samples were collected at each site; the time that maximum concentration occurred was used to estimate the drain water velocity.

Median three hourly wind speed and air temperature data were taken from the Broadfield Ews (Plant and Food Research), Lincoln metrological station (Cliflo No. 17603, - 43.62, 172.47).

### 3.2.3 Mixed tracer solution

Two experiments were performed: the first was a preliminary experiment (Experiment 1), performed on 20<sup>th</sup> January, 2015. Propane ( $\text{C}_3\text{H}_8$ ) was added as a gas tracer with a conservative tracer ( $\text{Br}^-$ ) and a visual tracer (Rhodamine<sup>WT</sup> dye) to measure the gas transfer coefficient of the drain. The second experiment (Experiment 2) was performed on 12<sup>th</sup> August, 2015 with  $\text{C}_3\text{H}_8$ ,  $\text{Br}^-$ , Rhodamine<sup>WT</sup> and the  $^{15}\text{N-NH}_4^+$  tracer as a nitrifiable N source, in order to measure the gas transfer coefficient and  $\text{N}_2\text{O}$  emissions due to nitrification of  $\text{NH}_4^+$ .

In experiment 1, a tracer solution was constituted on site in an 80 L carboy. The carboy solution comprised of: 0.3 kg of potassium bromide (KBr) and 10 mL of Rhodamine<sup>WT</sup> dissolved in 5 L of drain water. The carboy was then filled with stream water (75 L) and mixed well before being released, while being constantly purged with 99.9%  $\text{C}_3\text{H}_8$ , into the drain using a peristaltic pump (Fondriest, CA, USA). The solution was released at a rate of  $17 \text{ mL s}^{-1}$  to increase the drain water  $\text{Br}^-$  concentration so that it was  $> 0.1 \text{ mg L}^{-1}$  for 60 minutes.

In experiment 2, the tracer solution comprised of 1.0 kg of KBr and 800 g of  $^{15}\text{N}$  enriched  $(\text{NH}_4)_2\text{SO}_4$  in an 80 L carboy. When experiment 2 was performed, the drain discharge volume was estimated to be  $130 \text{ L s}^{-1}$  and the carboy solution was continuously released into the drain using a peristaltic pump at a rate of  $17 \text{ mL s}^{-1}$  while 99.9% pure  $\text{C}_3\text{H}_8$  continued to purge the solution. The pump rate and the solution concentrations were based on needing to increase the stream water  $\text{Br}^-$  concentration by approximately  $1 \text{ mg L}^{-1}$ . Due to the potential for the visual tracer, Rhodamine<sup>WT</sup>, to interfere with the  $\text{NH}_4^+$  detection method (phenol, hypochlorite colorimetric method), Rhodamine<sup>WT</sup> was added in a separate dosing experiment, immediately after the final collection of water samples as noted below, in order to determine water speed.

### 3.2.4 Sampling time, stations and collection

In experiment 1, water and gas sampling sites were positioned along the drain at 15, 40, 65, and 165 metres from the tracer solution injection point. The samples were collected every 15 minutes, four times for an hour (15, 30, 45 and 60 minutes) following commencement of tracer injection at time zero. At each site, sampling involved collecting triplicate water samples for dissolved  $\text{C}_3\text{H}_8$ ,  $\text{Br}^-$  and Rhodamine<sup>WT</sup> dye measurements.

In experiment 2, sampling sites were positioned at 15, 40, 65, 165 and 215 m from the injection point. Both water and air samples were collected every 15 minutes, five times for 1.25 hours (15, 30, 45, 60 and 75 minutes), following commencement of tracer injection at time zero. At each site, triplicate water samples were collected for dissolved  $\text{C}_3\text{H}_8$ ,  $\text{Br}^-$  and Rhodamine<sup>WT</sup> dye measurements.

Additionally, in experiment 2, surface  $\text{C}_3\text{H}_8$  and  $\text{N}_2\text{O}$  gas fluxes were also determined using floating chambers at sites located at 25, 50, and 200 m. Floating chamber design, construction and gas sampling procedures were previously described in Clough et al. (2006). The total volume of the chamber headspace was 4.2 L with an area of  $0.159 \text{ m}^2$ . Fluxes of  $\text{C}_3\text{H}_8$  were measured using three chambers at each site. Each chamber was sampled at 15 minute intervals for 75 minutes (5 times), after tracer was released, using a glass syringe, fitted with a three way stopcock and a 27 gauge needle. When sampling the needle was inserted through the septa of the chambers and flushed twice and then 10 mL gas samples were extracted and injected into pre-evacuated 6.0 mL Exetainer<sup>®</sup> (Labco Ltd, High Wycombe, UK) vials. Prior to each gas sampling, the syringe was flushed twice with ambient air to prevent any contamination between samples. Then, the sample vials were transported to the laboratory for  $\text{C}_3\text{H}_8$  and  $\text{N}_2\text{O}$  analyses by gas chromatography (GC).

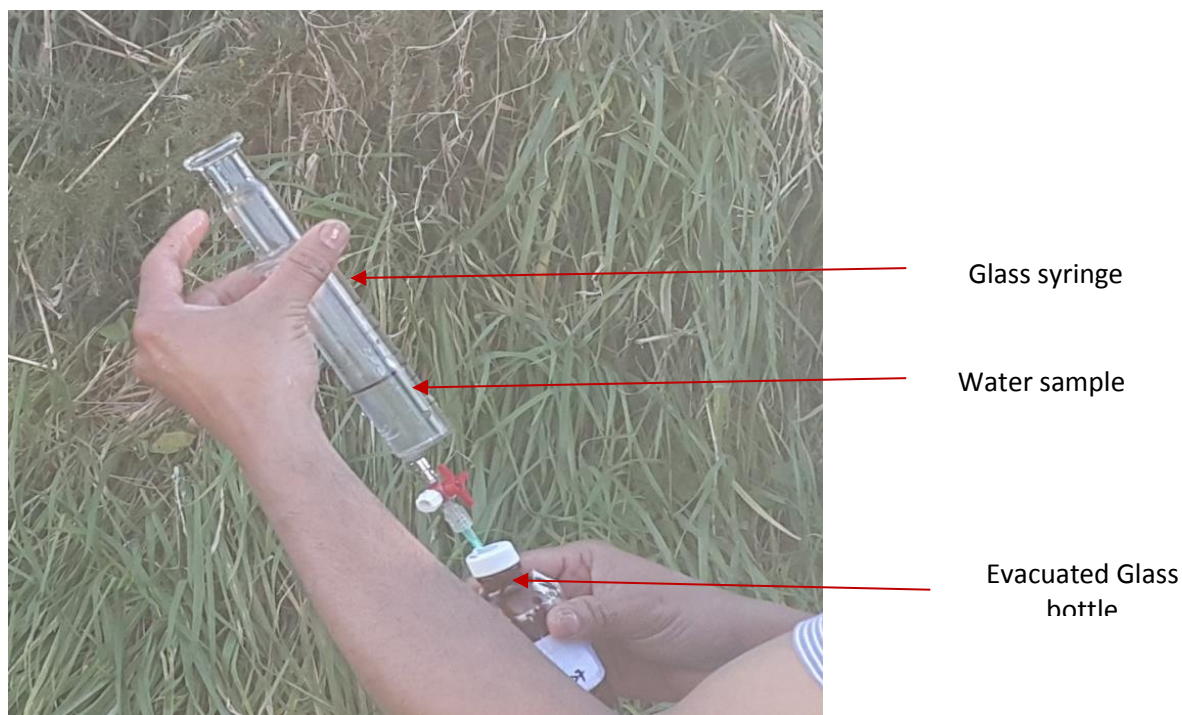




Figure 3-2 Topographical map showing measurement sites of the Rainey's road drain. Direction of the water flow is shown by the arrow. (Scale 1.0 cm: 0.25 Km)

### 3.2.5 Dissolved propane measurements

In both experiments, triplicate 50 mL water samples were collected 10 cm below the water surface by slowly drawing 50 mL of water into a pre-flushed gas-tight glass syringe (Cadence science inc, Staunton, VA) fitted with a three-way stopcock (Figure 3-3).



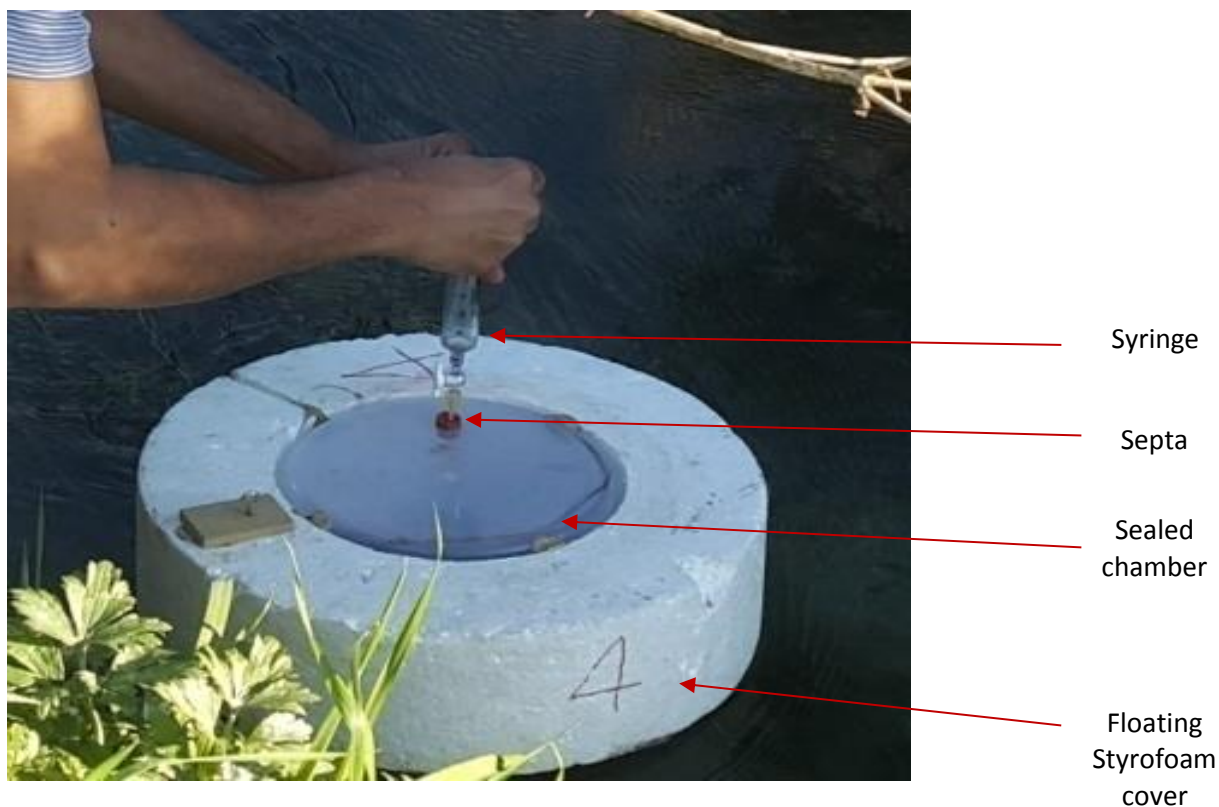
**Figure 3-3 Dissolved gas extractions by headspace method**

A needle was placed on the stopcock, and the dead-space within the needle was displaced with the sampled water by exerting pressure on the syringe, prior to injecting the water sample into a helium-flushed pre-evacuated glass bottle ( $105 \pm 2$  mL) fitted with a butyl rubber septum (Figure 3-3). The bottles were stored in a chilly-bin and transported to the laboratory. The bottles' headspace (55 mL) were filled with UHP helium and shaken for 5 minutes to equilibrate the dissolved gasses in the liquid and gas phases. The headspace gas was sampled using a glass syringe fitted with a three-way stopcock and then 10 mL was transferred to pre-evacuated 6.0 mL vials. Ambient air samples were also collected at each sampling site. The same sampling procedure, using 50 mL distilled water, was performed in the laboratory as a control.

### 3.2.6 Floating chamber gas collection and measurements

In experiment 2, gas samples were collected from floating chambers (Figure 3-4) at sites 1, 3 and 5. Five gas samples were collected from the headspace of each chamber at 15, 30, 45, 60 and 75 minutes as previously described (Clough et al., 2006).





**Figure 3-4 Floating chamber headspace gas sampling**

### 3.2.7 Gas analysis

Gas samples in the 6 mL Extetainers were analysed for  $\text{N}_2\text{O}$  and  $\text{C}_3\text{H}_8$  concentrations using an SRI 8610 CA USA, Gas Chromatograph (GC). Propane and  $\text{N}_2\text{O}$  were separated using a 2 m long Poropak Haysep B column held at  $65^\circ\text{C}$ , where the  $\text{N}_2\text{O}$  retention time was eight minutes and the  $\text{C}_3\text{H}_8$  retention time was 12 minutes. Propane and  $\text{N}_2\text{O}$  concentrations were detected using a heated Flame Ionization Detector (FID) at  $100^\circ\text{C}$  and an Electron Capture Detector (ECD) at  $310^\circ\text{C}$ , respectively. A range of reference gases ( $0.02$  to  $1000\ \mu\text{L L}^{-1}$ , BOC, NZ) were used to generate standard curves to determine  $\text{C}_3\text{H}_8$  and  $\text{N}_2\text{O}$  concentrations. The configuration of the GC and sample handling procedures have been described previously (Kelliher et al., 2015).

### 3.2.8 Dissolved gas concentrations and gas transfer rate calculations

#### 3.2.8.1 Headspace equilibrium method for determination of N<sub>2</sub>O transfer coefficient ( $k'_{N_2O}$ )

Total dissolved C<sub>3</sub>H<sub>8</sub> and N<sub>2</sub>O concentrations were calculated using the formula of (Tiedje, 1983).

$$M = C_g \times [V_g + (V_l \times \beta)] \quad 3.3$$

where,  $M$  is the total gas present in an evacuated bottle ( $\mu\text{L}$ ),  $C_g$  is the head space gas concentration ( $\mu\text{L L}^{-1}$ ),  $V_g$  is the volume of gas in the bottle (L),  $V_l$  is the volume of liquid (L) and  $\beta$  is the Bunsen coefficient ( $\mu\text{L L}^{-1}$ ).

Since the bottles were initially evacuated all the C<sub>3</sub>H<sub>8</sub> and N<sub>2</sub>O gas derives from the 50 mL water sample initially added to the bottle. Therefore, the dissolved gas volume in a litre of water was measured by dividing  $M$  ( $\mu\text{L}$ ) by the volume of water (L) (Davidson & Firestone, 1988).

The moles of the gas in the water sample were calculated using the ideal gas law;

$$n = PV / RT \quad 3.4$$

where,  $n$  is the gas concentration (moles  $\text{L}^{-1}$ ),  $P$  is the atmospheric pressure (1 atm),  $V$  is the volume of gas (L),  $R$  is the universal gas constant ( $0.0821 \text{ L atm K}^{-1} \text{ mol}^{-1}$ ) and  $T$  is the air temperature (K).

The difference in the dissolved trace gas concentrations ( $dC$ ) between time zero and travel time  $t$  ( $dt$ ) is equivalent to the amount of gas lost into the atmosphere. Thus, the tracer gas dissipation rate was determined as;

$$dC/dt = k' (C_t - C_0) \quad 3.5$$

where,  $dC/dt$  is the rate of concentration change per minute ( $\text{mol L}^{-1} \text{ min}^{-1}$ ),  $k'$  is the gas transfer coefficient ( $\text{min}^{-1}$ ),  $C_t$  is the gas concentration ( $\text{mol L}^{-1}$ ) after time  $t$  and  $C_0$  is the gas concentration at time  $t_0$  ( $\text{mol L}^{-1}$ ).

The gas exchange from water to air is a first order kinetic process (Stolk et al., 2009). To measure the gas transfer coefficient ( $k'$ ), the gas concentration at time  $t$  ( $C_t$ ) was measured as;

$$C_t = C_0 - k' (t_1 - t_0) \quad 3.6$$

Therefore,

$$\ln C_t / C_0 = -k' (t_1 - t_0) \quad 3.7$$

where,  $(t_1 - t_0)$  is the gas travel time in minutes and  $\ln C_t / C_0$  is the natural log concentration ratio at time  $t$  and time  $t_0$  for a given distance.

According to equation 3.7, the gas transfer coefficient ( $k'$ ) can be determined by plotting the logarithm of the dissolved gas concentration as a function of time (Chapra & Wilcock, 2000). The slope of the plotted linear regression is the gas transfer coefficient ( $k'$ ).

Generally, the gas transfer coefficient is a function of water turbulence, the kinematic viscosity and the diffusion coefficient of the water (Wanninkhof, 1992). The Schmidt number is a unitless ratio of the kinematic viscosity to the diffusion coefficient of the gas of interest ( $C_3H_8$  and  $N_2O$ ), which is sensitive to temperature. The Schmidt value ( $Sc$ ) for dissolved gasses in fresh water was calculated as a function of temperature for  $C_3H_8$  and  $N_2O$  according to equation 3.8 and 3.9 (Wanninkhof, 1992);

$$Sc_{(C_3H_8)} = 1911.1 - 118.11 * T + 3.4527 * T^2 - 0.04132 * T^3 \quad 3.8$$

$$Sc_{(N_2O)} = 2055.6 - 137.11 * T + 4.3173 * T^2 - 0.05435 * T^3 \quad 3.9$$

where,  $T$  is the temperature in degrees Celsius.

Using the propane gas transfer coefficient ( $k'_{C_3H_8}$ ) derived from data sets of experiment 1 and 2, the  $N_2O$  transfer coefficient ( $k'_{N_2O}$ ) was estimated as follows;

$$k'_{N_2O} = (Sc_{N_2O} / Sc_{C_3H_8})^n * k'_{C_3H_8} \quad 3.10$$

where,  $Sc$  is the temperature specific Schmidt number for  $C_3H_8$  and  $N_2O$  (Wanninkhof, 1992),  $n$  is the Schmidt exponent, which is equal to 0.5 for rough bottom surfaces and 0.66 for smooth bottom surfaces (Jähne et al., 1987). Then, the estimated  $k'_{N_2O}$  is standardised at 20°C as  $k'_{2(N_2O)}$  according to (Wanninkhof, 1992);

$$k'_{2(N_2O)} = k'_{N_2O} (600 / Sc_{N_2O(T)})^n \quad 3.11$$

where,  $k'_{2(N_2O)}$  is the  $N_2O$  gas transfer coefficient standardised at 20°C and  $Sc_{N_2O(T)}$  is the  $N_2O$  Schmidt number at temperature  $T$ .

The water-air  $N_2O$  transfer coefficient transfers to the air-water  $N_2O$  transfer velocity that is specific for the measurement drain. As per equation 2.3, the calculated  $k'_{2(N_2O)}$  value was multiplied by depth

of the drain (m) to determine the air-water N<sub>2</sub>O transfer velocity ( $k_{N2O}$ ), which can be used to directly calculate the N<sub>2</sub>O flux.

### 3.2.8.2 Floating chamber method for determination of N<sub>2</sub>O transfer velocity ( $k_{N2O}$ ) using propane (C<sub>3</sub>H<sub>8</sub>) as a tracer gas

The gas flux,  $F$  ( $\mu\text{mol m}^{-2} \text{ hr}^{-1}$ ) from the drain surface was calculated using the following equation (Beaulieu et al., 2011; Frankignoulle, 1988).

$$F = (dC/dt) * (V/A) * (P/RT) \quad 3.12$$

where,  $dC/dt$  is the increased rate of gas partial pressure within the chamber ( $\mu\text{L L}^{-1} \text{ hr}^{-1}$ ),  $V$  is the volume of chamber (L),  $A$  is the surface area of the drain water enclosed in the chamber ( $\text{m}^2$ ),  $P$  is the atmospheric pressure (atm),  $R$  is the universal gas constant ( $0.0821 \text{ L atm K}^{-1} \text{ mol}^{-1}$ ), and  $T$  is the air temperature in (K).

Then, the calculated propane flux ( $F_{C3H8}$ ) from the chamber measurements and the dissolved gas concentrations at each site were substituted into equation 3.13 to determine the C<sub>3</sub>H<sub>8</sub> transfer velocity ( $k_{C3H8}$ ) according to (Beaulieu et al., 2008);

$$k_{C3H8} = F_{C3H8} / (X_{aq} - X_g) \quad 3.13$$

where,  $k_{C3H8}$  is the C<sub>3</sub>H<sub>8</sub> transfer velocity ( $\text{m hr}^{-1}$ ),  $F$  is the C<sub>3</sub>H<sub>8</sub> flux from water to air ( $\mu\text{mol or moles, m}^{-2} \text{ hr}^{-1}$ ),  $X_{aq}$  is the C<sub>3</sub>H<sub>8</sub> concentration in the aqueous phase ( $\text{moles m}^{-3}$ ),  $X_g$  is the equilibrium C<sub>3</sub>H<sub>8</sub> concentration in the liquid phase ( $\text{mol m}^{-3}$ ).

Using the C<sub>3</sub>H<sub>8</sub> gas transfer velocity ( $k_{C3H8}$ ), the N<sub>2</sub>O transfer velocity ( $k_{N2O}$ ) was estimated as follows.

$$k_{N2O} = (S_{C_{N2O}} / S_{C_{C3H8}})^{-n} * k_{C3H8} \quad 3.14$$

where,  $Sc$  is the temperature specific Schmidt number for C<sub>3</sub>H<sub>8</sub> and N<sub>2</sub>O (Wanninkhof, 1992),  $n$  is the Schmidt exponent, which is equal to 0.5 for rough bottom surfaces and 0.66 for smooth bottom surfaces (Jähne et al., 1987).

Then the estimated  $k_{N2O}$  was standardised at 20°C as  $k_{(N2O)}$  according to the previously described equation 3.11 as follows (Wanninkhof, 1992);

$$k_{(N2O)} = k_{N2O} (600 / S_{C_{N2O}(T)})^{-n} \quad 3.15$$

where,  $k_{(N2O)}$  is the N<sub>2</sub>O gas transfer velocity standardised at 20°C and  $S_{C_{N2O}(T)}$  is the N<sub>2</sub>O Schmidt number at temperature  $T$ .

### 3.2.8.3 Determination of N<sub>2</sub>O transfer velocity ( $k_{N_2O}$ ) from Wilcock (1982) model

Oxygen transfer velocity ( $k_{O_2}$ ) was determined for sampling site depth using equation 2.10. Using the  $k_{O_2}$  derived from data sets of experiment 1 and 2, the N<sub>2</sub>O transfer coefficient ( $k_{N_2O}$ ) was estimated as follows;

$$k_{N_2O} = (Sc_{N_2O} / Sc_{O_2})^{-n} * k_{O_2} \quad 3.16$$

where,  $Sc$  is the temperature specific Schmidt number for N<sub>2</sub>O and O<sub>2</sub> (Wanninkhof, 1992),  $n$  is the Schmidt exponent, which is equal to 0.5 for rough bottom surfaces and 0.66 for smooth bottom surfaces (Jähne et al., 1987). Then, the estimated  $k_{N_2O}$  is standardised at 20°C as  $k_{(N_2O)}$  as per equation 3.11.

### 3.2.8.3 Direct N<sub>2</sub>O transfer velocity ( $k_{N_2O}$ ) using N<sub>2</sub>O flux and dissolved N<sub>2</sub>O concentrations

The N<sub>2</sub>O flux from the drain surface was calculated according to equation 3.12. Then, equation 2.4 was used to estimate  $k_{N_2O}$ , substituting the measured N<sub>2</sub>O flux and the known equilibrium N<sub>2</sub>O concentrations. The estimated  $k_{N_2O}$  is standardised at 20°C as  $k_{(N_2O)}$  as per equation 3.11.

### 3.2.9 Statistical analysis

Statistical analyses were performed using Minitab® version 16 (Minitab Inc., PA, USA) and Microsoft Excel, 2010. Means, standard deviations and standard errors were calculated for data as appropriate. Analysis of variance was employed, if the means of variables differed between sampling times. When the difference occurred, the effect of time on tracer mixing was calculated by the sum of squares between groups divided by the total sum of squares ( $\eta^2$ ). The Bonferroni post-hoc tests were performed to determine the significance of the variations between sampling times.

### 3.3 Results

#### 3.3.1 Micro-metrological conditions

During the first tracer addition (Experiment 1), average atmospheric pressure, air temperature and wind speed were 1012 mbar, 17.3°C and 5.9 km hr<sup>-1</sup> (Southwest), respectively. During the second tracer addition (Experiment 2), average atmospheric pressure and air temperature were 1022 mbar and 6.4°C, respectively. The wind speed was 2.2 km h<sup>-1</sup> from the northeast over the 1.5 hr experimental period.

#### 3.3.2 Drain water hydro physical measurements

Hydro physical conditions of the drain were typical in both experiment 1 (summer) and experiment 2 (late winter). The drain discharge rate (Equation 3.1) was stable over the 1 and 1.5 hr study periods of experiments 1 and 2, respectively. From December 2014 to September 2015, fortnightly recorded typical base flow rates averaged  $54 \pm 21 \text{ L s}^{-1}$  in summer (December 2014 to February 2015),  $78 \pm 33 \text{ L s}^{-1}$  in autumn (March to May 2015), and  $135 \pm 45 \text{ L s}^{-1}$  in winter (June to August, 2015). The drain water temperature, dissolved O<sub>2</sub>, and geo-physical measurements are summarised in Table 3.1 and 3.2.

**Table 3.1 Experiment 1; the drain water chemistry and physical measurements. (Temperature and dissolved oxygen errors =  $\pm$  standard deviations of three samples).**

Measurement	Site 1 (15 m)	Site 2 (40 m)	Site 3 (65 m)	Site 4 (165 m)	Mean
Temperature °C (n=3)	15.1 $\pm$ 0.2	15.2 $\pm$ 0.3	15.3 $\pm$ 0.4	15.5 $\pm$ 0.3	15.3 $\pm$ 0.3
Dissolved O <sub>2</sub> mg L <sup>-1</sup> (n=3)	11.2 $\pm$ 0.9	11.0 $\pm$ 0.6	11.1 $\pm$ 0.8	10.7 $\pm$ 0.3	11.0 $\pm$ 0.7
Width (m)	1.35	1.45	1.50	1.40	1.42 $\pm$ 0.05
Wetted width (m)	2.10	2.25	1.98	2.32	2.16 $\pm$ 0.12
Depth (m) (n=3)	0.19 $\pm$ 0.02	0.18 $\pm$ 0.02	0.19 $\pm$ 0.02	0.20 $\pm$ 0.03	0.19 $\pm$ 0.02

**Table 3.2 Experiment 2; the drain water chemistry and physical measurements. (Temperature and dissolved oxygen errors =  $\pm$  standard deviations of three samples).**

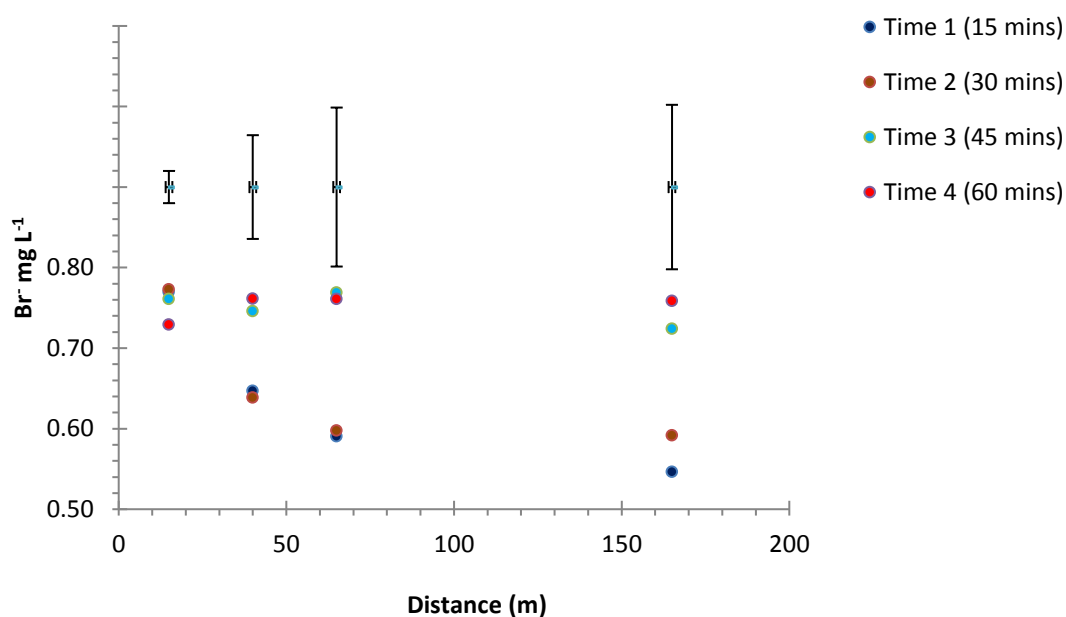
Measurement	Site 1 (15 m)	Site 2 (40 m)	Site 3 (65 m)	Site 4 (165 m)	Site 5 (215 m)	Mean
<b>Temperature °C (n=3)</b>	11.3 $\pm$ 0.3	11.5 $\pm$ 0.2	11.9 $\pm$ 0.2	12.2 $\pm$ 0.3	12.4 $\pm$ 0.4	11.9 $\pm$ 0.31
<b>Dissolved O<sub>2</sub> mg L<sup>-1</sup> (n=3)</b>	12.4 $\pm$ 0.9	11.4 $\pm$ 0.6	11.3 $\pm$ 0.8	11.2 $\pm$ 0.3	11.0 $\pm$ 0.3	11.5 $\pm$ 0.6
<b>Width (m)</b>	1.43	1.52	1.64	1.47	1.98	1.61 $\pm$ 0.20
<b>Wetted width (m)</b>	2.26	2.34	2.08	2.59	3.35	2.52 $\pm$ 0.44
<b>Depth (m), (n=3)</b>	0.32 $\pm$ 0.03	0.31 $\pm$ 0.02	0.30 $\pm$ 0.02	0.36 $\pm$ 0.04	0.38 $\pm$ 0.05	0.33 $\pm$ 0.03

The drain physical measurements (Table 3.1 and 3.2) show that, the drain width, wetted width and water depth during experiment 1 were smaller than during experiment 2. In experiment 1, the average drain water temperature at site 1 was 15.1  $\pm$  0.2°C and this increased to 15.5  $\pm$  0.3°C at 165 m downstream. In experiment 2, the average drain water temperature at site 1 was 11.3  $\pm$  0.3°C and this increased to 12.4  $\pm$  0.4°C at 215 m downstream (Table 3.1 and 3.2).

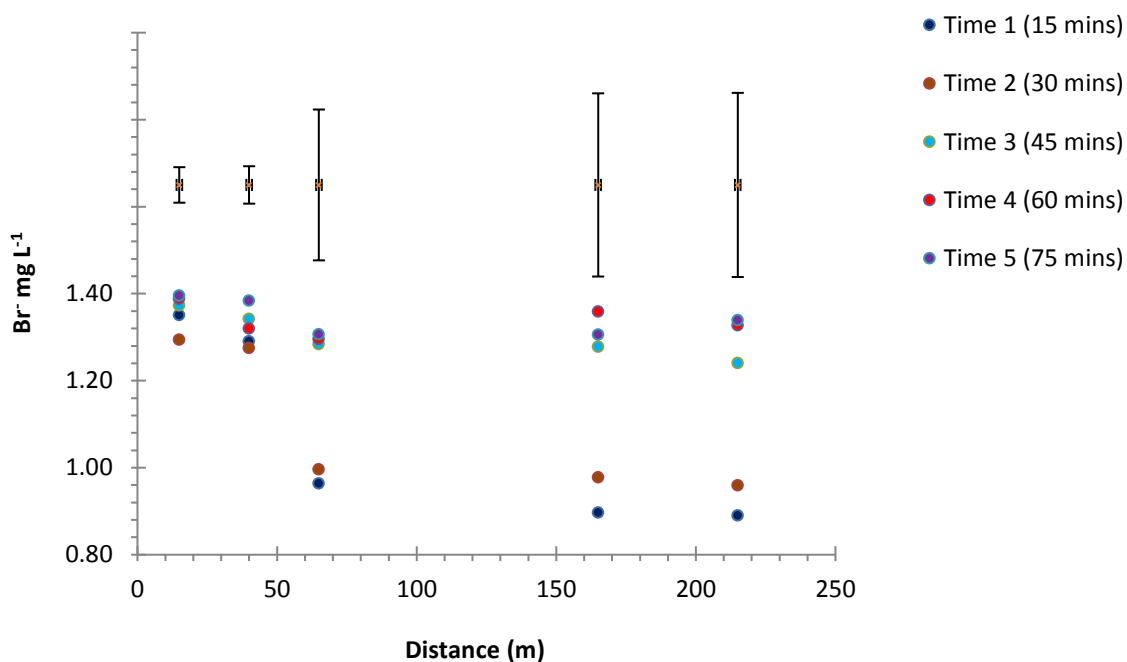
### 3.3.3 Drain water Bromide (Br<sup>-</sup>) measurements

In experiment 1, Br<sup>-</sup> was released into the drain at a rate of 0.017 L s<sup>-1</sup> at a concentration of 3 g L<sup>-1</sup>. In experiment 2, Br<sup>-</sup> was released into the drain at the same rate, but the concentration of Br<sup>-</sup> was increased to 10 g L<sup>-1</sup> due to the larger discharge volume in the drain at this time. Before commencement of Br<sup>-</sup> addition, there was no detectable Br<sup>-</sup> in the water. The discharge rate,  $Q$  (L s<sup>-1</sup>) was calculated using the bromide (Br<sup>-</sup>) dilution data as per equation 3.1.

In experiment 1, at site 1, the overall mean Br<sup>-</sup> concentration was 0.76  $\pm$  0.02 mg L<sup>-1</sup> and at site 5, it was 0.66  $\pm$  0.10 mg L<sup>-1</sup> (Figure 3-5). In experiment 2, at site 1, the overall mean Br<sup>-</sup> concentration was 1.35  $\pm$  0.04 mg L<sup>-1</sup> and at site 5, it was 1.08  $\pm$  0.21 mg L<sup>-1</sup> for all sampling times (Figure 3-6).



**Figure 3-5 Experiment 1: Drain water  $\text{Br}^-$  concentration over distance and sampling time following commencement of tracer solution injection at time zero. Error bars = stdev, (n = 4) of mean  $\text{Br}^-$  concentrations over all sampling times.**



**Figure 3-6 Experiment 2: Drain water  $\text{Br}^-$  concentration over distance and sampling time following commencement of tracer solution injection at time zero. Error bars = Stdev, (n = 5) of mean  $\text{Br}^-$  concentrations over all sampling times.**



The standard deviations of the Br<sup>-</sup> concentrations (Stdev) in both experiments increased with sampling distance (Figures 3-5 & 3-6). There was also a trend for Br<sup>-</sup> concentrations to increase as time progressed, especially in downstream sampling sites. The variations in Br<sup>-</sup> concentrations may occur due to insufficient mixing of tracer solution at the earlier sampling times and the impact of time on Br<sup>-</sup> concentration is evaluated further below.

### 3.3.4 Drain water steady state measurements – correction from Br<sup>-</sup> concentration

A one-way analysis of variance (ANOVA) was performed to assess the impact of time on Br<sup>-</sup> concentrations at a given sampling site. There were statistical differences in Br<sup>-</sup> concentration due to sampling time in both experiments 1 and 2 ( $p < 0.05$ ). The mean Br<sup>-</sup> concentration differences declined with later sample collections; increased sampling times (Figure 3-5 and 3-6). In experiment 1, the time effect on Br<sup>-</sup> concentration, calculated using  $\eta^2$  (Sum of squares between groups divided by the total sum of squares) for times 1, 2, 3, 4, times 2, 3, 4, and times 3 and 4 were 0.54, 0.47 and 0.07, respectively. Thus, the effect of sampling time on Br<sup>-</sup> concentration was not significant when sampling times 3 and 4 were considered. In addition, in experiment 1, the Post hoc corrected T-test (two samples assuming equal variances between sampling times) for sampling times 3 and 4 was  $< 0.012$  which further demonstrated that there were no significant Br<sup>-</sup> concentration differences between sampling times 3 and 4. In experiment 2, the time effect on Br<sup>-</sup> concentration was again estimated using  $\eta^2$  for times 1, 2, 3, 4, 5, times 2, 3, 4, 5 and times 3, 4 and 5 with values of 0.58, 0.49 and 0.17, respectively. Following the same trend as in experiment 1, the time effect on Br<sup>-</sup> concentration in experiment 2 declined with increasing sampling times. The Post hoc corrected T-test between sampling times 3, 4 and 5 of experiment 2 was  $< 0.1$ . Thus, in experiment 2, there were no significant Br<sup>-</sup> concentration differences between sampling times 3, 4 and 5.

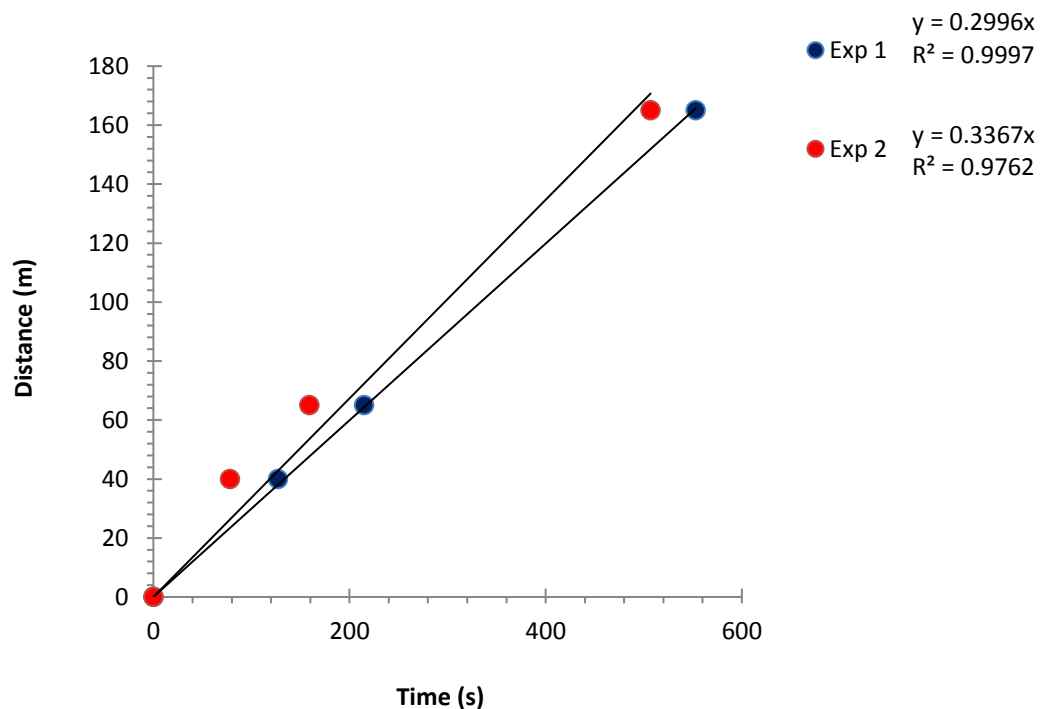
Therefore, it was concluded that the drain water mixed with the tracer solution to reach a steady state by sampling times 3 and 4 in experiment 1, and by sampling times 3, 4 and 5 in experiment 2.

In experiment 1, the average Br<sup>-</sup> concentration across all sites when pooling data for times 3 and 4, was  $0.76 \pm 0.02 \text{ mg L}^{-1}$ . In experiment 2, the average Br<sup>-</sup> concentration at time 3, 4 and 5 was  $1.33 \pm 0.05 \text{ mg L}^{-1}$  across all sites. Therefore, the estimated steady state drain water discharge rates (Equation 3.1) derived using these average Br<sup>-</sup> concentrations, in experiment 1 and 2 were  $67.5 \pm 1 \text{ L s}^{-1}$  and  $126.7 \pm 3.6 \text{ L s}^{-1}$ , respectively.

### 3.3.5 Drain water velocity

Water velocity was estimated using the breakthrough concentration curves of the Rhodamine<sup>WT</sup> dye that was injected into the drain immediately after experiments concluded. The injection time was taken as time zero.

In experiment 1, the Rhodamine<sup>WT</sup> dye was released at site 1 (15 m) and three water samples were collected at sites 2 (40 m), 3 (65 m) and 4 (165 m). The estimated travel times from site 1 to sites 2, 3 and 4 were 127, 215 and 553 seconds respectively. The slope of the time (seconds) vs. distance (m) plot equates to the drain water velocity (Figure 3-7) which was 0.299 m s<sup>-1</sup>.



**Figure 3-7** Mean water velocity obtained from the slope of graph for both experiment 1 and 2. Travel time is determined using breakthrough concentrations of Rhodamine<sup>WT</sup> dye.

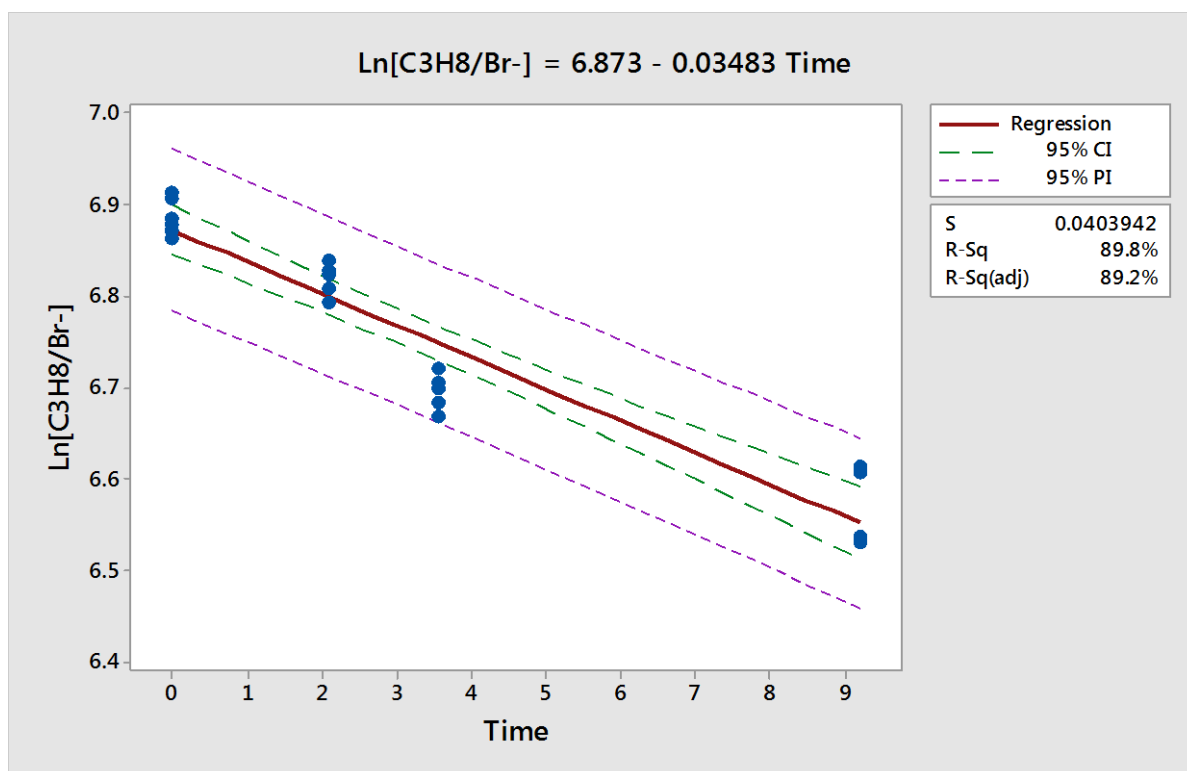
In experiment 2 three water samples were collected at sites 2 (40 m), 3 (65 m) and 4 (165 m) and a plot of time vs distance showed the drain water velocity was 0.337 m s<sup>-1</sup> (Figure 3-7).

### 3.3.6 Nitrous oxide transfer velocity ( $k_{N2O}$ ) measurement using propane ( $C_3H_8$ ) as a tracer gas

#### 3.3.6.1 Headspace equilibrium

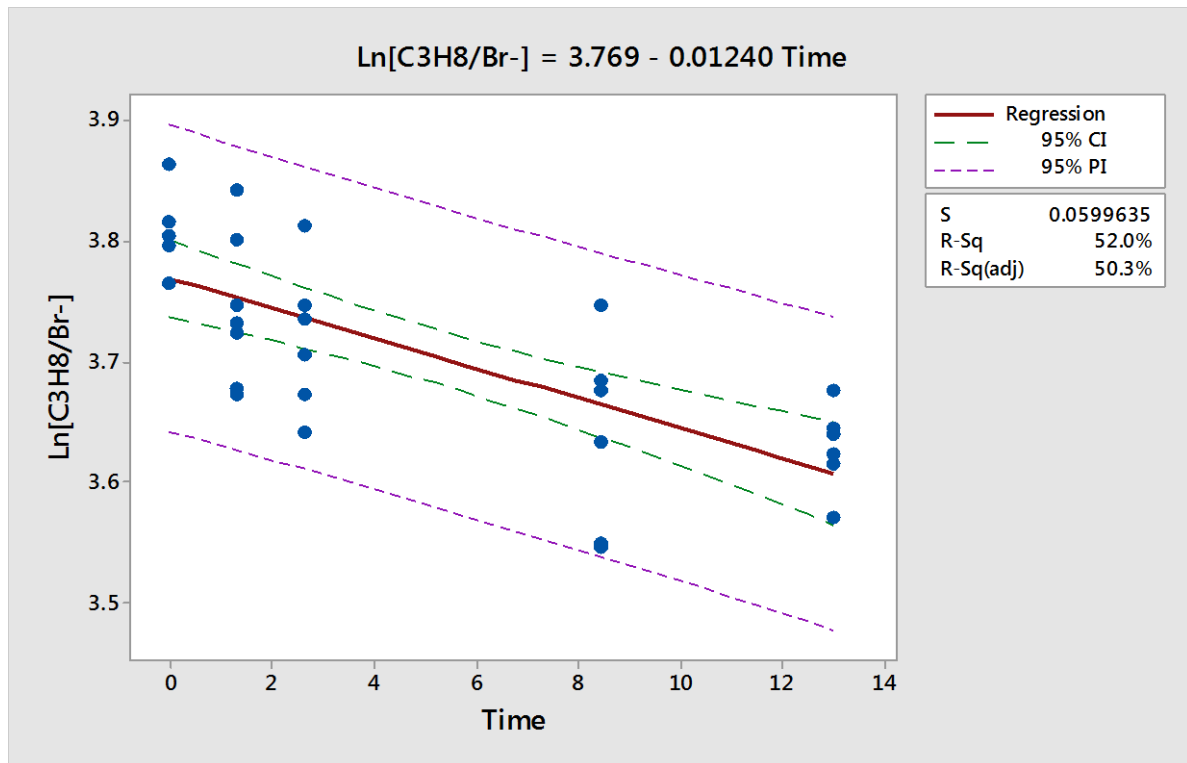
Determination of  $k_{N2O}$  values are based on the  $Br^-$  analyses data. The results of 3.3.4 showed uniform mixing of the tracer solutions at times 3 and 4 for experiment 1 and at times 3, 4 and 5 for experiment 2. Thus, the natural log data of dilution corrected  $C_3H_8$  concentrations ( $\ln [C_3H_8/Br^-]$ ) were used to determine  $k'_{N2O}$  come from times 3 and 4 for experiment 1 and times 3, 4 and 5 for experiment 2.

In experiment 1, at sampling times 3 and 4, a total of 24 water samples were collected. However, six gas samples were rejected due to insufficient vacuum within the sample bottles' headspace and so 18 of the samples were used to determine the  $C_3H_8$  transfer coefficient ( $k'_{C3H8}$ ). The calculated  $\ln [C_3H_8/Br^-]$  values were plotted according to equation 3.7, and the best-fit lines determined using Minitab® version 16. The slope of the best-fit line equates to the  $C_3H_8$  transfer coefficient ( $k'_{C3H8}$ );  $0.035 \text{ min}^{-1}$  (Figure 3-8).



**Figure 3-8** Experiment 1, results of the natural log of  $C_3H_8/Br^-$  over time. The data points are individual sample values. The area between the green lines represents the 95% confidence interval and the brown line is the best-fit line. The area between the purple lines represents the prediction interval, and the slope of the best-fit line is the propane transfer coefficient ( $k'_{C3H8}$ ).

In experiment 2, at sampling times 3, 4 and 5, a total of 45 water samples were collected. However, 15 gas samples were rejected due to insufficient headspace vacuum conditions within sample bottles and 30 of the samples were used for  $C_3H_8$  transfer coefficient ( $k'_{C_3H_8}$ ) analysis. Following the same procedure as in experiment 1, the calculated  $\ln [C_3H_8 / Br^-]$  values were plotted according to equation 3.7, and the best-fit line was determined using Minitab® version 16. The slope of the best-fit line was  $0.012 \text{ min}^{-1}$  which equates to the  $C_3H_8$  transfer coefficient ( $k'_{C_3H_8}$ ) (Figure 3-9).



**Figure 3-9** Experiment 2, results of the natural log of  $C_3H_8/Br^-$  over time. The data points are individual sample values. The area between the green lines represents the 95% confidence interval and the brown line is the best-fit line. The area between the purple lines represents the prediction interval. The slope of the best-fit line is the propane transfer coefficient ( $k'_{C_3H_8}$ ).

The obtained  $C_3H_8$  transfer coefficient ( $k'_{C_3H_8}$ ) values were used to estimate the  $N_2O$  transfer coefficients ( $k'_{N_2O}$ ) at each sampling site (Equation, 3.10). Then, the  $N_2O$  transfer velocities ( $k_{N_2O}$ ) within the drain, at each sampling site, for both experiments were estimated as described in section 3.2.8.1 and results are presented in Table 3.3.

**Table 3.3 Headspace N<sub>2</sub>O transfer velocity ( $k_{N_2O}$ ) calculations from experiment 1 (20/01/2015) and experiment 2 (12/08/2015).**

	Site	$k'_{C_3H_8}$ (min <sup>-1</sup> )	Sc <sub>C<sub>3</sub>H<sub>8</sub></sub>	Sc <sub>N<sub>2</sub>O</sub>	$k'_{N_2O}$ (min <sup>-1</sup> ) <i>Eqn 3.10</i>	$k_{2(N_2O)}$ (min <sup>-1</sup> ) <i>Eqn 3.11</i>	Depth (cm)	$k_{N_2O}$ (cm hr <sup>-1</sup> )	$K_{(N_2O)}$ (m day <sup>-1</sup> )
<b>Experiment 1</b>	1	0.035	1143	774	0.045	0.046	19.5	52.97	12.71
	2	0.035	1143	774	0.045	0.046	18.4	49.98	11.99
	3	0.035	1143	774	0.045	0.046	18.7	50.79	12.19
	4	0.035	1143	774	0.045	0.046	20.4	55.41	13.30
								<b>Mean</b>	<b>12.55</b>
								<b>Stdev</b>	<b>0.58</b>
<b>Experiment 2</b>	1	0.012	1399	950	0.015	0.016	32.8	30.50	7.32
	2	0.012	1399	950	0.015	0.016	31.3	29.10	6.99
	3	0.012	1399	950	0.015	0.016	29.6	27.51	6.61
	4	0.012	1399	950	0.015	0.016	35.5	33.01	7.92
	5	0.012	1399	950	0.015	0.016	37.6	34.97	8.39
								<b>Mean</b>	<b>7.44</b>
								<b>Stdev</b>	<b>0.72</b>

Stdev = Standard deviation

### 3.3.6.2 Floating chambers

In experiment 2, the  $C_3H_8$  flux from the water surface was also collected using floating chambers at sample sites 1, 3 and 5. The dissolved equilibrium  $C_3H_8$  concentration was estimated using equations 3.3 and 3.4. Then, the value of the  $C_3H_8$  transfer velocity ( $k_{C_3H_8}$ ) was determined using equation 3.13. The estimated  $k_{C_3H_8}$  was converted into  $k_{N_2O}$  using equation 3.14 and the  $k_{N_2O}$  values were normalized to a temperature of 20°C using equation 3.15 (Table 3.4).

**Table 3.4 Nitrous oxide transfer velocity ( $k_{N_2O}$ ) values derived from  $C_3H_8$  surface flux measurements**

Site	$C_3H_8$ Flux $\mu\text{mol m}^{-2} \text{ hr}^{-1}$	Equilibrated $C_3H_8$ $(\mu\text{mol m}^{-3})$	$k_{C_3H_8}$ $(\text{m hr}^{-1})$	$k_{N_2O}$ $(\text{m hr}^{-1})$	$K_{N_2O}$ $(\text{m day}^{-1})$
1	$10.31 \pm 0.83$	$46.71 \pm 1.13$	0.221	0.285	$6.84 \pm 0.94$
3	$8.45 \pm 0.21$	$34.94 \pm 1.70$	0.217	0.281	$6.83 \pm 0.35$
5	$7.26 \pm 0.22$	$30.52 \pm 0.79$	0.238	0.307	$7.38 \pm 0.17$

The average  $k_{N_2O}$  values for site 1, 3 and 5 using  $C_3H_8$  surface flux measurements (Table 3.4) were  $6.84 \pm 0.94$ ,  $6.83 \pm 0.35$  and  $7.38 \pm 0.17$ , respectively.

### 3.3.7 Nitrous oxide transfer velocity ( $k_{N_2O}$ ) measurement using the Wilcock (1982) transfer velocity model

Using the drain water velocity and depth data for each sampling site, Wilcock (1982) modelled (Equation 2.10) the reaeration transfer velocity for oxygen ( $k_{O_2}$ ). This was used to determine the  $k_{N_2O}$  (equation 3.16). Then, the  $k_{N_2O}$  values were normalized to a temperature of 20°C using equation 3.15 (Table 3.5).

**Table 3.5** N<sub>2</sub>O transfer velocity ( $k_{N2O}$ ) determined using the model of Wilcock (1982) for data from experiment 1 (20/01/2015) and experiment 2 (12/08/2015).

	Site	$k_{O2}$ (m day <sup>-1</sup> )	Sc <sub>O2</sub>	Sc <sub>N2O</sub>	$K_{(N2O)}$ (m day <sup>-1</sup> )
<b>Experiment 1</b>	1	21.27	678	774	19.49
	2	23.20	678	774	21.26
	3	22.65	678	774	20.76
	4	19.88	678	774	18.22
<b>Experiment 2</b>	1	8.97	832	950	8.75
	2	9.62	832	950	9.39
	3	10.46	832	950	10.21
	4	7.97	832	950	7.77
	5	7.30	832	950	7.13

The average  $k_{N2O}$  values using the Wilcock (1982) model (Table 3.5) for experiment 1 and 2 were  $19.93 \pm 1.37$  and  $8.65 \pm 1.23$ , respectively.

### 3.3.8 Direct $k_{N2O}$ measurement from floating chambers

In experiment 2, the N<sub>2</sub>O flux from the water surface was determined using floating chambers at sample sites 1, 3 and 5. The dissolved equilibrium N<sub>2</sub>O concentration was estimated using 3.3 and 3.4 equations. Then, the value of the N<sub>2</sub>O transfer velocity ( $k_{N2O}$ ) was determined using equation 2.5 and the  $k_{N2O}$  values were normalized to a temperature of 20°C using equation 3.15 (Table 3.6).

**Table 3.6** Nitrous oxide transfer velocity ( $k_{N2O}$ ) values derived from floating chamber N<sub>2</sub>O surface flux measurements.

Site	N <sub>2</sub> O-N Flux (µg m <sup>-2</sup> hr <sup>-1</sup> )	Equilibrated N <sub>2</sub> O-N (µg m <sup>-3</sup> )	$k_{N2O}$ (m hr <sup>-1</sup> )	$K_{N2O}$ (m day <sup>-1</sup> )
<b>1</b>	15.37 ± 1.53	94	0.211	3.93 ± 1.32
<b>3</b>	29.18 ± 2.58	119	0.215	5.88 ± 2.24
<b>5</b>	43.99 ± 4.44	126	0.284	8.38 ± 2.41

The average  $k_{N_2O}$  values for site 1, 3 and 5 using  $N_2O$  surface flux measurements (Table 3.6) were  $3.93 \pm 1.32$ ,  $5.88 \pm 2.24$  and  $8.38 \pm 2.41$ , respectively.

### 3.3.9 Comparisons of $N_2O$ transfer velocity ( $k_{N_2O}$ ) estimations

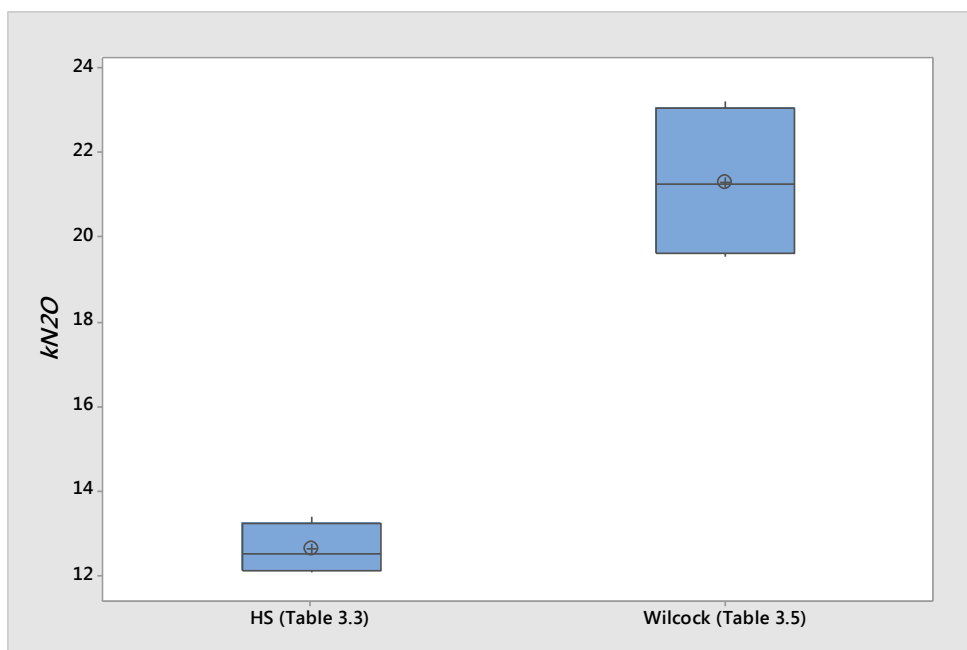
The summary of measured  $k_{N_2O}$  from headspace equilibrium method, floating chamber method, Wilcock (1982) model and the back calculated real time  $k_{N_2O}$  measurements from floating chambers are summarised in Table 3.7, Figure 3-10 and Figure 3-11 as follows.

**Table 3.7 Comparisons between experimentally observed  $k_{N_2O}$  ( $m\ day^{-1}$ ) using propane as a tracer gas at each site from headspace equilibrium (HS) and floating chamber (FC) methods, Wilcock (1982) model and  $N_2O$  flux measurements.**

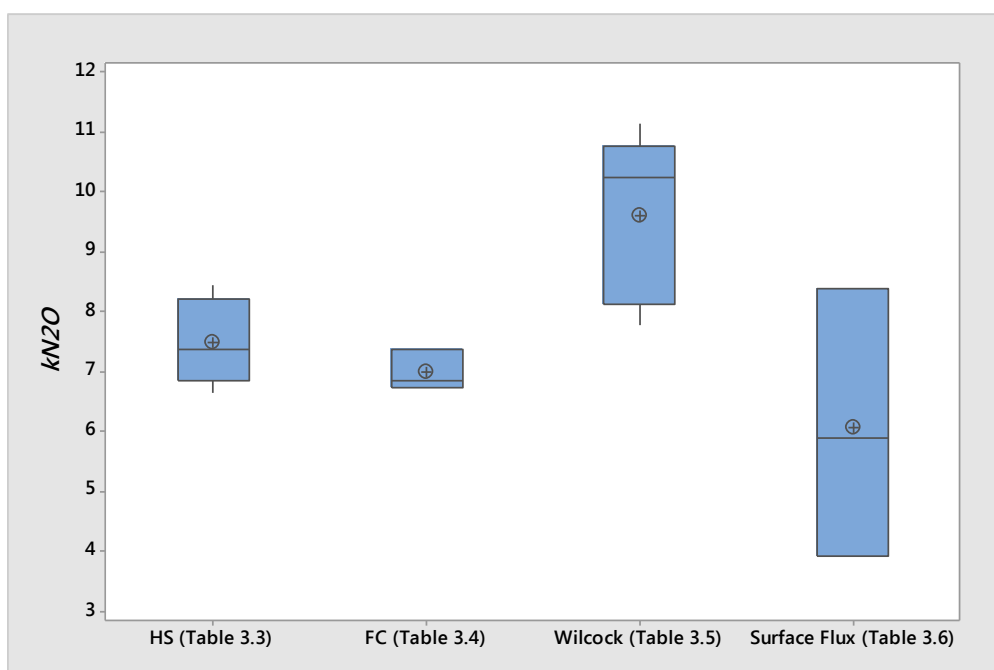
Experiment number and sampling sites		Obtained $k_{N_2O}$ value from Headspace method (HS) Floating Chambers (FC) and surface flux measurements.	$k_{N_2O}$ value from Wilcock, (1982) model.
<b>Exp #</b>  <b>1</b>	<b>Site 1</b>	12.80 (HS)*	19.49
	<b>Site 2</b>	12.07 (HS)*	21.26
	<b>Site 3</b>	12.27 (HS)*	20.76
	<b>Site 4</b>	13.39 (HS)*	18.22
<b>Exp #</b>  <b>2</b>	<b>Site 1</b>	7.37 (HS)*, 6.84 (FC)'	8.75
	<b>Site 2</b>	7.03 (HS)*	9.39
	<b>Site 3</b>	6.65 (HS)*, 6.83 (FC)'	10.21
	<b>Site 4</b>	7.97 (HS)*	7.77
	<b>Site 5</b>	8.44 (HS)*, 7.38 (FC)'	7.13
<b>Experiment 1 Average <math>\pm</math> Stdev</b>		<b>12.63 <math>\pm</math> 0.59</b>	<b>19.93 <math>\pm</math> 1.37</b>
<b>Experiment 2 Average <math>\pm</math> Stdev</b>		<b>7.49 <math>\pm</math> 0.72 (HS)* 6.98 <math>\pm</math> 0.34 (FC)'</b>	<b>8.65 <math>\pm</math> 1.23</b>
		<b>6.06 <math>\pm</math> 2.23 (SF)</b>	

(HS)\* Headspace equilibrium method, (FC)' Floating chamber method and (SF) surface flux measurements





**Figure 3-10** The interquartile box plot comparisons of experiment #1  $N_2O$  transfer velocity ( $k_{N_2O}$ ) determined using  $C_3H_8$  as a tracer gas between HS (Headspace equilibrium) and Wilcock (1982) model. The box represents the interquartile range (25% to 75%) for each group, the middle line is median, the symbol is the mean value and the upper (> 75%) and lower (< 25%) whiskers are the outside values of interquartile range.



**Figure 3-11** The interquartile box plot comparisons of experiment #2  $N_2O$  transfer velocity ( $k_{N_2O}$ ) determined using  $C_3H_8$  as a tracer gas between HS (Headspace equilibrium), Floating chambers (FC) and Wilcock (1982). The determined  $k_{N_2O}$  from surface flux is based on  $N_2O$  flux measured in chambers. The box represents the interquartile range (25% to 75%) for each group, the middle line is median, the symbol is the mean value of the group and the upper (> 75%) and lower whiskers (< 25%) are the outside values of the interquartile range.

## Chapter 4

### Nitrous Oxide Transfer Velocity ( $k_{N_2O}$ )

#### 4.1 Evaluation of methods used to establish $k_{N_2O}$

The agreement between the  $N_2O$  transfer velocity ( $k_{N_2O}$ ) derived from the observed data and the predictive equation as explained by Connor and Dobbins (1958), equation 2.9 as interpreted by Wilcock (1982) was generally poor (Table 3.7).

In order to probe the cause for the difference between the values obtained using the model and direct measurements, the O'Connor and Dobbins study data were evaluated. The reaeration coefficient of the O'Connor and Dobbins model is influenced by river velocity and depth (equation 2.9). They used a two –film theory for mass transfer processes that explains the rate of dissolved particles at a surface layer being replaced by the particles arising from turbulence motion. They verified the model using a laboratory experiment and found the rate of the surface renewal proportionally increased with the water oscillation speed. However, the total turbulence motion depends on both water speed and depth. In addition, in their experiment water was isotropic (uniform), but in natural environments, the shallow drains are more likely to be anisotropic (non-uniform).

O'Connor and Dobbins study generalized their model, applying it to a wide range of river depth data. The average depth for five out of their six studies ranged between 0.57 m to 6.10 m and re-aeration coefficients ranged from  $2.6 \text{ day}^{-1}$  to  $0.018 \text{ day}^{-1}$ . However, for the study that was performed in the Elk River, the depth was only 0.27 m and the observed and computed re-aeration coefficients were  $4.8$  and  $5.3 \text{ day}^{-1}$ , respectively. The Elk River depth is closer to the depth of the Rainey's Road drain in this study where the model computed  $k_{N_2O}$  values higher than the observed values.

Few past studies have doubted the accuracy of O'Connor and Dobbins model (equation 2.9) that measured the re-aeration coefficient in low depth rivers. The summary of those studies is as follows.

1. Wilcock (1984) used  $CHCl_3$  as a gas tracer to measure the re-aeration coefficient in five New Zealand (North Island) streams. Results of that study showed, the measured values were about 40% less than the estimated values.
2. Young and Huryn (1999) examined the reaeration coefficient in streams that were tributaries to the Taieri River in south east, New Zealand. They observed higher re-aeration

coefficients values than the empirically predicted values. These higher values were generally produced in small rivers/streams. Young & Huryn (1999) further stated that, removing higher values from the analysis, the O'Connor and Dobbins' model predicted values correlated with the measured values ( $r = 0.57$ ).

3. Grant and Skavronneck (1980) compared the tracer addition method and predictive equations for determination of stream reaeration coefficients on three small streams in Wisconsin, USA. According to their evaluation, the O'Connor and Dobbins equation produced mean absolute error of reaeration coefficients of between 50-232% against the measured values.

4. Robert et al. (2007), added  $C_3H_8$  with salt into the 0.06 to 0.09 m deep Walker Branch, Tennessee, as a tracer to measure the re-aeration coefficient. They found the re-aeration coefficients ranged between 5.52 - 14.42  $\text{day}^{-1}$  and they were higher than the O'Connor and Dobbins' model predicted.

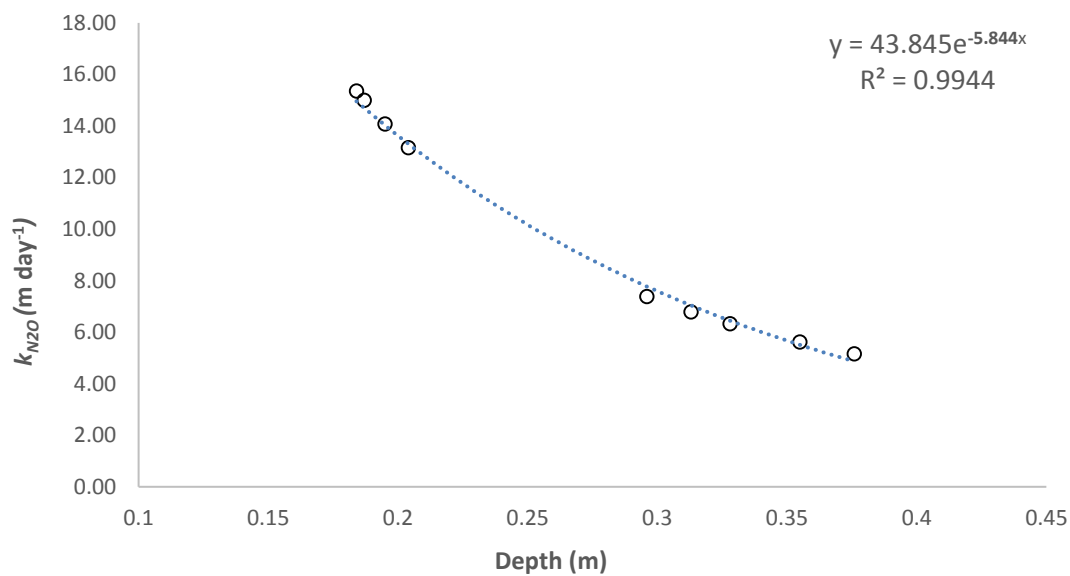
According to these previous studies and results of this current experiment, the gas transfer velocity in low depth ( $< 0.5$  m) rivers was unable to be measured accurately using O'Connor and Dobbins model. In spite of considering discrepancies, Wilcock (1982), introduced equation 2.10 to measure oxygen transfer velocities and suggested changing the multiplier in the equation with relevant river velocity and depth data. Specifically, Wilcock (1982) increased the drain depth coefficient to a value of 1.5, which is extremely sensitive to low depths. The model was validated with six separate gas studies that were carried out in the Tarawera River, between 1983 -1986. However, the depth of five of the six study sites were between 1-3.46 m and deeper than the sites of this study.

In the current study, the  $C_3H_8$  gas tracer enabled accurate and real time  $k_{N_2O}$  measurements. According to Wilcock (1982) model, oxygen transfer velocity ( $k_{O_2}$ ) is proportionally sensitive to drain depth. As a result, in experiment 1, with a slightly slower speed and shallower depth, the measured  $k_{N_2O}$  was 5.41  $\text{m day}^{-1}$  higher than in experiment 2 (Table 3.5). When comparing the measured  $k_{N_2O}$  using propane as a tracer gas, the Wilcock model overestimated  $k_{N_2O}$  by 59.5% and 18.3% in experiments 1 and 2, respectively. According to Wilcock's (1982) suggestion, we reduced the multiplier by 28% from 3.74 to 2.7 in equation 2.10. Using the modified equation, the estimated  $k_{N_2O}$  for experiment 1 was 15.1% greater than the mean measured and the estimated  $k_{N_2O}$  for experiment 2 was 14.6% less than the mean measured (Table 4.1).

**Table 4.1 Comparisons between  $k_{N2O}$  obtained at each site ( $\text{m day}^{-1}$ ) from equation 2.10 (multiplier 3.74), and the modified model (multiplier 2.70) measured  $k_{N2O}$ .**

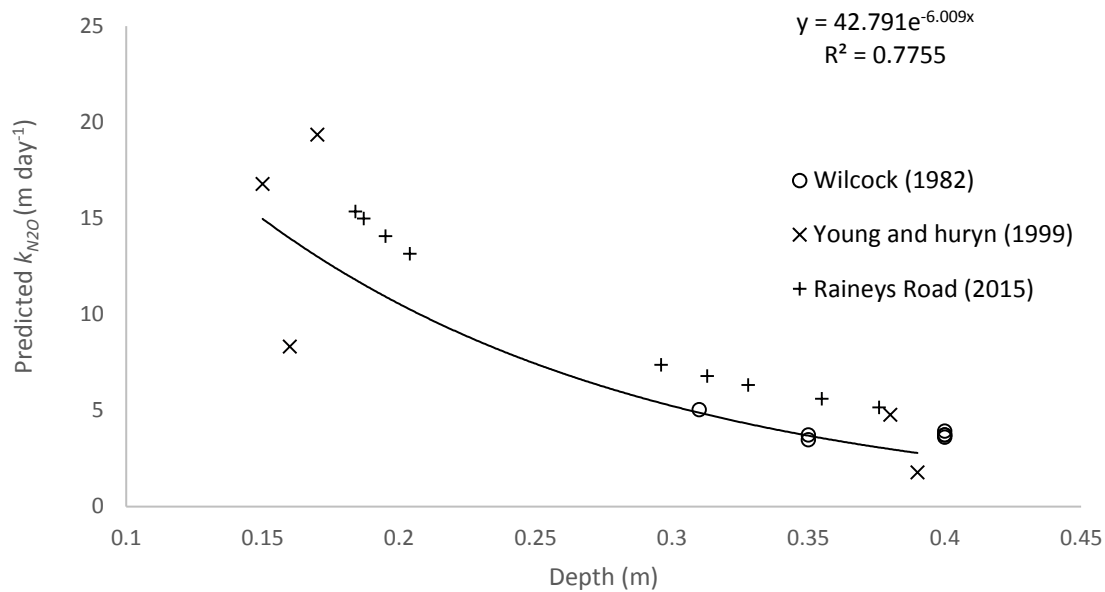
Experiment #	$k'_{N2O}$ ( $\text{m day}^{-1}$ ) using original multiplier <b>3.74</b>	$k'_{N2O}$ ( $\text{m day}^{-1}$ ) using modified multiplier <b>2.70</b>	Measured Total transfer Velocity ( $\text{m day}^{-1}$ )
1	$19.9 \pm 1.4$	$14.4 \pm 1.0$	$12.63 \pm 0.59$ (HS)*
2	$8.7 \pm 1.2$	$6.3 \pm 0.9$	$7.49 \pm 0.72$ (HS)*  $6.98 \pm 0.34$ (FC)'

In order to find the relationship between the modified (multiplier 2.7) model predicted  $k_{N2O}$  and the water depth, each sampling sites  $k_{N2O}$  values were plotted against site depth (Figure 4-1).



**Figure 4-1 The modified model predicted  $k_{N2O}$  ( $\text{m day}^{-1}$ ) in Rainey's Road sites depth (m).**

According to Figure 4-1, the value of  $k_{N2O}$  doubles with approximately 0.1 m of depth decrease. The modified model was applied to the low depth (<0.5 m) stream data of Wilcock (1984) and the data of Young and Huryn (1999), (Figure 4-2).



**Figure 4-2 The modified model predicted  $k_{N2O}$  (m day<sup>-1</sup>) vs. sampling site depth (m) of Wilcock (1984), Young, and Huryn (1999) and Rainey's Road drain (2015).**

The Figure 4-2 also shows  $k_{N2O}$  decreased with river depth at a similar rate;  $k_{N2O}$  halved when a drain depth increased by 0.1 m.

O'Connor and Dobbins developed their water turbulence transfer velocity model in a laboratory with a constant depth with different oscillation speeds. Their experiment was in an isotropic medium and they validated their model collecting the data from a wide range of river depths. Wilcock (1982) re-interpreted the O'Connor and Dobbins model, increasing the depth coefficient to 1.5, and suggested changing the multiplier according to the drain velocity and depth. The results of our experiments show that  $k_{N2O}$  decreases as depth increases. There is no single study that has measured  $k_{N2O}$  or  $k_{O2}$  against depth in small rivers. However, the trend with depth is incorporated into most of the energy dissipation models. Therefore, this study provides a nonlinear regression relationship between  $k$  and a gas escape coefficient as a function of the depth in shallow waters.

## 4.2 Gas transfer velocity in small rivers

The observed gas transfer velocities among the studies were highly variable and such variability in small rivers and streams occurred due to different hydro physical conditions. The studies have illustrated that high  $k$  values occur in small streams and they may be summarised as follows.

- A sensitivity analysis showed that  $k$  is dependent on the width to depth ratio. When water depth is shallower than 3 m, the variations in  $k$  are higher (Alin et al., 2011).
- Hydro-physical variations such as channel width, water velocity and depth in small streams result in highly variable  $k$  values (Alin et al., 2011).
- The average  $k$  values were 40% higher from small rivers compared to larger rivers (Wanninkhof R., 1990).
- The observed  $k$  values in small rivers and streams (< 100 m) have higher variability (1 to 71.1 cm h<sup>-1</sup>) than in larger rivers (1.2 to 44.5 cm h<sup>-1</sup>) (Alin et al., 2011).
- The wind effect on  $k$  values was considerably lower in small rivers. The estimated wind effect on  $k$  in large rivers and small rivers ranged from 0 to 5.2 cm h<sup>-1</sup> and 0 to 1.3 cm h<sup>-1</sup>, respectively (Rasera et al., 2008).
- Within the flowing water systems, effects of hydro physical parameters on  $k$  declined with stream order (Turner et al., 2015).

According to the above summary, hydro physical parameters of waters are the key drivers of  $k$  in small rivers and streams. In addition, exposure to the wind will also have significantly less effect in small streams with deep banks and sheltering plant canopies. The bed friction may have significant impact on  $k$ , but the majority of studies do not describe the drain waterbed characteristics.

Roughness / bed-friction of bottom surfaces of drains is a major factor that can alter the gas transfer velocity. Drains with stony, gravel bottom surfaces break the water flow and should result in higher  $k$  values than drains with smooth, clay bottom surfaces. Even though the Schmidt number coefficient is assigned to address bed friction (as 0.5 for rough surfaces and 0.66 for smooth surfaces), the variations among the bottom surfaces are large. Distributions of hydrological parameters overlapped to some extent between studied data. Therefore, to develop a more refined model to measure the  $k_{N2O}$  values in drains, a broader range of hydro physical measurements is needed.

### 4.3 Summary and suggestion for future research

The following key aspects were observed to control  $k_{N_2O}$  in two separate experiments within the drain study site.

- The tracer gas addition method provided more accurate and precise  $k_{N_2O}$  values than the Wilcock (1982) model predicted values.
- The results show that  $k_{N_2O}$  decreases as depth increases (Figure 4-1 and 4-2).
- A narrow and deeper drain system with low  $k_{N_2O}$  would result in lower  $N_2O$  emissions than wider and shallower drains with high  $k_{N_2O}$  values.
- According to Henry's law function, water temperature is inversely correlated with the volume of the gas dissolved. Therefore, in cold winter months, drain water  $k_{N_2O}$  is lower than the warmer summer months.

The following key areas have to be investigated in future studies.

- The two experiments performed are insufficient to establish clear trends in  $k_{N_2O}$  against drain depth. Therefore, further tracer gas addition studies are required in variable drain depths.
- The tracer gas has to be added over a longer time scale for drain water steady state sampling.

## Chapter 5

# Effect of Ammonium ( $\text{NH}_4^+\text{-N}$ ) on $\text{N}_2\text{O}$ emissions from an agricultural drain

### 5.1 Introduction

Agricultural drains are a significance source of  $\text{N}_2\text{O}$  emissions, but relatively little is known about  $\text{N}_2\text{O}$  production and indirect emissions from waterways. River studies indicate that  $\text{N}_2\text{O}$  emissions increase with N loading (Harrisons, 2003). It has been estimated that river networks are responsible for  $\sim 10\%$  of global anthropogenic  $\text{N}_2\text{O}$  emissions, but uncertainty is high (Beaulieu, 2011). Variable residence time, different N loading rates, numerous biota interactions and changes in hydro physical conditions within river systems contribute to this uncertainty.

Biological nitrification and denitrification mechanisms are the two main  $\text{N}_2\text{O}$  production pathways. Nitrification is an aerobic process in which ammonium ( $\text{NH}_4^+$ ) is oxidised to nitrite ( $\text{NO}_2^-$ ) and then nitrate ( $\text{NO}_3^-$ ). But denitrification is an anaerobic process in which  $\text{NO}_3^-$  is reduced to  $\text{N}_2\text{O}$  and ultimately  $\text{N}_2$ . Similarly,  $\text{NH}_4^+$  produced from organic matter decomposition in waters can be nitrified into  $\text{NO}_3^-$  and subsequently denitrified. Therefore, nitrification maybe a significance process contributing to indirect  $\text{N}_2\text{O}$  emissions from waterways. However, no studies have been performed within drains, streams or river systems to specifically examine the role of nitrification in  $\text{N}_2\text{O}$  emissions. Unlike soil systems, shallow and fast moving water within drain systems, tends to be oxygenated and well mixed. As a result, the effect of nitrification on  $\text{N}_2\text{O}$  emissions from agricultural drain systems remains to be investigated.

Experiments in this chapter tested the hypothesis that nitrification of  $\text{NH}_4^+\text{-N}$  would contribute to  $\text{N}_2\text{O}$  emissions in an agricultural drain. Similarly, the experiment provided an opportunity to both directly measure  $\text{N}_2\text{O}$  fluxes and estimate  $\text{N}_2\text{O}$  fluxes using the  $k_{\text{N}_2\text{O}}$  value that was determined in chapter four.



## 5.2 Methods

### 5.2.1 Mixed tracer solution

Prior to the  $^{15}\text{N}$  tracer addition experiment, a preliminary experiment was also performed. This evaluated  $\text{NH}_4^+$  and  $\text{NO}_3^-$  concentration changes in the drain, following the addition of an unlabelled  $\text{NH}_4^+$  pulse (05<sup>th</sup> June, 2015). The main  $^{15}\text{N}$  tracer addition experiment was performed on 12<sup>th</sup> August, 2015 (previously described in chapter 3 as experiment 2).

The preliminary experiment was performed to determine, if nitrification of ammonium ( $\text{NH}_4^+$ ) could be observed. A solution of  $\text{NH}_4^+$  was made up on site in an 80 L carboy with a conservative tracer, potassium bromide (KBr). The carboy solution comprised of: 500 g of ammonium sulphate  $(\text{NH}_4)_2\text{SO}_4$  and 800 g of KBr dissolved in 5 L of water inside the carboy. The carboy was then filled with stream water (75 L) and mixed well before being released into the drain using a Pegasus Alexi's peristaltic pump (Fondriest, CA, USA). The masses of added  $(\text{NH}_4)_2\text{SO}_4$  and  $\text{Br}^-$  were expected to increase both  $\text{NH}_4^+$  and  $\text{Br}^-$  concentrations in the drain by  $1 \text{ mg L}^{-1}$ , based on a solution release rate of  $17 \text{ mL s}^{-1}$ . The drain  $\text{NH}_4^+$  and  $\text{Br}^-$  background concentrations were  $< 0.1$  and  $0 \text{ mg L}^{-1}$ , respectively, and the estimated drain discharge volume was  $67.5 \text{ L s}^{-1}$ .

In experiment 2, the tracer solution comprised of 800 g of  $^{15}\text{N}$  enriched  $(\text{NH}_4)_2\text{SO}_4$  and 1.0 kg of KBr in an 80 L carboy. When experiment 2 was performed, the drain discharge volume was estimated at  $126.7 \text{ L s}^{-1}$ . The carboy solution was continuously released into the drain using the peristaltic pump at a rate of  $17 \text{ mL s}^{-1}$  while 99.9% pure propane ( $\text{C}_3\text{H}_8$ ) continued to purge the solution. The pump rate and injected solution concentrations were chosen to result in a  $^{15}\text{NH}_4^+$  enrichment of 3 atom % and a  $\text{Br}^-$  concentration of  $1 \text{ mg L}^{-1}$  approximately. Due to potential interferences of the visual tracer Rhodamine<sup>WT</sup> on the  $\text{NH}_4^+$  detection method (phenol, hypochlorite colorimetric method), Rhodamine<sup>WT</sup> was added in a separate dosing experiment, immediately after the final collection of water samples as noted below, in order to determine water speed.

### 5.2.2 Sampling time, stations and collection

In the preliminary experiment, water-sampling sites were positioned along the drain at 15, 40, 65 and 165 m from the tracer injection site (Figure 3-2). At each site, triplicate water samples were collected for determination of inorganic-N ( $\text{NH}_4^+$ -N and  $\text{NO}_3^-$ -N) and  $\text{Br}^-$  concentrations.

In the preliminary experiment, the sample site at 165 m had higher  $\text{NO}_3^-$  concentrations with lower  $\text{C}_3\text{H}_8$  concentrations. Thus, another sample site was added at 215 m in experiment 2 in order to increase the potential recovery of  $\text{NO}_3^-$ . Therefore, in experiment 2 sampling sites were positioned along the drain at 15, 40, 65, 165 and 215 m. At each site, triplicate water and gas samples were collected every 15 minutes, five times for 1.25 hours (15, 30, 45, 60 and 75 minutes) following commencement of tracer injection at time zero. Samples were collected for inorganic-N concentrations and their  $^{15}\text{N}$  enrichments ( $\text{NH}_4^+$  and  $\text{NO}_3^-$ ), dissolved  $\text{N}_2\text{O}$  (concentrations and  $^{15}\text{N}$  enrichments),  $\text{Br}^-$  concentrations, pH, and dissolved  $\text{C}_3\text{H}_8$  concentrations.

In experiment 2, the surface gas fluxes were also determined using floating chambers at sites located at 40, 65, and 215 m. The detailed description of floating chamber design, construction and gas sampling procedures were as previously reported in Clough et al., (2006). A 10 mL gas sample was extracted and injected into a pre-evacuated 6.0 mL Exetainer® (Labco Ltd, High Wycombe, UK). In addition, after 75 minutes, a further 15 mL gas sample was taken from each chamber and placed in a pre-evacuated 12.0 mL Exetainer for subsequent  $^{15}\text{N}_2\text{O}$  analysis. Ambient air samples were also taken to measure background  $\text{N}_2\text{O}$  concentrations. Prior to each gas sampling, the syringe was flushed with ambient air to prevent cross contamination between samples. Then, the sample vials were transported to the laboratory for  $\text{C}_3\text{H}_8$  and  $\text{N}_2\text{O}$  analysis using a GC (Section 3.2.7), and  $^{15}\text{N}_2\text{O}$  analyses using a trace gas analyser (TGII) connected to a continuous isotope ratio mass-spectrophotometer (IRMS). The detailed description of IRMS analyses can be found in the section 5.2.4.

### 5.2.3 Dissolved $\text{N}_2\text{O}$ measurements

The gas sampling procedures and determination of dissolved  $\text{N}_2\text{O}$  were as previously reported (Section 3.2.8). In experiment 2, the headspace gas was transferred to pre-evacuated 6.0 mL and 12.0 mL Exetainers for  $\text{N}_2\text{O}$  concentration and  $^{15}\text{N}$  enrichment analyses, respectively. Ambient air samples were also collected at each sampling. The same procedure, using 50 mL of distilled water was performed in the laboratory to act as a control.

#### 5.2.4 Gas sample analyses on GC and TGII-IRMS

Gas sample analysis methods for  $\text{N}_2\text{O}$  and  $\text{C}_3\text{H}_8$  samples were as previously described in section 3.2.7.

The 12 mL gas samples collected for  $^{15}\text{N}$  enrichment of  $\text{N}_2\text{O}$ , which were analysed using a trace gas analyser interfaced to an IRMS (TGII/IRMS; Sercon™, Crew, UK). The sample vials were placed on a Gilson auto sampler and flushed with ultra-high purity helium through a double – ended concentric needle. Since  $\text{N}_2\text{O}$  is condensable below  $-90^\circ\text{C}$ , the  $\text{N}_2\text{O}$  was removed by cryogenic trapping in liquid nitrogen. Prior to the sample injection into the separation column, elliptical stainless steel cryo-traps were lowered into liquid nitrogen ( $-196^\circ\text{C}$ ) concentrating the  $\text{N}_2\text{O}$ . The  $\text{CO}_2$  and water in the gas samples was scrubbed prior to this using  $\text{NaOH}$  (sodium hydroxide) and  $\text{Mg}(\text{ClO}_4)_2$  (magnesium perchlorate), respectively. Then the concentrated  $\text{N}_2\text{O}$  sample was passed through a GC capillary column, (Pora PLOT- Q) 30 m long and 0.32 mm diameter (J & W Scientific, CA, USA), that separated  $\text{N}_2\text{O}$  and  $\text{C}_3\text{H}_8$ . The recorded retention times for the  $\text{N}_2\text{O}$  and  $\text{C}_3\text{H}_8$  gasses were 540 and 585 seconds, respectively. To protect the IRMS source from  $\text{C}_3\text{H}_8$ , the analysis time was reduced to 575 seconds while the column elute was directed to exit at 570 seconds.

#### 5.2.5 Dissolved $\text{N}_2\text{O}$ and $\text{N}_2\text{O}$ flux calculation

Concentrations of dissolved gasses in the drain water were estimated according to equations 3.3 and 3.4. Equilibrium  $\text{N}_2\text{O}$  concentrations ( $\text{nmol L}^{-1}$ ) in the drain water were determined by taking the atmospheric  $\text{N}_2\text{O}$  partial pressure ( $3.29 \times 10^{-7}\text{atm}$ ) and the appropriate solubility coefficient for  $\text{N}_2\text{O}$  ( $\text{mol L}^{-1} \text{atm}^{-1}$ ) at the temperature of the sampled water (Weiss & Price, 1980). To compare the  $\text{N}_2\text{O}$ -N emissions, due to nitrification of  $\text{NH}_4^+$ , and to evaluate the  $\text{N}_2\text{O}:\text{NH}_4^+$  and  $\text{N}_2\text{O}:\text{NO}_3^-$  ratios, the dissolved  $\text{N}_2\text{O}$  concentrations were converted to units of  $\mu\text{g N}_2\text{O-N L}^{-1}$ .

The  $\text{N}_2\text{O}$ -N flux was estimated using floating chambers at drain sites 1, 3 and 5 according to the equation 3.12.

#### 5.2.6 Inorganic –N analysis

Inorganic-N, ( $\text{NH}_4^+\text{-N}$  and  $\text{NO}_3^-\text{-N}$ ) analyses were performed on an Alpkem FS - 3000 twin channel Flow Injection Analyser (FIA) (Alpkem, College station, TX, USA). Ammonium was analysed using a gas diffusion technique and  $\text{NO}_3^-$  -N was determined using cadmium reduction to nitrite ( $\text{NO}_2^-$ )

followed by colorimetric determination (SolÓRzano, 1969). Detection limits of the FIA were  $0.5 \mu\text{g mL}^{-1}$  for  $\text{NH}_4^+\text{-N}$  and  $0.1 \mu\text{g mL}^{-1}$  for  $\text{NO}_3^-\text{-N}$ . Therefore, low  $\text{NH}_4^+\text{-N}$  concentrations were reanalysed using a manual indo-phenol blue method. This reaction is based on there being  $\text{NH}_4^+$  or  $\text{NO}_3^-$  in alkaline solution and when 'phenate' is introduced, an indo-phenol blue colour is produced in the presence of an oxidising agent, such as hypochlorite. This method detects both  $\text{NH}_4^+$  and  $\text{NO}_3^-$  forms of N with a detection limit of  $0.2 \mu\text{g mL}^{-1}$ .

### 5.2.7 Plants, biofilms and sediments

Aquatic plant samples were cut from available sites and brought to the laboratory where they were gently washed with de-ionized water. Then samples were dried at  $40^\circ\text{C}$  for 72 h. The plant samples were then finely ground ( $< 200 \mu\text{m}$ ) and 4 mg of sample was then placed in a tin capsule for total N and  $^{15}\text{N}$  enrichment determination using an IRMS (EA-CF/IRMS; Sercon™, Crew, UK).

Biofilms were scraped from 'planted' ceramic tiles that had been present for  $> 100$  days before the experiment. The tiles were rinsed and scraped using a sterile spatula with the biofilms suspended in DI water in 30 mL plastic vials (Figure 5-1). Then the samples were filtered through glass filter papers and oven dried at  $35^\circ\text{C}$  for 48 hours. Dried bio-film material was carefully removed using a sterile spatula and placed in tin capsules for total N and  $^{15}\text{N}$  enrichment determination using an IRMS.

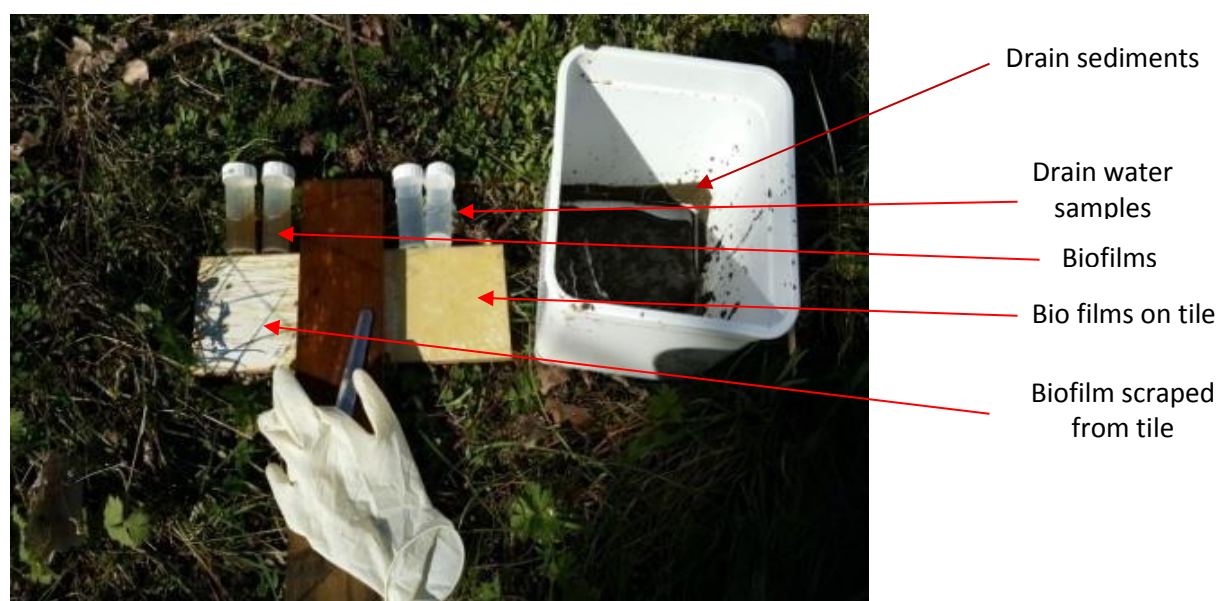


Figure 5-1 A photo of biofilm and soil sediment.

Sediment samples (0- 5 mm deep) were siphoned through plastic tube and transferred into plastic vials. The samples were then dried in an oven at 100°C for 24 hours. The dried sediment samples (50 mg) were placed in tin capsules and analysed for total N and  $^{15}\text{N}$  enrichment using an IRMS.

### 5.2.8 Plants, biofilms, sediments and diffusions analysis in EA-CF IRMS

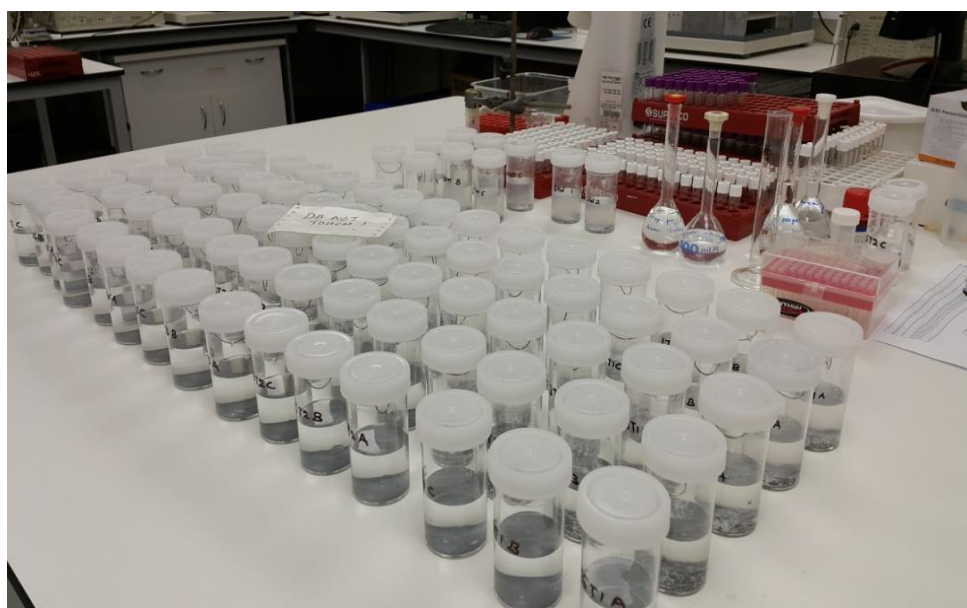
To determine  $^{15}\text{N}$  enrichment of the solid samples in the tin capsules, they were placed into the auto-sampler of an elemental analyser (Sercon™ GSL, Crew, UK). Reference standards were also prepared in the same way and placed at a rate of one reference for every eight samples with further 'check' standards, to assess precision and accuracy. The samples were combusted in the presence of oxygen at 1000°C, converting the N to a mixture of  $\text{N}_2$  and  $\text{NO}_x$ , which then passed through a packed copper reduction column at 600°C reducing any  $\text{NO}_x$  to  $\text{N}_2$ . Subsequently, the gas sample pulse flowed through  $\text{CO}_2$  and moisture scrubbers and a GC column (0.5 m, Carbo-sieve G, 60-80 a mesh column). Finally, the gas passed into the IRMS (EA-CF/IRMS; Sercon™, Crew, UK) where masses 28, 29 and 30 were determined and subsequently used to calculate atom percent  $^{15}\text{N}$  enrichment.



**Figure 5-2** A photo of aquatic plant species; (a) *Ranunculus sp.* (b) Aquatic grass – *Carex sp.* (c) Duckweed – *Lemnoideae sp.*

### 5.2.9 Inorganic-N $^{15}\text{N}$ enrichment

The collected 1 L water samples were analysed for  $^{15}\text{N}\text{-NH}_4^+$  and  $^{15}\text{N}\text{-NO}_3^-$  using the diffusion methodology described by Brooks et al. (1989). This involved suspending 7 mm Whatman GF/D filter paper discs, on stainless steel wire, in the headspace of sealed jars. Prior to this an aliquot (10  $\mu\text{L}$ ) of 2.5 M  $\text{KHSO}_4$  (potassium bisulphate) was pipetted on to the filter discs immediately. Analyses showed the majority of the water samples had  $\text{NH}_4^+\text{-N}$  concentrations  $< 1 \mu\text{g mL}^{-1}$ , thus to get a minimum of 50  $\mu\text{g N}$ , a 150 mL water sample was placed in the jar, prior to it being sealed, along with 0.2 mg of furnace dried  $\text{MgO}$  (magnesium oxide) and a glass bead. The  $\text{MgO}$  raised the solution pH, causing the  $\text{NH}_4^+\text{-N}$ :  $\text{NH}_3\text{-N}$  equilibrium to shift in favour of  $\text{NH}_3\text{-N}$  whereupon volatilisation of  $\text{NH}_3$  occurred, and the  $\text{NH}_3$  was trapped on the acidified paper disc. The samples were left for six days. The filter papers were then removed and dried in desiccators for 24 hours. The filter papers were placed in tin capsules for  $^{15}\text{N}\text{-NH}_4^+$  analysis. For  $^{15}\text{N}\text{-NO}_3^-$  analysis, 50 mL of sample solution, with  $\text{NH}_4^+$  already removed via diffusion was transferred to a clean 100 mL jar. Then, a new filter paper acidified with 10  $\mu\text{L}$  of 2.5 M  $\text{KHSO}_4$  was placed in the jar headspace before 0.4 Devarda's alloy and  $\text{MgO}$  were added. Devarda's alloy reduced the  $\text{NO}_3^-\text{-N}$  to  $\text{NH}_4^+\text{-N}$  which then volatilised as before. Care was taken to prevent the alkaline solution from contacting the acidified filter paper and neutralising the acid. The jars were again left for another six days at  $20^\circ\text{C}$ . Then, filter papers were removed, dried and transferred into tin capsules for IRMS analysis as before.



**Figure 5-3** Samples undergoing  $^{15}\text{N}$  diffusion to determine inorganic-N  $^{15}\text{N}$  enrichment.

### 5.2.10 <sup>15</sup>N enrichment and recovery calculations

The absolute abundance of <sup>15</sup>N measurements are commonly reported in terms of atom percent.

The atom % is determined as;

$$\text{Atom \% of } ^{15}\text{N} = [^{15}\text{N} / (^{15}\text{N} + ^{14}\text{N})] * 100 \quad 5.1$$

Compare to atmospheric <sup>15</sup>N abundance, the absolute ratio of <sup>15</sup>N enrichment in plant, soil sediment and gas samples was quite small and appeared on the third or fourth decimal place. Therefore, those samples' <sup>15</sup>N enrichment were transformed to parts per thousand and the values are reported as delta <sup>15</sup>N (δ<sup>15</sup>N). The δ<sup>15</sup>N transformation was performed as;

$$\delta^{15}\text{N} = [(^{15}\text{N} / ^{14}\text{N} \text{ sample}) / (^{15}\text{N} / ^{14}\text{N} \text{ air}) - 1] * 1000 \quad 5.2$$

where, <sup>15</sup>N/<sup>14</sup>N air is 0.0036765.

The percentage <sup>15</sup>N recovery was calculated using the following equation (Cabrera & Kissel, 1988).

$$^{15}\text{N recovered (\%)} = 100 \times \frac{p \times (c - b)}{f \times (a - b)} \quad 5.3$$

where,  $p$  = the moles of N in the sample;  $f$  = the moles of N in the applied <sup>15</sup>N enriched (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>;  $c$  = atom % of the recovered pool;  $a$  = atom % of the applied <sup>15</sup>N (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>; and  $b$  = atom % <sup>15</sup>N abundance of control.

### 5.2.11 Statistical analysis

Statistical analyses were performed using Minitab® version 16 (Minitab Inc, PA, USA), Sigma Plot 12.3 and Microsoft Excel, 2010. Means, standard deviations and standard errors were calculated for different measurements where appropriate. Analysis of variance was employed to test if means of variables differed between sampling sites. When differences occurred, two-way Student tests were performed to determine the significance of differences between means and the levels of significance.

Both NH<sub>4</sub><sup>+</sup>-N and NO<sub>3</sub><sup>-</sup>-N time series concentrations were fitted to a first order exponential function as follows (Lavagnini & Magno, 2007):

$$C_{(t)} = C_{(0)} e^{-kt} \quad 5.4$$

where,  $C$  is the concentration of  $\text{NH}_4^+\text{-N}$  and  $\text{NO}_3^-\text{-N}$  ( $\text{mg L}^{-1}$ ) at time  $t$  (minutes),  $C_0$  is the initial concentration at site 1, and  $k$  is the degradation constant (per minute). Values of the half-life ( $t^{1/2}$ ) were calculated as;

$$t^{1/2} = \ln(0.5) / -k \quad 5.5$$

where,  $t^{1/2}$  is the half-life (minutes), and  $k$  is the degradation constant (per minute).

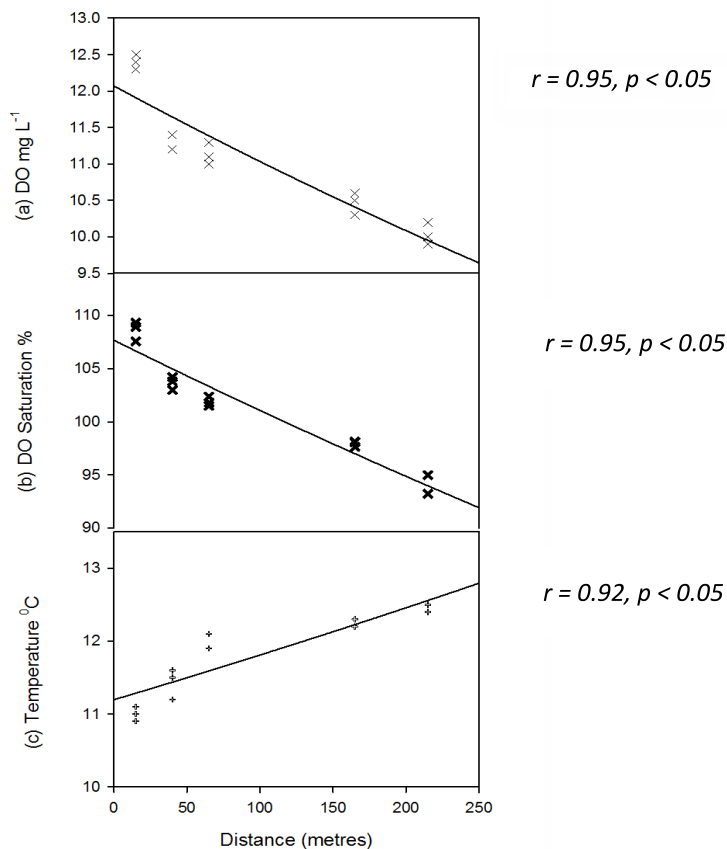


## 5.3 Results

Complete mixing of tracer in the drain occurred 45 minutes after the tracer solution injection commenced (section 3.3.4). Therefore, the data used to assess drain water hydro-physical, biological and chemical transformations are taken from sampling times 3 (45 minutes), 4 (60 minutes) and 5 (75 minutes) only.

### 5.3.1 Dissolved oxygen (DO) and water temperature

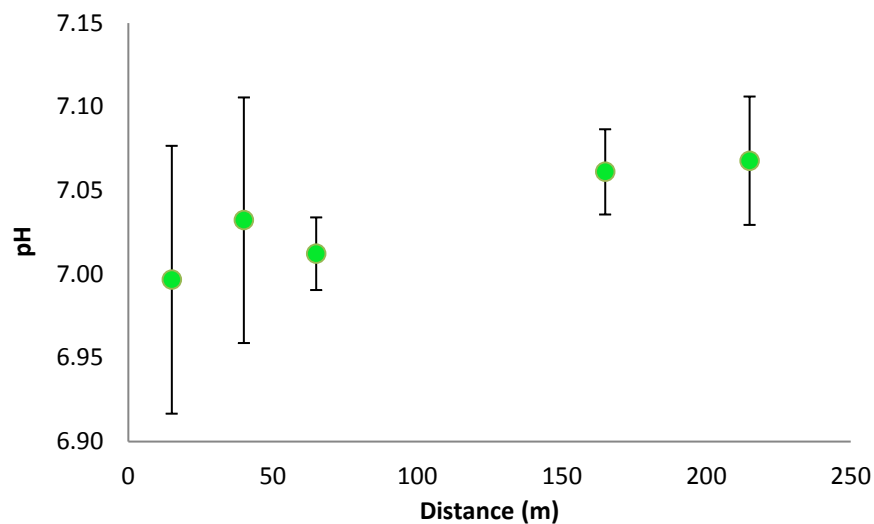
Before the tracer solution injection, the average drain water dissolved oxygen (DO) concentration was relatively high  $12.0 \pm 0.1$  ( $\pm$  stdev)  $\text{mg L}^{-1}$  which equated to  $109.9 \pm 0.7\%$  saturation. However, following tracer solution addition, DO declined with increasing distance ( $p < 0.05$ ). The DO averaged  $12.4 \pm 0.1$   $\text{mg L}^{-1}$  ( $108.9 \pm 1.8\%$ ) at site 1 and gradually decreased to  $10.1 \pm 0.2$   $\text{mg L}^{-1}$  ( $94.97 \pm 1.3\%$ ) at site 5 (Figure 4.4). In contrast, the average water temperature increased with distance ( $p < 0.05$ ) averaging  $11.0 \pm 0.1^\circ\text{C}$  at site 1 and increasing to  $12.4 \pm 0.1^\circ\text{C}$  at site 5 (Figure 5-4).



**Figure 5-4** Change in (a) dissolved oxygen (DO) concentrations, (b) DO saturation and (c) water temperature over distance. Each data point denotes a single measurement at 10 cm depth ( $n = 15$ ).

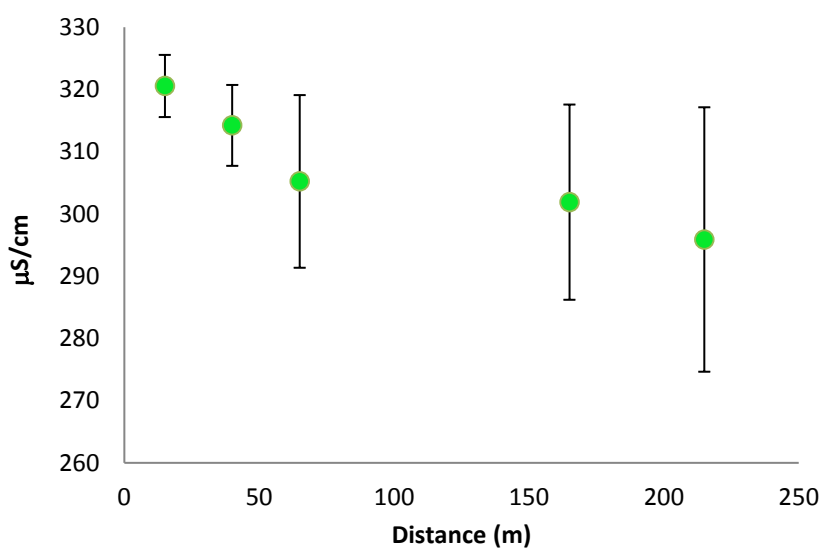
### 5.3.2 Drain water pH and electrical conductivity

There was a trend for pH to increase with distance following tracer injection, but this was not statistically significant ( $p > 0.05$ ). The drain water pH averaged  $6.99 \pm 0.08$  at site 1 and  $7.07 \pm 0.04$  ( $\pm$  stdev) at site 5 when averaged across sample times 3 to 5 (Figure 5-5).



**Figure 5-5** Change in water pH over distance. Data points are means,  $n=9$  (3 samples X 3 times) and error bars are  $\pm$  Stdev.

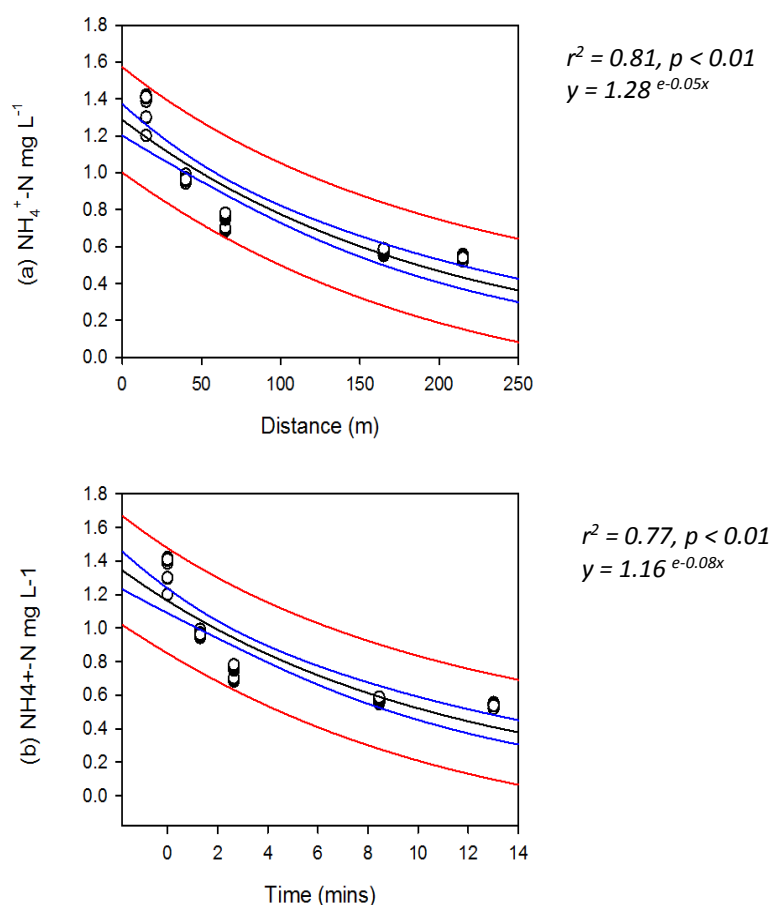
There was a trend for electrical conductivity (EC) to decrease with distance after tracer solution injection, although this was not statistically significant ( $p > 0.05$ ). The drain water EC averaged  $321 \pm 5$  at site1 and  $296 \pm 21$  ( $\pm$  stdev) at site 5, when averaged across sample times 3 to 5 (Figure 5-6).



**Figure 5-6** Drain water EC over distance. Data points are means,  $n=9$  (3 samples X 3 sampling times) and error bars are  $\pm$  Stdev.

### 5.3.3 Distribution of $\text{NH}_4^+\text{-N}$

Before the tracer solution was added, there was no detectable  $\text{NH}_4^+\text{-N}$  in the drain. Following tracer solution injection, the average drain water  $\text{NH}_4^+\text{-N}$  concentration immediately increased to an average of ( $\pm$  stdev)  $1.36 \pm 0.08 \text{ mg L}^{-1}$  and then declined over distance and time to  $0.54 \pm 0.01 \text{ mg L}^{-1}$  ( $p < 0.01$ ).

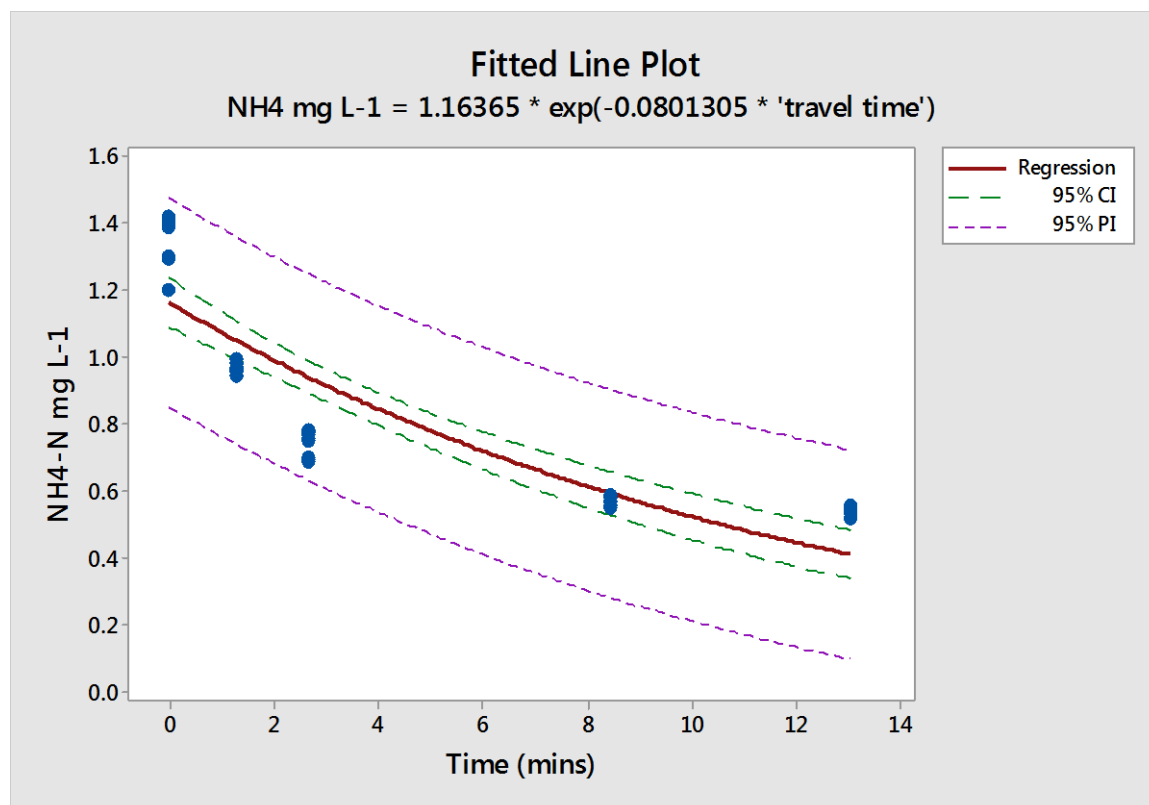


**Figure 5-7** Drain water  $\text{NH}_4^+\text{-N}$  concentration versus distance (a) and time (b). The best-fit exponential regression lines are black, the 95% confidence intervals are between blue lines and predicted intervals are between red lines. Each data point denotes a single sample measurement ( $n = 45$ ).

The mean  $\text{NH}_4^+\text{-N}$  concentrations were highest at site 1 ( $1.34 \pm 0.07 \text{ mg L}^{-1}$ ;  $\pm$  stdev) and lowest at site 5 ( $0.54 \pm 0.01 \text{ mg L}^{-1}$ ). Ammonium -N concentrations decayed exponentially with both distance and time with regression analysis explaining 81 and 77% of the variations in  $\text{NH}_4^+\text{-N}$  concentration, respectively (Figure 5-7).

### 5.3.4 Half-life of $\text{NH}_4^+\text{-N}$

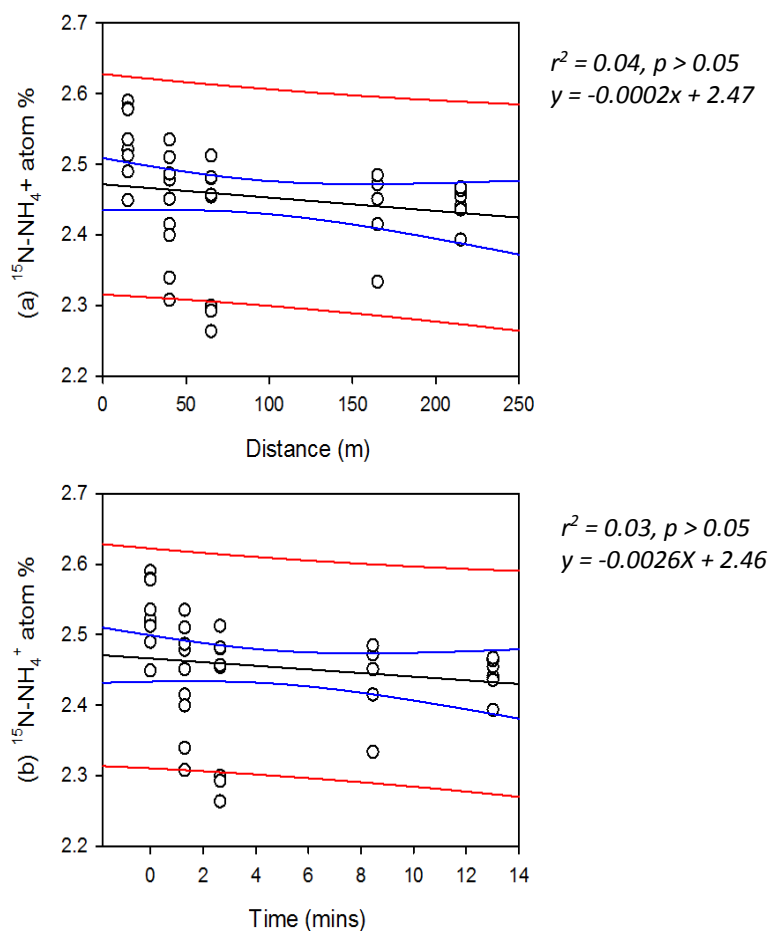
A fitted first order exponential decay function was fitted using Minitab, version 17 to determine the half-life of  $\text{NH}_4^+\text{-N}$ . Using equation 4.6 (section 4.2.11) and the degradation constant of the best-fit line (Figure 5-8), the half-life of  $\text{NH}_4^+\text{-N}$  was estimated to be  $8.62 \pm 0.26$  ( $\pm$  stdev) minutes, equating to a distance of  $141.9 \pm 36.8$  m based on the drain water velocity of  $126.7 \pm 3.6 \text{ L s}^{-1}$  (Section 3.3.4).



**Figure 5-8** Drain water  $\text{NH}_4^+\text{-N}$  concentration versus time. The brown line is the best-fit exponential curve ( $r^2 = 1.0$ ). The brown line is the best-fit line ( $r^2 = 1$ ), the area between the green lines represents the 95% confidence interval and the area between purple lines represents the prediction interval.

### 5.3.5 $^{15}\text{N-NH}_4^+$ atom percentage

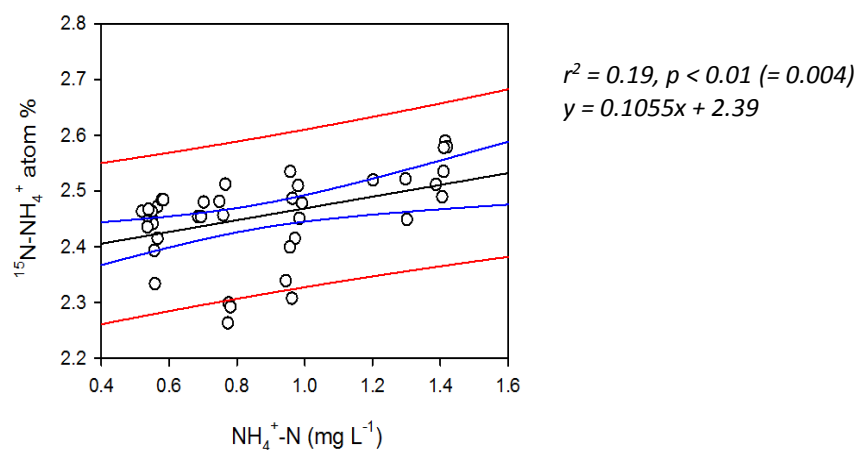
Linear regression analysis was performed on the  $^{15}\text{N-NH}_4^+$  enrichment over distance and time (Figure 5-9). The variation in the  $^{15}\text{N}$  enrichment of  $\text{NH}_4^+$  was not significant ( $p > 0.05$ ), and poorly explained by regression against distance or time,  $r^2$  values of 0.04 and 0.03, respectively.



**Figure 5-9** Drain water  $^{15}\text{N-NH}_4^+$  atom % versus distance (a) and time (b). The black line is the best-fit regression curve, 95% confidence intervals are between blue lines and predicted intervals are between red lines. Each data point denotes a single sample measurement ( $n = 42$ ).

### 5.3.6 $\text{NH}_4^+\text{-N}$ concentration versus $^{15}\text{N}\text{-NH}_4^+$ atom %

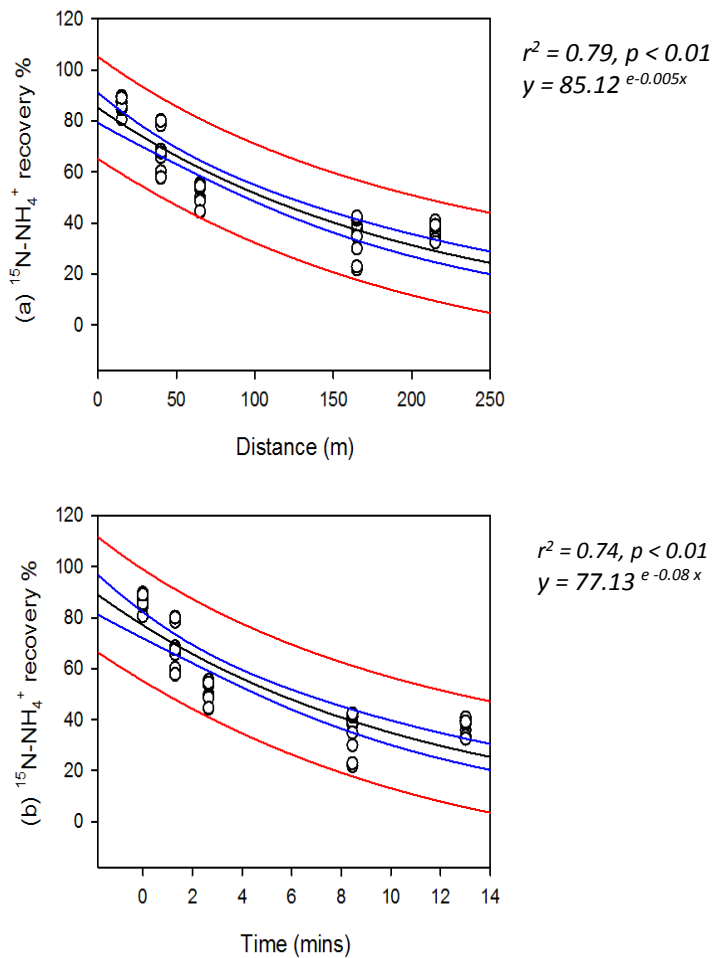
Linear regression analysis of  $\text{NH}_4^+\text{-N}$  concentration versus  $^{15}\text{N}\text{-NH}_4^+$  atom % (Figure 5-10) was poor with an  $r^2$  values of 0.19.



**Figure 5-10** Drain water  $\text{NH}_4^+\text{-N}$  concentration versus  $^{15}\text{N}\text{-NH}_4^+$  atom %. The black line is the best-fit regression curve, 95% confidence intervals are between blue lines and predicted intervals are between red lines. Each data point denotes a single sample measurement ( $n = 42$ ).

### 5.3.7 $^{15}\text{N-NH}_4^+$ recovery

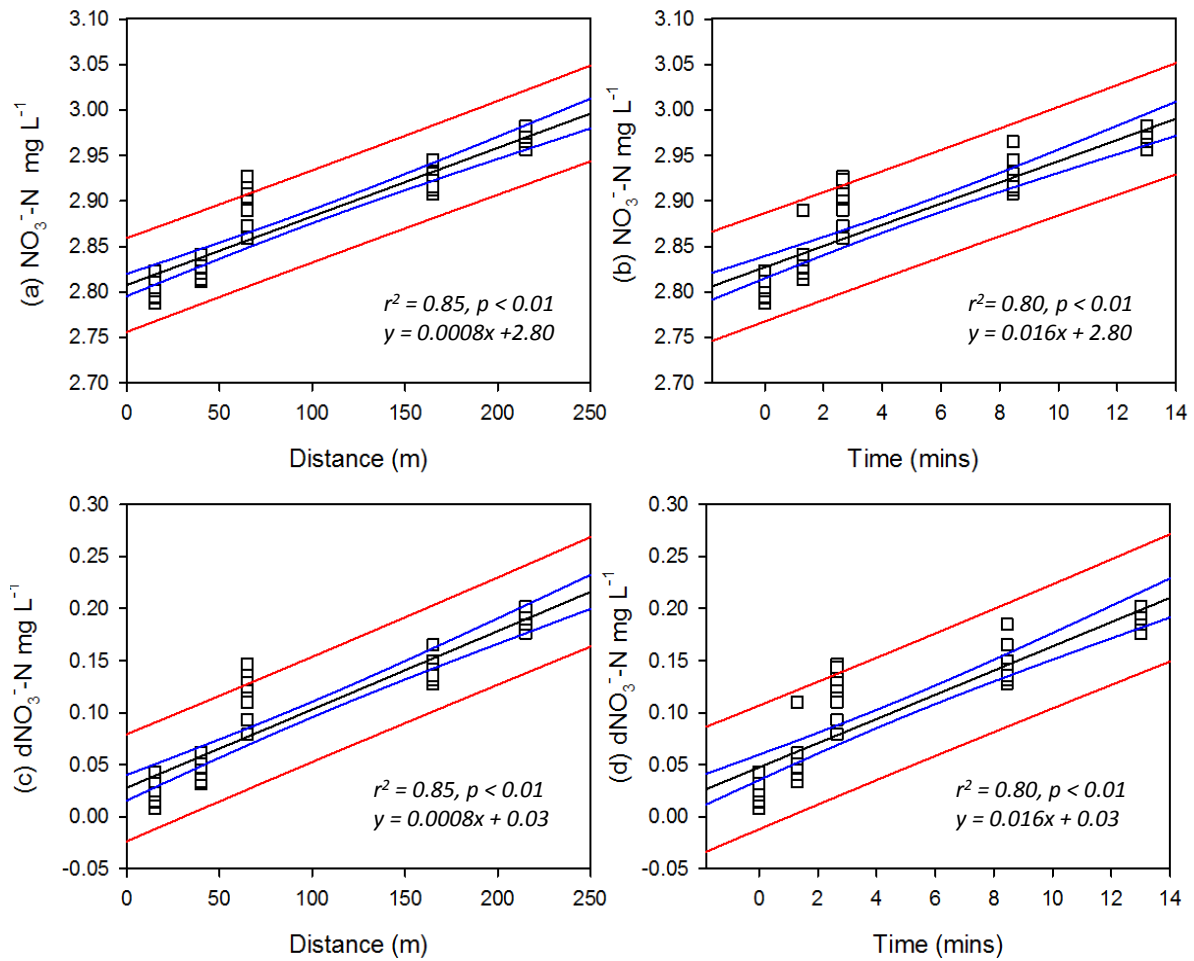
Recovery of  $^{15}\text{N}$  injected as  $^{15}\text{N-NH}_4^+$  declined exponentially over both distance and time. The  $^{15}\text{N-NH}_4^+$  recovery averaged  $86.3 \pm 2.9\%$  ( $\pm$  stdev) at site 1 and declined to  $37.8 \pm 4.1\%$  at site 5. The variation in  $^{15}\text{N}$  recovery as  $^{15}\text{N-NH}_4^+$  was significant ( $p < 0.01$ ), and well explained by changes in distance or time with  $r^2$  values of 0.79 and 0.74, respectively (Figure 5-11).



**Figure 5-11** Drain water  $^{15}\text{N-NH}_4^+$  recovery versus distance (a) and time (b). The black line is the best-fit regression curve, 95% confidence intervals are between blue lines and predicted intervals are between red lines. Each data point denotes a single sample measurement ( $n = 42$ ).

### 5.3.8 Distribution of $\text{NO}_3^-$ -N

Before the tracer solution injection, the average drain water  $\text{NO}_3^-$ -N concentration was  $2.78 \pm 0.12 \text{ mg L}^{-1}$  at all sampling sites. After the tracer solution injection,  $\text{NO}_3^-$ -N concentrations increased to  $2.96 \pm 0.01 \text{ mg L}^{-1}$  ( $\pm \text{stdev}$ ) at site 5.



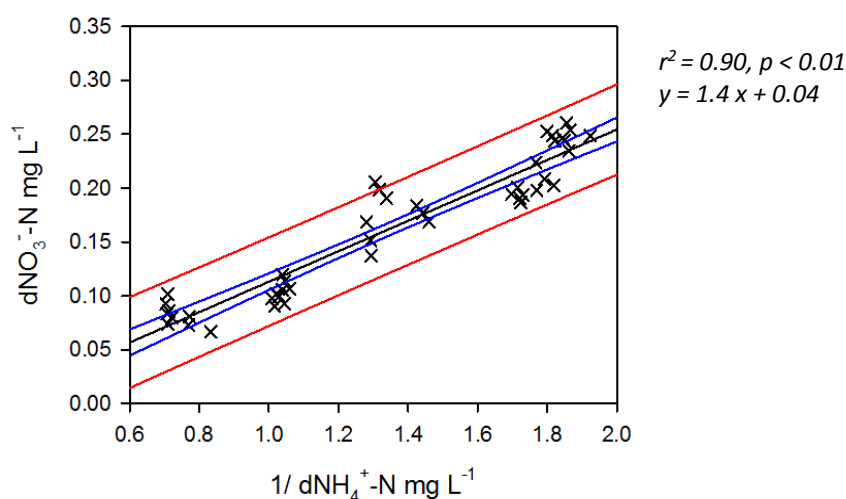
**Figure 5-12** Drain water  $\text{NO}_3^-$ -N concentration versus distance (a) and time (b) and the net change of  $\text{NO}_3^-$ -N concentrations ( $d\text{NO}_3^-$ -N) versus distance (c) and time (d). Black lines are the best-fit regression lines, the area between blue lines is 95% confidence interval and the area between red lines is predicted interval. Each data point denotes a single sample measurement ( $n = 45$ ).



The increase in drain water  $\text{NO}_3^-$ -N concentration was well explained by distance and time with  $r^2$  values of 0.85 and 0.80, respectively. Changes in the difference between the pre-existing  $\text{NO}_3^-$ -N concentration and the post equilibrium concentration ( $\text{dNO}_3^-$ -N) were also well explained by distance and time with by  $r^2$  values of 0.85 and 0.80, respectively (Figure 5-12).

### 5.3.9 $\text{NH}_4^+$ -N concentration versus $\text{NO}_3^-$ -N concentration

The increase in  $\text{dNO}_3^-$ -N was proportional to the  $\text{dNH}_4^+$ -N. A regression of  $1/\text{dNH}_4^+$ -N versus  $\text{dNO}_3^-$ -N concentrations showed a strong linear relationship with an  $r^2$  value of 0.90 (Figure 5-13).



**Figure 5-13** The  $1/\text{dNH}_4^+$ -N concentration versus the  $\text{dNO}_3^-$ -N concentration ( $n = 45$ ). The black line is the best-fit linear regression curve, the area between blue lines is 95% confidence intervals and the area between red lines is the predicted interval. Each data point denotes a single sample measurement ( $n = 42$ ).

### 5.3.10 Doubling time of $\text{NO}_3^-$ -N

Minitab 17 was used to obtain the best-fit line for  $\text{dNO}_3^-$ -N over time (Figure 5-14). A fitted first order exponential function was employed to measure the doubling time of  $\text{dNO}_3^-$ -N. Using equation 4.6 (section 4.2.11) and the constant of the best-fit line (Figure 5.14) the doubling time of  $\text{dNO}_3^-$ -N was estimated to be  $12.63 \pm 0.63$  ( $\pm$  stdev) minutes equating to a distance of  $192.8 \pm 9.6$  m based on drain water velocity.

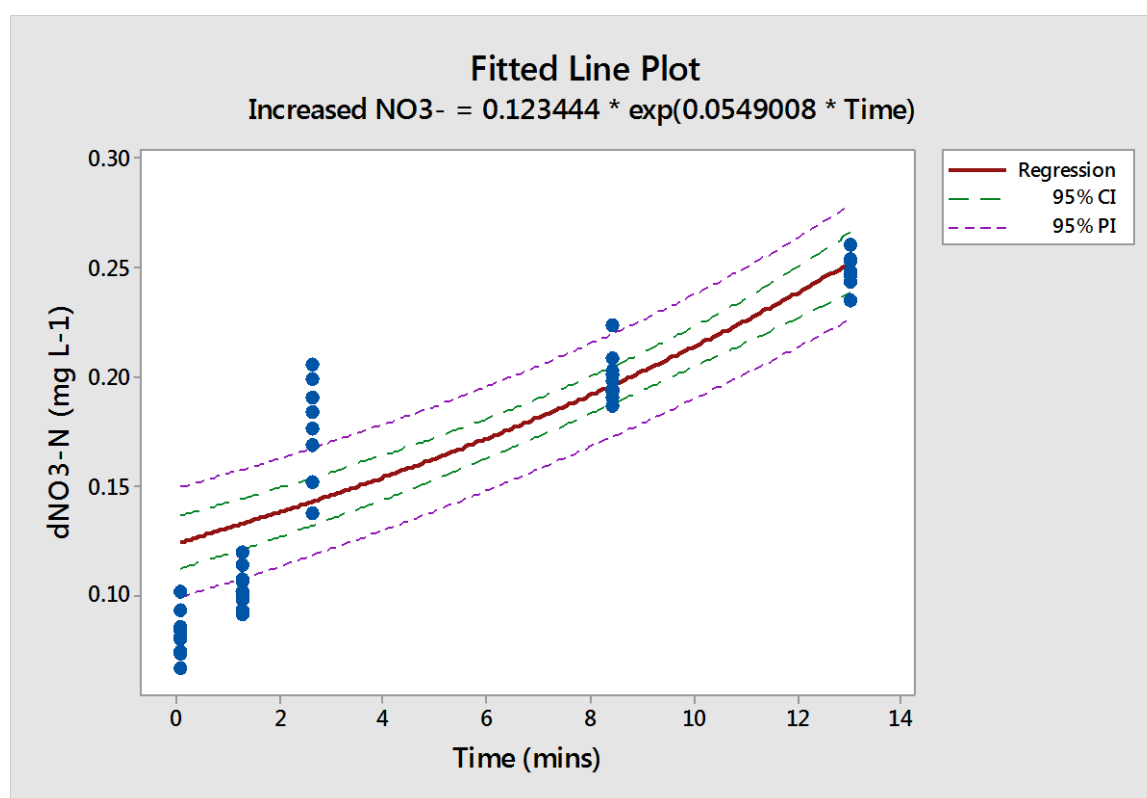
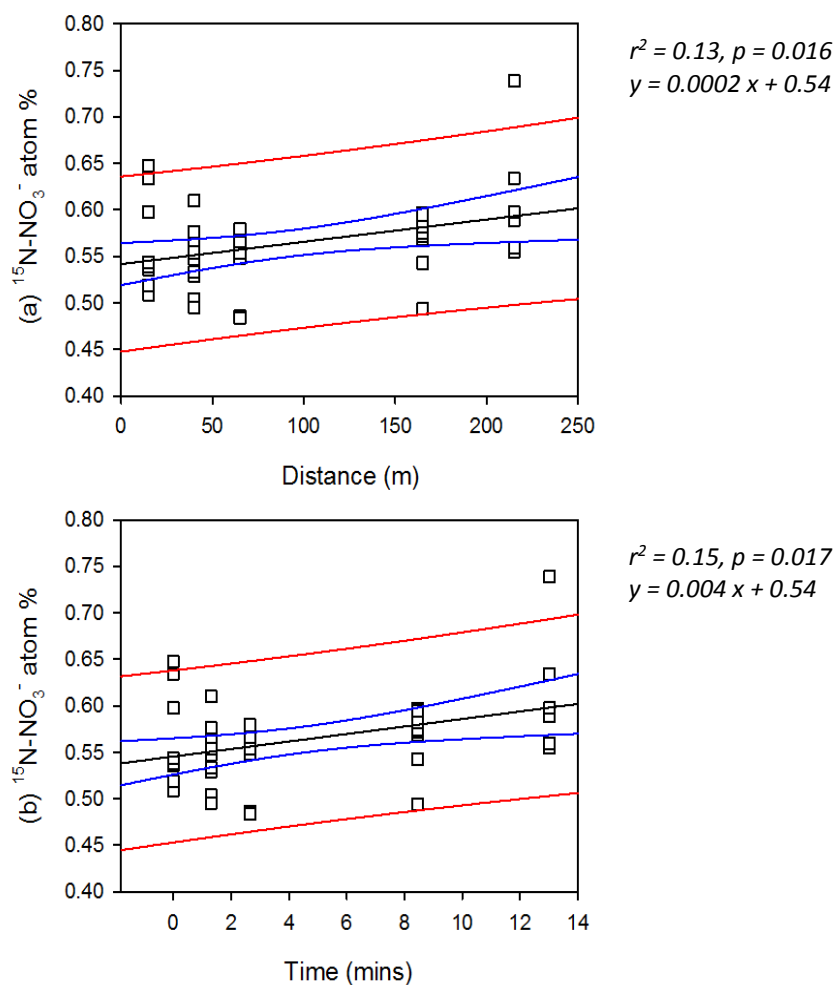


Figure 5-14 Drain water  $\text{dNO}_3^-$ -N concentration versus time. The brown line is the best-fit exponential curve ( $r^2 = 1.0$ ). The brown line is the best-fit line ( $r^2 = 1$ ), the area between the green lines represents the 95% confidence interval and the area between purple lines represents the prediction interval.

### 5.3.11 $^{15}\text{N}\text{-NO}_3^-$ atom percentage.

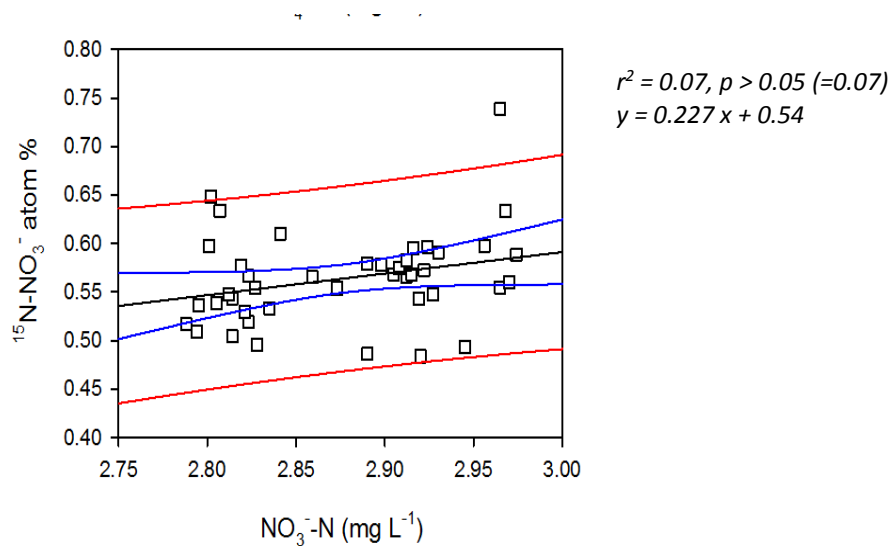
Regression analysis of the  $^{15}\text{N}$  enrichment of  $\text{NO}_3^-$  versus distance or time showed small increases in the  $^{15}\text{N}$  enrichment of  $\text{NO}_3^-$  over distance or time (Figure 5-15) and the relative variation in  $^{15}\text{N}$  enrichment of  $\text{NO}_3^-$  for distance or time were 13% and 15%, respectively.



**Figure 5-15 Drain water  $^{15}\text{N}\text{-NO}_3^-$  atom % versus distance (a) and time (b). The black lines are the best-fit linear regression lines, the area between blue lines is 95% confidence interval and the area between red lines is the predicted interval. Each data point denotes a single sample measurement ( $n = 42$ ).**

### 5.3.12 $\text{NO}_3^-$ -N concentration versus $^{15}\text{N}$ - $\text{NO}_3^-$ -N atom %

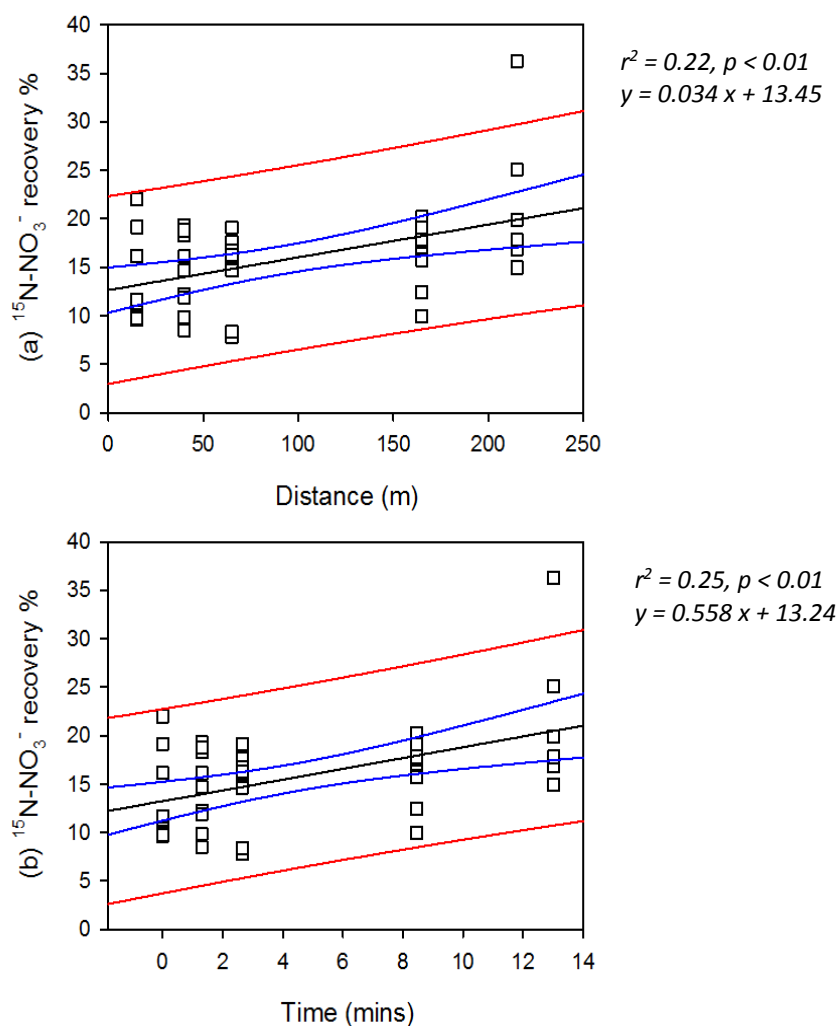
Linear regression analysis of  $^{15}\text{N}$ -  $\text{NO}_3^-$ -atom % versus  $\text{NO}_3^-$ -N concentration (Figure 5-16). The variation in the  $^{15}\text{N}$  enrichment of  $\text{NO}_3^-$  was not significant ( $r^2 = 0.07$ ).



**Figure 5-16** Drain water  $^{15}\text{N}$ -  $\text{NO}_3^-$  atom % versus  $\text{NO}_3^-$ -N concentration. The black lines are the best-fit linear regression lines, the area between blue lines is 95% confidence interval and the area between red lines is the predicted interval. Each data point denotes a single sample measurement ( $n = 42$ ).

### 5.3.13 $^{15}\text{N}\text{-NO}_3^-$ recovery

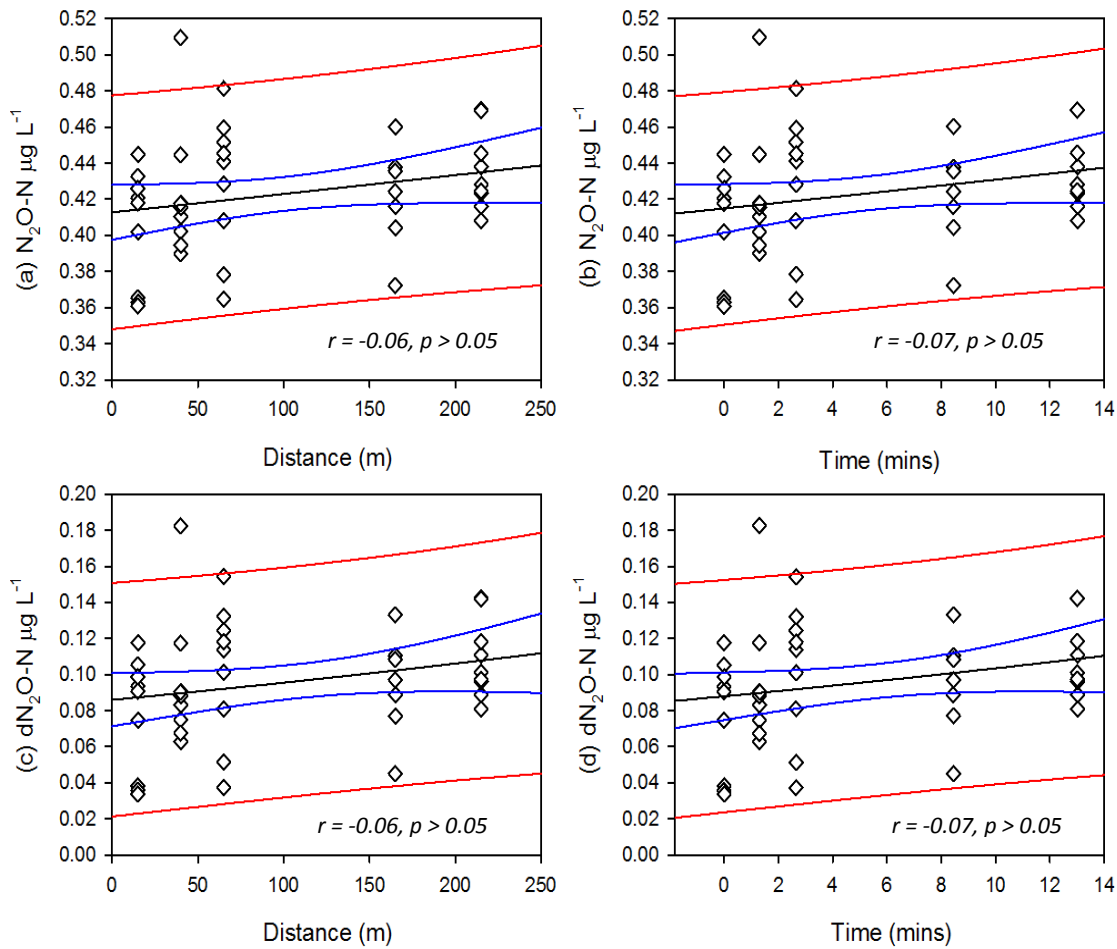
In contrast to  $^{15}\text{N}\text{-NH}_4^+$  recovery, the recovery of  $^{15}\text{N}$  as  $\text{NO}_3^-$  increased with distance ( $r^2 = 0.22$ ) and time ( $r^2 = 0.25$ ). The average  $^{15}\text{N}$  recovered as  $\text{NO}_3^-$  at site 1 was  $13.9 \pm 4.6\%$  and this increased to  $26.4 \pm 10.4\%$  ( $\pm$  stdev) at site 5.



**Figure 5-17** Drain water  $^{15}\text{N}\text{-NO}_3^-$  recovery versus distance (a) and time (b). The black lines are the best-fit linear regression lines, the area between blue lines is 95% confidence interval and the area between red lines is the predicted interval. Each data point denotes a single sample measurement (n = 42).

### 5.3.14 Distribution of N<sub>2</sub>O-N

Before the tracer solution injection, the drain water N<sub>2</sub>O saturation ranged from 110 to 115% (0.35-0.37 µg N<sub>2</sub>O-N L<sup>-1</sup>; 12.4 -12.9 nmol L<sup>-1</sup>) across all sampling sites. Following tracer solution addition, drain water N<sub>2</sub>O saturation increased and averaged 129% (0.42 µg N<sub>2</sub>O-N L<sup>-1</sup>; 14.6 nmol L<sup>-1</sup>) with the highest saturation equating to 156 % (0.51 µg N<sub>2</sub>O-N L<sup>-1</sup>; 17.6 nmol L<sup>-1</sup>).

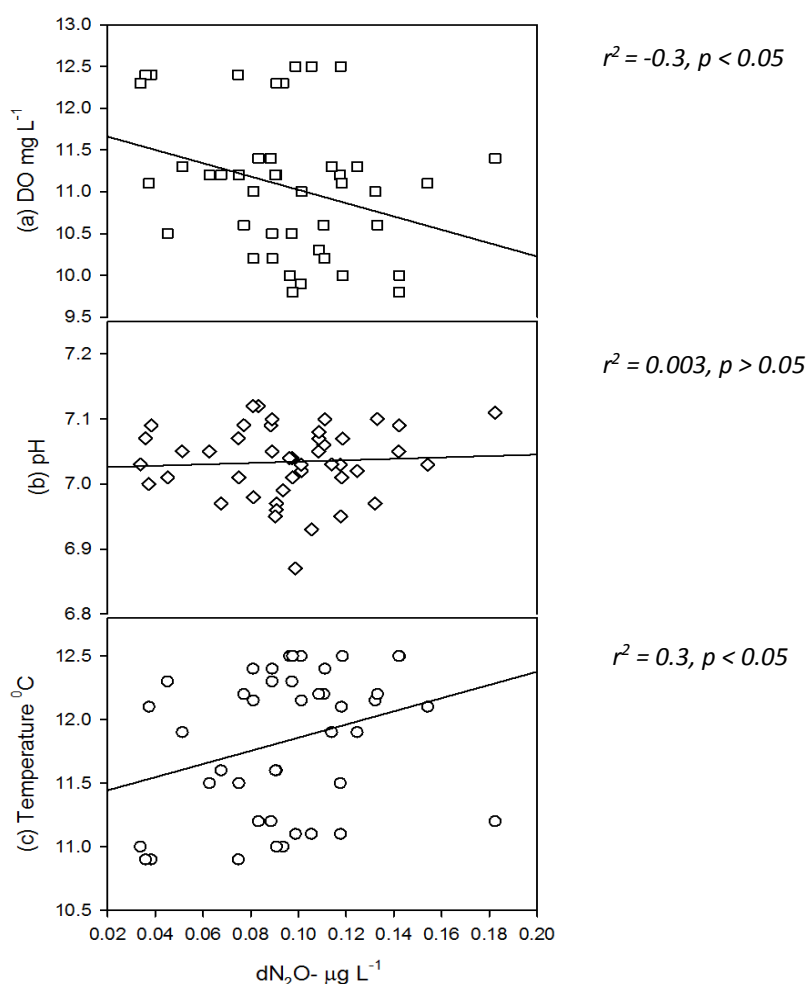


**Figure 5-18** Drain water N<sub>2</sub>O-N concentration versus distance (a) and time (b) and the net change of N<sub>2</sub>O-N concentrations (dN<sub>2</sub>O-N) versus distance (c) and time (d). The best-fit exponential regression lines are black, the area between blue lines is 95% confidence interval and the area between red lines is the predicted interval. Each data point denotes a single sample measurement (n = 39).

There was no statistically significant relationship ( $p > 0.05$ ) between drain water  $\text{N}_2\text{O}$ -N concentrations and either distance or time with  $r^2$  values of 0.06 and 0.07, respectively (Figure 5-18). When calculating the difference between pre-existing  $\text{N}_2\text{O}$ -N concentrations and the new equilibrium concentrations ( $d\text{N}_2\text{O}$ -N) across distance and time, no significant relationship was observed distance or time with  $r^2$  values of 0.06 and 0.07, respectively.

### 5.3.15 Effect of DO, pH and temperature on $\text{N}_2\text{O}$ production

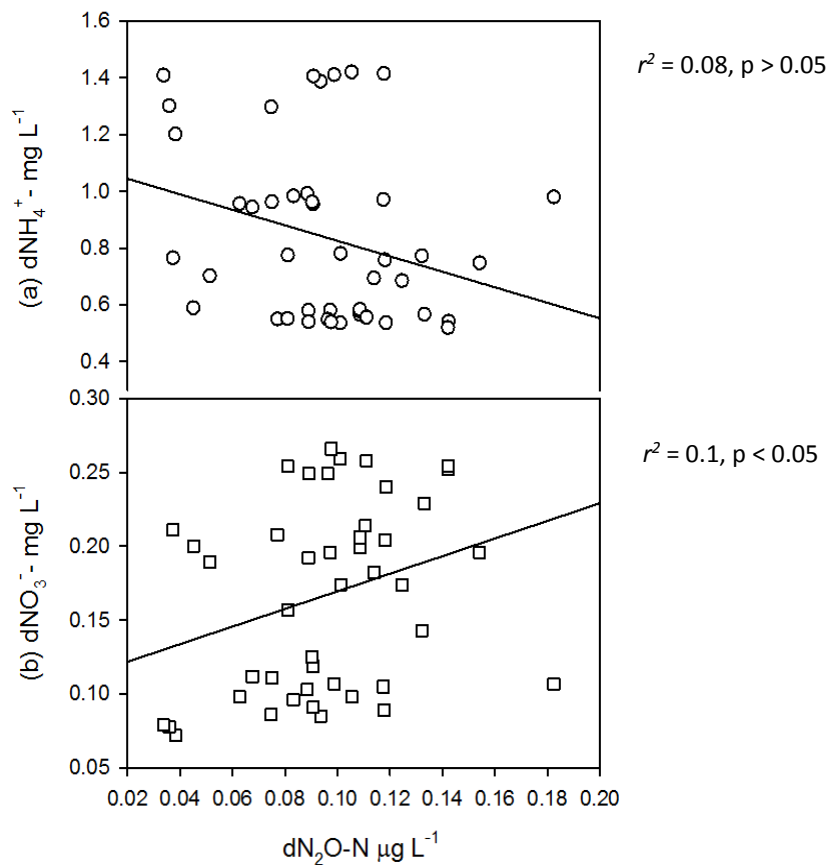
Regression analyses were performed on drain water DO, pH and water temperature versus dissolved  $\text{N}_2\text{O}$  concentrations (Figure 5-19). The drain water  $\text{N}_2\text{O}$  concentrations showed a weak negative relationship with drain water DO ( $r^2 = -0.3$ ,  $p < 0.05$ ). There was no relationship between the dissolved  $\text{N}_2\text{O}$  concentration and water pH ( $r^2 = 0.003$ ,  $p > 0.05$ ). In contrast, drain water  $\text{N}_2\text{O}$  concentration showed a weak positive relationship with water temperature ( $r^2 = 0.3$ ,  $p < 0.05$ ).



**Figure 5-19** Change in  $\text{N}_2\text{O}$ -N concentrations versus (a) DO, (b) pH and (c) water temperature. The performed trend lines represent linear regressions ( $n = 45$ ).

### 5.3.16 Inorganic-N ( $\text{NH}_4^+\text{-N}$ & $\text{NO}_3^-\text{-N}$ ) versus $\text{N}_2\text{O}$ production

Regression analysis was performed to assess the impact of  $\text{dNH}_4^+\text{-N}$  or  $\text{dNO}_3^-\text{-N}$  on  $\text{dN}_2\text{O-N}$  (Figure, 5-20). The drain water  $\text{dN}_2\text{O-N}$  concentration had a weak, negative relationship to  $\text{dNH}_4^+\text{-N}$  concentration ( $r^2 = 0.08$ ). In contrast,  $\text{dN}_2\text{O-N}$  concentration had a weak, but positive relationship with  $\text{dNO}_3^-\text{-N}$  concentrations ( $r^2 = 0.10$ ).

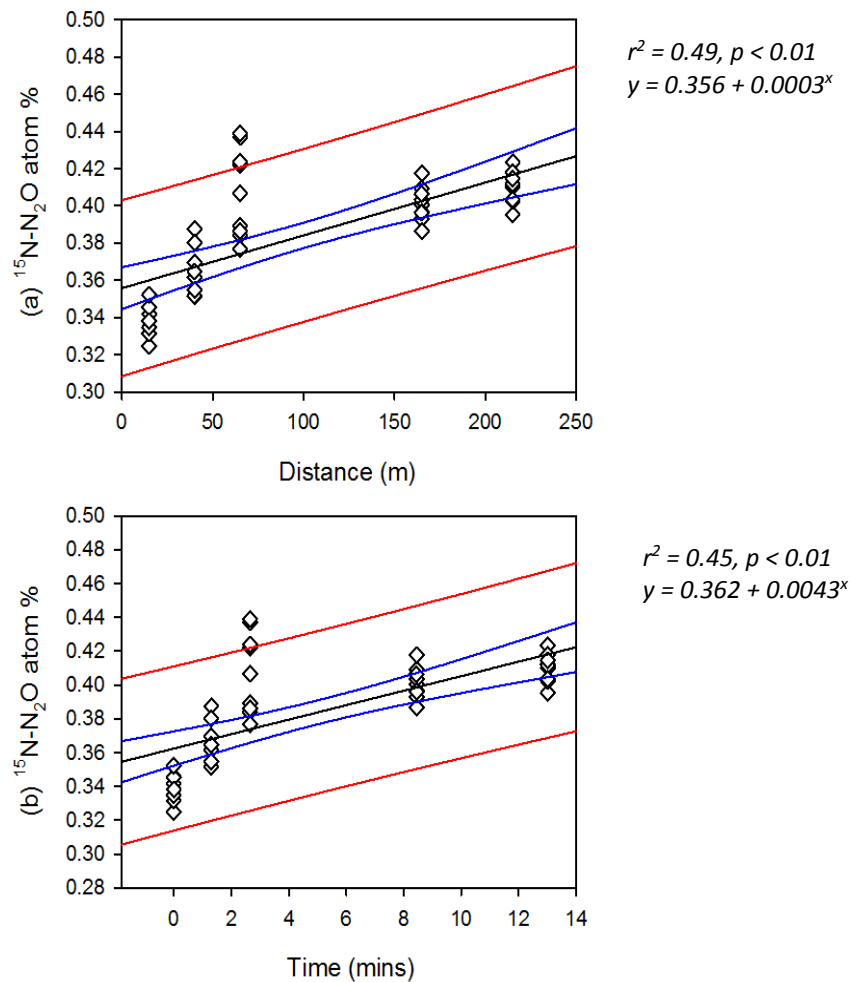


**Figure 5-20** The drain water  $\text{dN}_2\text{O-N}$  changes versus (a)  $\text{NH}_4^+\text{-N}$  concentration and (b)  $\text{dNO}_3^-\text{-N}$  concentrations. The trend lines are simple linear regressions ( $n = 45$ ).



### 5.3.17 $^{15}\text{N}\text{-N}_2\text{O}$ atom %

The  $^{15}\text{N}$  enrichment of the  $\text{N}_2\text{O}$  increased linearly over distance and time (Figure 5-21). The variation in  $\text{N}_2\text{O}$  atom percentage between sampling sites was significant ( $p < 0.05$ ) and the variation in  $\text{N}_2\text{O}$  atom % was explained by distance or time,  $r^2 = 49\%$  and  $45\%$ , respectively.



**Figure 5-21** Drain water  $^{15}\text{N}\text{-N}_2\text{O}$  atom % versus distance (a) and time (b). The black line are the best-fit regression lines, the area between blue lines are 95% confidence interval and the area between red lines are predicted interval. Each data point denotes a single sample measurement ( $n = 39$ ).

### 5.3.18 $\text{NH}_4^+\text{-N}$ & $\text{NO}_3^-\text{-N}$ atom % vs versus $\text{N}_2\text{O}$ atom %

Regression analysis was performed to assess the relationships between  $^{15}\text{N}$  enriched  $\text{NH}_4^+$ ,  $\text{NO}_3^-$  and  $\text{N}_2\text{O}$  atom % (Figure 5-22). The drain water  $\text{NH}_4^+$  atom % was not strongly related to  $\text{NO}_3^-$  atom % ( $r^2 = 0.34\%$ ;  $p > 0.05$ ). However,  $\text{N}_2\text{O}$  atom % was lower when  $\text{NH}_4^+$  atom % was higher ( $r^2 = 29$ ;  $p < 0.05$ ).

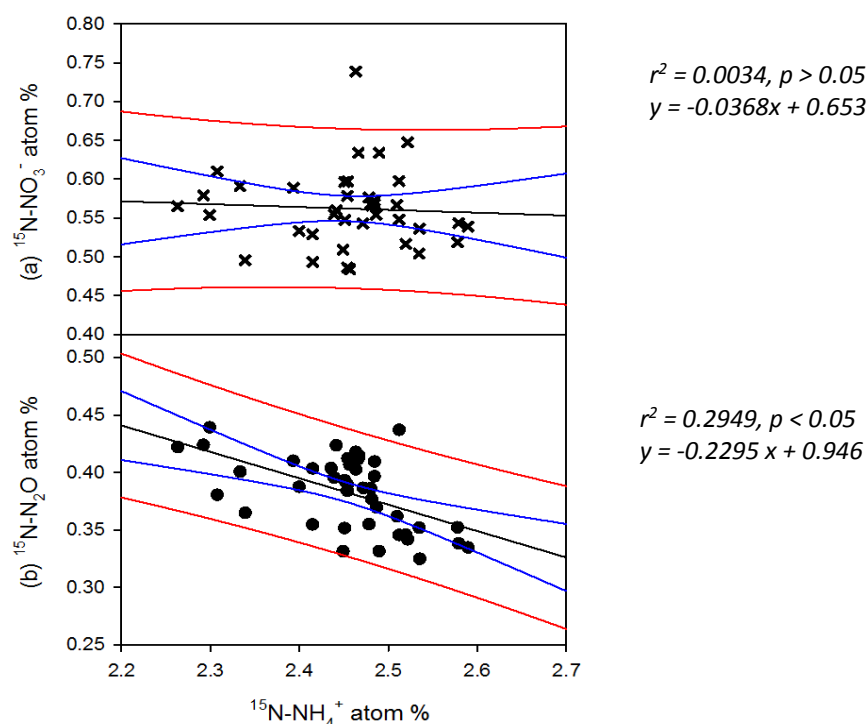


Figure 5-22 The drain water  $^{15}\text{N}\text{-NH}_4^+$  atom % versus  $^{15}\text{N}\text{-NO}_3^-$  atom % (a) and  $^{15}\text{N}\text{-N}_2\text{O}$  atom % (b).

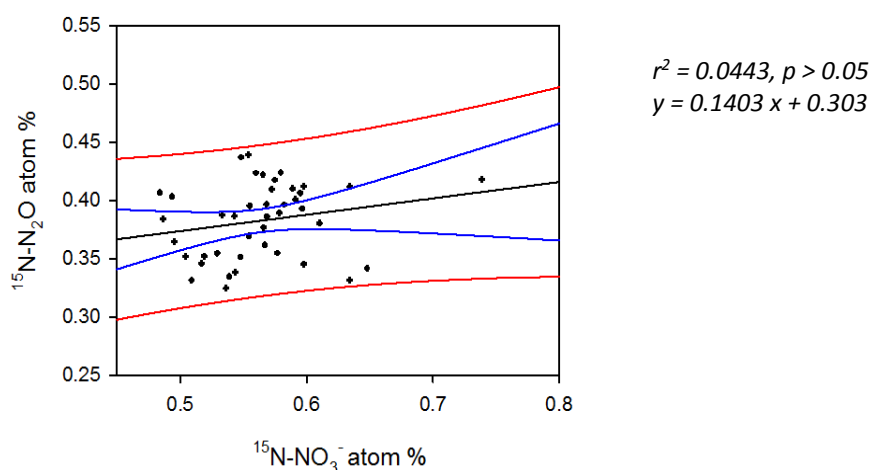
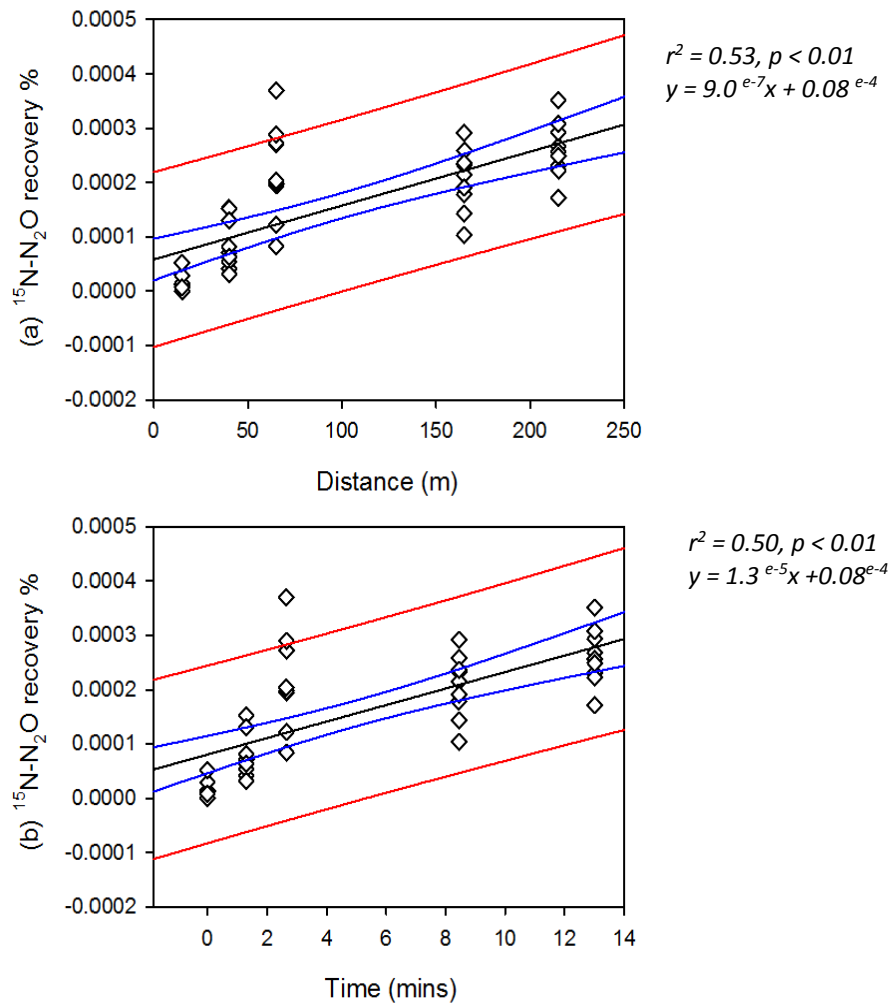


Figure 5-23 The drain water  $^{15}\text{N}\text{-NO}_3^-$  atom % versus  $^{15}\text{N}\text{-N}_2\text{O}$  atom %.

The  $\text{NO}_3^-$  atom % showed no relationship with  $\text{N}_2\text{O}$  atom % ( $r^2 = 4\%$ ;  $p > 0.05$ ).

### 5.3.19 $^{15}\text{N}\text{-N}_2\text{O}$ recovery

When compared to  $^{15}\text{N}\text{-NH}_4^+$  and  $^{15}\text{N}\text{-NO}_3^-$  recoveries,  $^{15}\text{N}\text{-N}_2\text{O}$  recovery was significantly lower, but increased over distance and time.



**Figure 5-24** Drain water  $^{15}\text{N}\text{-N}_2\text{O}$  recovery versus distance (a) and time (b). The best-fit regression lines are black, the 95% confidence intervals are between blue lines and the predicted intervals are between red lines. Each data point denotes a single sample measurement ( $n = 39$ ).

### 5.3.20 Relationships of $^{15}\text{N}$ recoveries between $^{15}\text{N-NH}_4^+$ & $^{15}\text{N-NO}_3^-$ and $^{15}\text{N-N}_2\text{O}$

The drain water  $^{15}\text{N-NH}_4^+$  recovery showed a weak and negative relationship with  $^{15}\text{N-NO}_3^-$  recovery ( $r^2 = 8\%$ ). However, drain water  $^{15}\text{N-NH}_4^+$  recovery showed a strong and negative correlation with  $^{15}\text{N-N}_2\text{O}$  recovery ( $r^2 = 68\%$ ).

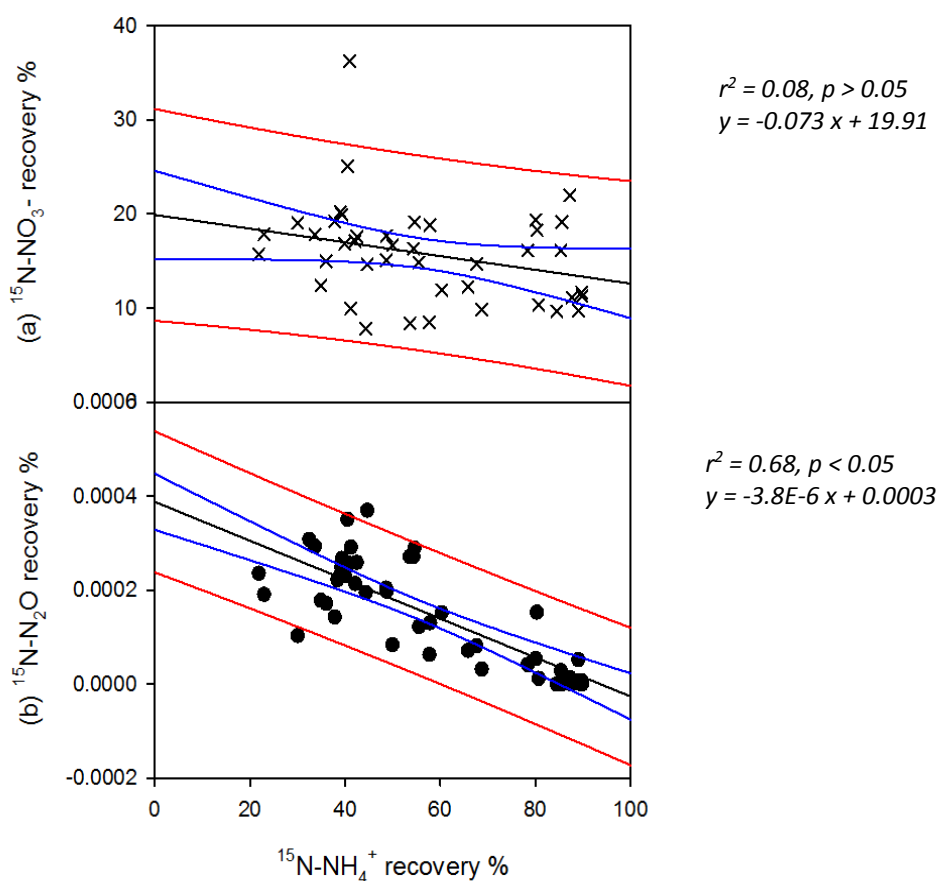
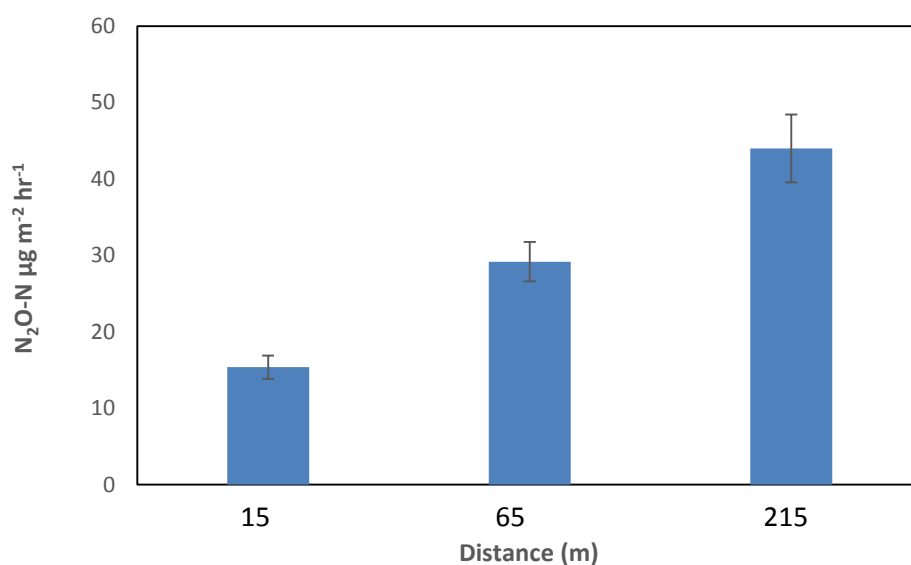


Figure 5-25 Interaction of the drain water  $^{15}\text{N-NH}_4^+$  recovery % with  $^{15}\text{N-NO}_3^-$  (a) and  $^{15}\text{N-N}_2\text{O}$  recovery % (b); (n=39).

### 5.3.21 Surface $\text{N}_2\text{O}$ and $^{15}\text{N-N}_2\text{O}$ flux measurements

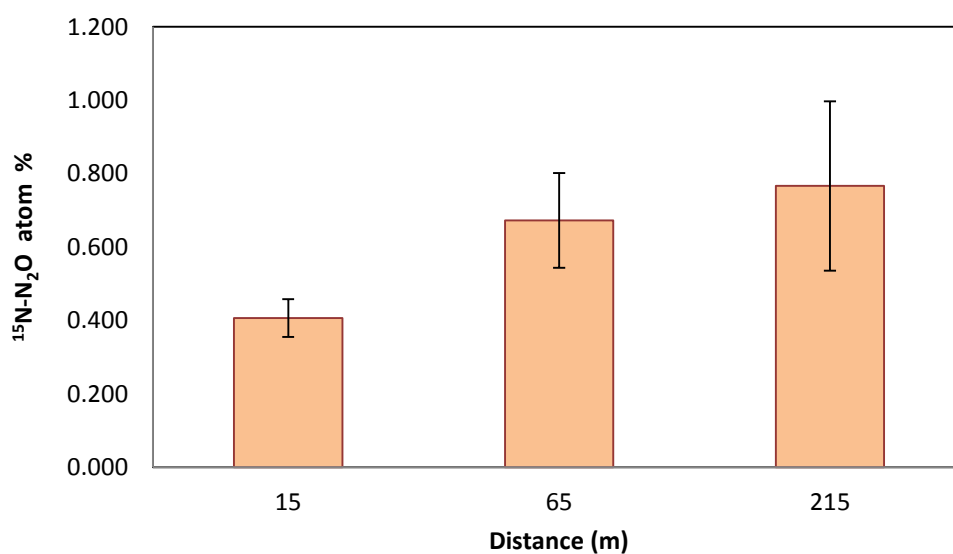
The surface gas samples were collected to measure  $\text{N}_2\text{O}$  and  $^{15}\text{N-N}_2\text{O}$  from floating chambers at site 1 (15 m), site 3 (65 m) and site 5 (215 m). The cumulative  $\text{N}_2\text{O}$  fluxes increased with distance reaching  $15.37 \pm 1.53$  ( $\pm$  stdev)  $\text{N}_2\text{O-N mg m}^{-2} \text{ h}^{-1}$  at site 1 to  $43.99 \pm 4.44$   $\text{N}_2\text{O-N mg m}^{-2} \text{ h}^{-1}$  at site 5 (Figure 5-26).



**Figure 5-26** Hourly average N<sub>2</sub>O flux at three sample sites (15 m, 65 m and 215 m; n = 3, error bars = ± stdev).

### 5.3.22 <sup>15</sup>N-N<sub>2</sub>O atom% from floating chambers

Following the N<sub>2</sub>O flux trend, the average <sup>15</sup>N-N<sub>2</sub>O atom percentage also increased with tracer travel distance (Figure 5-27). The average <sup>15</sup>N-N<sub>2</sub>O enrichment at site 1 was 0.41 ± 0.02 atom percentage. However, at site 3 and site 5, <sup>15</sup>N-N<sub>2</sub>O enrichment increased to 0.67 ± 0.12 and 0.77 ± 0.23 (± stdev) respectively.



**Figure 5-27** Average <sup>15</sup>N-N<sub>2</sub>O atom percentage at three sample sites (15 m, 65 m and 215 m; n = 3, error bars = ± stdev).

### 5.3.23 $^{15}\text{N}$ - $\text{N}_2\text{O}$ recovery from floating chambers

The average  $^{15}\text{N}$  recovery as  $\text{N}_2\text{O}$  also increased with tracer travel distance (Figure 5-28). The average  $^{15}\text{N}$  recovered as  $\text{N}_2\text{O}$  at site 1 was  $2.6\text{e-}5 \pm 2.0\text{E-}5 \%$  and this increased to  $2.6\text{E-}4 \pm 2.9\text{E-}5\%$  at site 5.

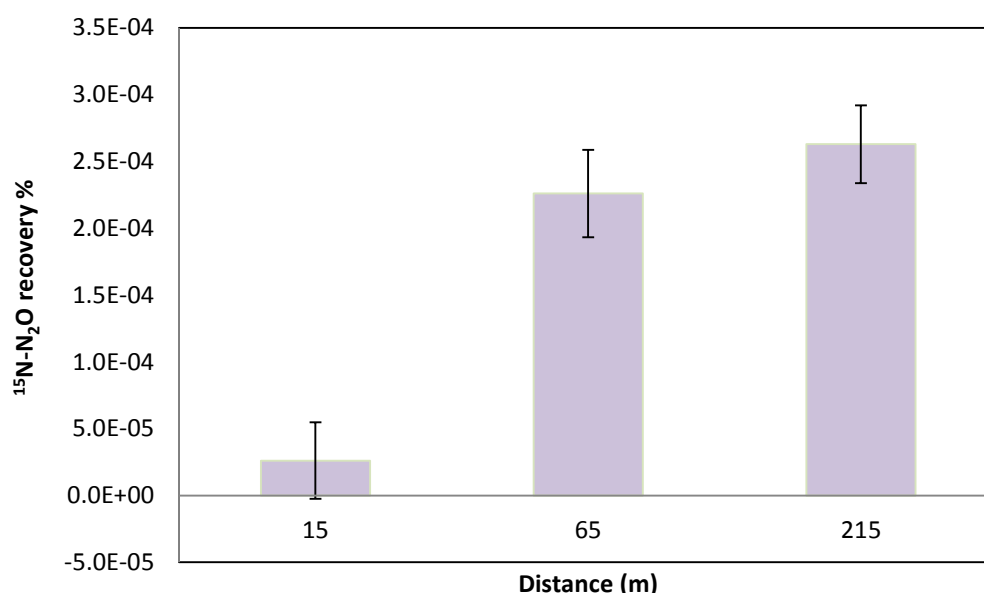
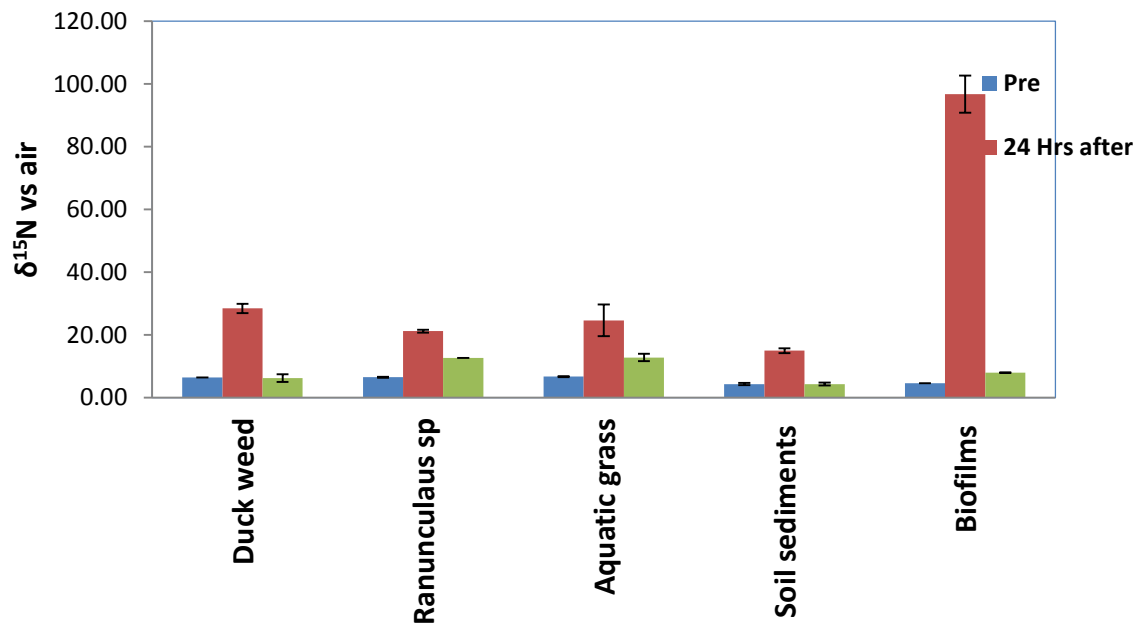


Figure 5-28 Average  $^{15}\text{N}$  recovery as  $\text{N}_2\text{O}$  at three sample sites (15 m, 65 m and 215 m;  $n = 3$ , error bars =  $\pm$  stdev).

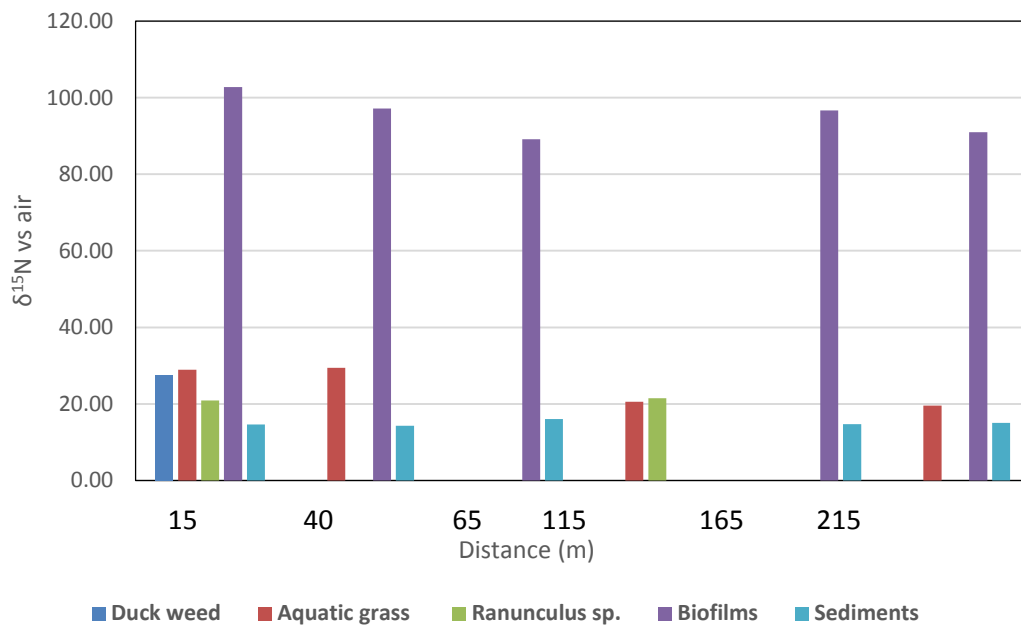
### 5.3.24 Nitrogen uptake by river components

The  $^{15}\text{N}$  enrichment of the drain water aquatic plants (*Ranunculus sp.*, Aquatic grass – *Carex sp.* and Duckweed – *Lemnoideae sp.*), soil sediments and biofilms of the planted tiles were measured before the tracer solution addition, 24 hours after  $^{15}\text{N}$  tracer addition and 10 days later. The pre tracer  $\delta^{15}\text{N}$  of aquatic plants, soil sediments and biofilms were  $6.53 \pm 1.5$ ,  $4.31 \pm 0.50$  and  $4.58 \pm 0.81\text{‰}$   $\text{N}_2$  air respectively. Twenty-four hours after  $^{15}\text{N}$  tracer addition, the same components were enriched in  $^{15}\text{N}$  with biofilms having the highest  $^{15}\text{N}$  enrichment ( $\delta^{15}\text{N}$   $96.81 \pm 8.00\text{‰}$ ). Ten days later,  $\delta^{15}\text{N}$  had declined in all components to values comparable to those pre-trial, but the  $\delta^{15}\text{N}$  of *Ranunculus sp.*, Aquatic grass and biofilms were still elevated  $12.7 \pm 0.05\text{‰}$ ,  $12.8 \pm 1.2\text{‰}$  and  $7.95 \pm 0.08\text{‰}$  respectively (Figure 5-29).



**Figure 5-29** Temporal changes in  $\delta^{15}\text{N}$  vs air (prior to tracer solution addition, 24 hrs after and 10 days later) in drain components (Biofilms  $n = 5$ , soil sediments  $n = 5$ , Duckweed  $n = 5$ , Aquatic grass  $n = 4$  and *Ranunculus sp*,  $n = 2$ ; Error bars =  $\pm$  stdev).

The  $^{15}\text{N}$  enrichment of the biotic drain water components were plotted over distance were plotted (Figure 5-30) but no spatial variances between sample sites occurred ( $p > 0.05$ ).



**Figure 5-30** Spatial variances of  $\delta^{15}\text{N}$  vs. air in drain components 24 hrs after tracer solution injection ( $n = 1$ ).

## Chapter 6

### Drain water N dynamics and EF5-r measurements

The  $^{15}\text{N}$  tracer addition study (Chapter 5) has provided new information on the fate of drain water  $\text{NH}_4^+\text{-N}$  and the effect of  $\text{NH}_4^+\text{-N}$  on drain  $\text{N}_2\text{O-N}$  and  $\text{NO}_3^-\text{-N}$ . Variations in dissolved  $\text{N}_2\text{O}$  saturation between sampling sites may indeed be due to drain hydro physical variations and associated water chemistry. While chamber flux measurements (Figure 5-26) showed  $\text{N}_2\text{O}$  fluxes gradually increased with distance and time, it is difficult to prescribe the exact mechanism or mechanisms for the  $\text{N}_2\text{O}$  dynamics over time or distance. Even though, denitrification has been considered as a major river  $\text{N}_2\text{O}$  production process, the data also conclusively demonstrates nitrification occurring. Therefore,  $\text{NH}_4^+\text{-N}$  cannot be ruled out as a contributing source for dissolved  $\text{N}_2\text{O}$ .

#### 6.1 $\text{NH}_4^+\text{-N}$ versus $\text{NO}_3^-\text{-N}$ as a source of $\text{N}_2\text{O}$

Following the tracer solution addition, the drain water  $\text{NH}_4^+\text{-N}$  concentrations declined more rapidly than the rate of  $\text{NO}_3^-\text{-N}$  production over distance and time (Figure 5-7). The drain  $\text{NH}_4^+\text{-N}$  concentration averaged  $1.36 \text{ mg L}^{-1}$  at sample site 1 and had reduced to  $0.54 \text{ mg L}^{-1}$  at site 5. The total  $\text{NH}_4^+\text{-N}$  loss which was estimated by concentration difference between sampling sites 1 and 5, was  $0.82 \text{ mg L}^{-1}$ . The drain water  $\text{NO}_3^-\text{-N}$  concentration was  $2.78 \text{ mg L}^{-1}$  before the tracer addition, and increased to  $3.03 \text{ mg L}^{-1}$  after addition (Figure 5-12, a & b), and only increased by an averaged  $0.25 \text{ mg L}^{-1}$ . The half-life of  $\text{NH}_4^+\text{-N}$  concentration (8.62 minutes) was shorter than doubling life of  $\text{NO}_3^-\text{-N}$  concentrations (12.63 minutes). Assuming the increase in  $\text{NO}_3^-\text{-N}$  was all derived from the  $\text{NH}_4^+\text{-N}$  injected, it accounts for 30.5% of the  $\text{NH}_4^+\text{-N}$  lost, while 26.4% of the  $^{15}\text{N-NH}_4^+$  was recovered as  $\text{NO}_3^-$  (Figure 5-17).

Ammonium  $^{15}\text{N}$  enrichment (atom %) did not change over distance or time (Figure 5-9) indicating  $\text{NH}_4^+\text{-N}$  inputs, other than the injected tracer, were not significant. Potentially, the increased  $\text{N}_2\text{O}$  flux could have been the result of demonstrated  $\text{NH}_4^+\text{-N}$  nitrification or the result of  $\text{NO}_3^-\text{-N}$  denitrification. However, the  $\text{N}_2\text{O-N}$  atom %,  $^{15}\text{N}$  enrichment increased over distance and time (Figure 5-21) indicating a  $^{15}\text{N}$  source was the substrate for  $\text{N}_2\text{O}$  production.

There was no relationship between the  $\text{NO}_3^-\text{-N}$  atom %  $^{15}\text{N}$  enrichment and the  $^{15}\text{N}$  enrichment of the  $\text{N}_2\text{O}$  evolved (Figure 5-23). However, there was a good relationship between  $\text{NH}_4^+\text{-N}$  atom %  $^{15}\text{N}$  enrichment and the  $^{15}\text{N}$  enrichment of the  $\text{N}_2\text{O}$  evolved (Figure 5-22, b) where  $\text{NH}_4^+\text{-N}$  atom %



declined as  $\text{N}_2\text{O}$ -N atom % increased. The  $^{15}\text{N}$  enrichment of the  $\text{N}_2\text{O}$ -N was not equal to the  $^{15}\text{N}$ - $\text{NH}_4^+$  enrichment indicating other natural abundance sources were also contributing to the drain  $\text{N}_2\text{O}$ -N flux. These could indicate antecedent  $\text{N}_2\text{O}$ , the less enriched  $\text{NO}_3^-$ -N pool, or nitrification of  $\text{NH}_4^+$ -N being released as a result of mineralization.

Following  $^{15}\text{N}$  tracer solution addition, biofilms, plants and soil sediments were highly enriched with  $^{15}\text{N}$  tracer. The latter, this study was identified, as contributing to organic N turnover were, for example, biofilms and aquatic plants. The greater disappearance rate of  $\text{NH}_4^+$ -N in drain water thus also resulted from a high biological demand. However, not only added  $\text{NH}_4^+$ -N, but dissolved  $\text{NO}_3^-$ -N also present in the drain. Mulholland et al., 2004 stated that uptake of  $\text{NH}_4^+$ -N in river environments is favoured due to lower energy requirements for plant and biota assimilation. As a result,  $\text{NH}_4^+$ -N loss rates could be accounted for due to assimilation. Ten days after the tracer solution addition,  $^{15}\text{N}$  enrichments of the drain biological components significantly reduced (Figure 5-29). Supporting of N mineralization was dominant in well oxygenated water, and benthic denitrification of  $\text{NO}_3^-$ -N would not be expected to be a dominant source of  $\text{N}_2\text{O}$ . However, potentially water sediment denitrification could have been greater for drain *in-situ*  $\text{N}_2\text{O}$  flux.

## 6.2 $\text{N}_2\text{O}$ -N flux estimations

In order to estimate the EF5-r, experiment #2 measured  $k_{\text{N}_2\text{O}}$  values and the equilibrated dissolved  $\text{N}_2\text{O}$  concentrations in drain were substituted into equation 2.4 and the emitted  $\text{N}_2\text{O}$ -N fluxes were calculated. The estimated drain water  $\text{N}_2\text{O}$ -N saturation averaged  $0.31 \mu\text{g N}_2\text{O-N L}^{-1}$ ;  $12.1 \text{ nmol L}^{-1}$ . Following  $^{15}\text{N}$  tracer addition, the drain water dissolved  $\text{N}_2\text{O}$ -N concentration averaged  $0.42 \mu\text{g N}_2\text{O-N L}^{-1}$ ;  $14.6 \text{ nmol L}^{-1}$ , where the net increase was  $0.11 \mu\text{g N}_2\text{O-N L}^{-1}$ ;  $2.5 \text{ nmol L}^{-1}$ . Therefore, the increase in the equilibrium  $\text{N}_2\text{O}$ -N concentration ( $\text{dC N}_2\text{O-N}$ ) was  $110 \mu\text{g m}^{-3}$ . Using this dissolved  $\text{N}_2\text{O}$ -N concentration and the  $k_{\text{N}_2\text{O}}$  derived from four previously described methods (Sections 3.3.6 and 3.3.7), the  $\text{N}_2\text{O}$ -N flux was determined (Table 6.1).

**Table 6.1 Nitrous oxide (N<sub>2</sub>O-N) flux estimations from the measured  $k_{N_2O}$  using different methods**

Methods	$k_{N_2O}$ (m day <sup>-1</sup> )	dC N <sub>2</sub> O-N (µg L <sup>-1</sup> )	dC N <sub>2</sub> O-N (µg m <sup>-3</sup> )	Flux N <sub>2</sub> O-N (µg m <sup>-2</sup> day <sup>-1</sup> )
1. Headspace equilibrium	7.49	0.11	110	824
2. Floating chambers	6.98			769
3. Wilcock (1982) model; equation 2.10	8.65			952
4. Surface Flux (direct N <sub>2</sub> O flux measurements)	6.06			667

From the data in Table 6.1, it can be seen that the N<sub>2</sub>O-N flux ranged between 667 and 952 µg m<sup>-2</sup> day<sup>-1</sup>, depending on methods used.

### 6.3 EF5-r estimations

The current IPCC default emission factor EF5-r has a value of 0.0025 kg N<sub>2</sub>O-N/ kg N leached. The IPCC methodology assumes nitrification rates exceed denitrification rates by two fold in rivers. Beaulieu et al., (2008) doubted N<sub>2</sub>O emissions could exceed 12 mg N<sub>2</sub>O-N m<sup>-2</sup> day<sup>-1</sup>. Clough and Kelliher (2012) measured N<sub>2</sub>O-N fluxes from the Waikato River that were < 120 µg m<sup>-2</sup> h<sup>-1</sup> (< 2880 µg m<sup>-2</sup> day<sup>-1</sup>). According to the Waikato River 10 year median values for NO<sub>3</sub><sup>-</sup> concentrations and flow rates, a calculated EF5-r value equated to 0.0005 kg (0.5 g) N<sub>2</sub>O-N: kg N leached. Clough and Kelliher (2006, 2007 and 2011) estimated N<sub>2</sub>O-N fluxes between 16 to 501 µg m<sup>-2</sup> h<sup>-1</sup> (384 to 12024 µg m<sup>-2</sup> day<sup>-1</sup>) that were based on the LII stream and low land spring fed streams and a braided river (Ashburton River) in the South Island, New Zealand. According to these studies and the study of Dong et al., (2004) is carried out in rivers of Wales and England, EF5-r for rivers has been estimated between 0.0003 and 0.0005 kg (0.3 and 0.5 g) N<sub>2</sub>O-N/ kg N leached.

In order to measure the EF5-r in the current study, the following three methods were used.

1. The estimated N<sub>2</sub>O-N fluxes in Table 6.1 are presented as a fraction of the drain NO<sub>3</sub><sup>-</sup>-N flux.
2. The measured N<sub>2</sub>O-N flux using chambers at sampling sites 1, 3 and 5 are expressed as a fraction of the NO<sub>3</sub><sup>-</sup>-N flux.
3. The current IPCC, EF5-r default value (0.0025 kg N<sub>2</sub>O-N: NO<sub>3</sub><sup>-</sup>-N kg) is used to measure the N<sub>2</sub>O-N flux as a fraction of the NO<sub>3</sub><sup>-</sup>-N flux.

### 6.3.1 EF5-r measurements using the estimated N<sub>2</sub>O-N fluxes and NO<sub>3</sub><sup>-</sup>-N flux

The measured flux (Table 6.1) using four different methods: the EF5-r is calculated as ratios of N<sub>2</sub>O-N kg per NO<sub>3</sub><sup>-</sup>-N kg of N (Table 6.2).

**Table 6.2** EF5-r estimations from the calculated N<sub>2</sub>O-N flux using different  $k_{N_2O}$

Methods	Flux N <sub>2</sub> O-N ( $\mu\text{g m}^{-2} \text{ day}^{-1}$ )	N <sub>2</sub> O-N from 314.4 ( $\text{m}^2 \text{ mg day}^{-1}$ )	NO <sub>3</sub> <sup>-</sup> -N ( $\text{kg day}^{-1}$ )	EF5-r  (N <sub>2</sub> O-N kg: NO <sub>3</sub> <sup>-</sup> -N kg)
1. Headspace equilibrium	824	259	31.6	8.21E-6 (8.2 mg/kg)
2. Floating chambers	769	242		7.66E-6 (7.66 mg/Kg)
3. Wilcock (1982) model	952	299		9.48E-6 (9.48 mg/Kg)
4. Surface N <sub>2</sub> O flux	667	210		6.64E-6 (6.64 mg/Kg)

The calculated EF5-r ( $\text{N}_2\text{O-N kg} / \text{NO}_3^- \text{-N Kg}$ ) ranged between  $6.64\text{E-}6$  ( $6.64 \text{ mg kg}^{-1}$ ) to  $9.48\text{E-}6$  ( $9.48 \text{ mg kg}^{-1}$ ) which is significantly less than the IPCC predicted EF5-r value of  $0.025 \text{ N}_2\text{O-N kg: NO}_3^- \text{-N Kg}$ . It is also smaller than the Dong et al., (2004) and Clough et al., (2012) EF5-r estimations of  $0.0003 \text{ N}_2\text{O-N kg}$  ( $0.3 \text{ g}$ ) and  $0.0005 \text{ N}_2\text{O-N kg}$  ( $0.5 \text{ g}$ ):  $\text{NO}_3^- \text{-N Kg}$ , respectively. The Wilcock (1982) model produced higher EF5-r than all the other three methods due to a high  $k_{\text{N}_2\text{O}}$  value. In contrast, the lowest EF5-r was estimated using the direct  $\text{N}_2\text{O}$  fluxes from floating chambers.

### 6.3.2 EF5-r measurements from $\text{N}_2\text{O-N}$ flux and dissolved $\text{NO}_3^- \text{-N}$

In experiment 2, the deployed chambers at sites 1, 3 and 5 directly measured the  $\text{N}_2\text{O-N}$  flux. The amount of  $\text{NO}_3^- \text{-N}$  flowing through each site was estimated using the  $\text{NO}_3^- \text{-N}$  concentration, drain water velocity and discharge rate ( $2.80 - 2.96 \text{ mg L}^{-1} * 126.7 \text{ L s}^{-1} * 3600 \text{ s hr}^{-1}$ ). Following the IPCC method, the EF5-r is calculated using the ratios of emitted  $\text{N}_2\text{O-N kg hr}^{-1}$  to  $\text{NO}_3^- \text{-N kg hr}^{-1}$  flux (Table 6.3)

**Table 6.3 EF5-r estimations from the chamber  $\text{N}_2\text{O-N}$  flux measurements at sites 1, 3 and 5.**

Site	$\text{N}_2\text{O-N}$ ( $\mu\text{g m}^{-2} \text{ hr}^{-1}$ )	Area ( $\text{m}^2$ )	$\text{N}_2\text{O-N}$ ( $\mu\text{g hr}^{-1}$ )	$\text{NO}_3^- \text{-N}$ ( $\text{kg hr}^{-1}$ )	EF5-r ( $\text{N}_2\text{O-N kg hr}^{-1} / \text{NO}_3^- \text{-N kg hr}^{-1}$ )
1	15.37	1.43	21.98	1.28	$1.72\text{E-}11$ ( $0.00002 \text{ mg/kg}$ )
3	29.18	1.64	47.85	1.32	$3.62\text{E-}11$ ( $0.00004 \text{ mg/kg}$ )
5	43.99	1.98	87.10	1.35	$6.43\text{E-}11$ ( $0.00006 \text{ mg/kg}$ )

The chamber estimated EF5-r values (Table 6.3) were significantly lower than those derived using  $k_{\text{N}_2\text{O}}$  (Table 6.2). The reason for lower EF5-r values could be, uneven water flow occurs in the drain due to bed friction which may have lowered the actual  $\text{NO}_3^- \text{-N}$  flow beneath the chambers than estimated. Similarly, deploying many chambers at a single sample site may have broken the drain water flow, causing release of  $\text{N}_2\text{O-N}$  to air before accumulating within chamber headspace. As a result the measured surface  $\text{N}_2\text{O}$  flux may have been underestimated.

### 6.3.3 Comparison of total N<sub>2</sub>O-N flux from EF5-r values

The drain water average NO<sub>3</sub><sup>-</sup>-N concentration was 2.883 mg L<sup>-1</sup> and the drain discharge rate was 126.7 L s<sup>-1</sup>. If the drain continuously discharges at the same rate with the same NO<sub>3</sub><sup>-</sup>-N concentration throughout a year, the annual total NO<sub>3</sub><sup>-</sup>-N mass would be 11519 kg (2.883 mg L<sup>-1</sup> \* 126.7 \* 3600 s hr<sup>-1</sup> \* 24 hrs day<sup>-1</sup> \* 365 days yr<sup>-1</sup>). Then, using the calculated EF5-r values and the IPCC EF5-r default value, the possible annual total N<sub>2</sub>O-N emissions from Rainey's Road drain were estimated. The possible annual N<sub>2</sub>O-N emissions from four different  $k_{N_2O}$  calculated EF5-r values (Table 6.2) ranged between 7.65E-2 and 9.46E-2 kg N<sub>2</sub>O-N yr<sup>-1</sup>: NO<sub>3</sub><sup>-</sup>-N kg yr<sup>-1</sup>. However, EF5-r derived from chamber N<sub>2</sub>O-N flux measurement (Table 6.3) was 4.5E-4 kg N<sub>2</sub>O-N yr<sup>-1</sup>: NO<sub>3</sub><sup>-</sup>-N kg yr<sup>-1</sup>. Using the current IPCC EF5-r default value, the annual loss of N<sub>2</sub>O-N was 28.8 kg N<sub>2</sub>O-N yr<sup>-1</sup>: NO<sub>3</sub><sup>-</sup>-N kg yr<sup>-1</sup> (0.0025 kg N<sub>2</sub>O-N \* 11519 kg NO<sub>3</sub><sup>-</sup>-N).

## 6.4 Summary and suggestions for future research

According to the above analysis, the IPCC suggested EF5-r default value significantly overestimates the N<sub>2</sub>O emissions from rivers and drainages. The EF5-r estimates using measured  $k_{N_2O}$  values were in general agreement. The  $k_{N_2O}$  derived from the Wilcock (1982) model and the dissolved N<sub>2</sub>O concentrations produced higher EF5-r values due to the measured higher value of  $k_{N_2O}$ . In contrast, the chamber methodology underestimated the N<sub>2</sub>O flux to NO<sub>3</sub><sup>-</sup>-N ratio and consequently produced lower EF5-r values and appears to be an inadequate for gas flux measurements on flowing water surfaces. However, it should be noted, the chamber data were collected from a single sample collection time at the end of experiment. Therefore, N<sub>2</sub>O flux measurements should be repeated using chambers.

The method used and detailed involving N isotope additions, have to be repeated to validate the measurements of dissolved N<sub>2</sub>O-N, N<sub>2</sub>O fluxes and NO<sub>3</sub><sup>-</sup>-N concentrations in drains. After the <sup>15</sup>N tracer addition, the increased <sup>15</sup>N enrichment within biotic components reduced to background levels, demonstrated mineralization occurred. More <sup>15</sup>N studies are required using both NH<sub>4</sub><sup>+</sup>-N and NO<sub>3</sub><sup>-</sup>-N moieties separately, under the same experimental conditions to verify the relative effect of nitrification and denitrification on drain N<sub>2</sub>O flux.

## Appendix A

### Abbreviations

A	Area
ANOVA	Analysis of variances
Br <sup>-</sup>	Bromide ions
CO <sub>2</sub>	Carbon dioxide
CH <sub>4</sub>	Methane
C <sub>3</sub> H <sub>8</sub>	Propane
CHCl <sub>3</sub>	Tri-Chloro methane
dC	Concentration difference
dt	Temperature difference
EF5	Emission factor for indirect nitrous oxide emissions
EF5-g	Nitrous oxide emission factor for ground water and surface drainage
EF5-r	Nitrous oxide emission factor for rivers and flowing waters
EF5-e	Nitrous oxide emission factor for estuaries
F	Gas flux
FRACLEACH	Fraction of nitrogen leached
GHG	Greenhouse gas
h	water depth
hr	hour
KBr	Potassium bromide
$k'$	Gas transfer coefficient
$k$	gas transfer velocity
K	Temperature in Kelvin
$k_H$	Henry's coefficient
KHSO <sub>4</sub>	Potassium bisulphate
MgO	Magnesium oxide
N <sub>2</sub>	Di nitrogen
N <sub>2</sub> O	Nitrous oxide
NH <sub>4</sub> <sup>+</sup>	Ammonium ions
NO <sub>3</sub> <sup>-</sup>	Nitrate ions
NO <sub>2</sub> <sup>-</sup>	Nitrite ions
NH <sub>3</sub>	Ammonia (gas)

$^{15}\text{N}$	$^{15}\text{N}$ labelled nitrogen
$(\text{NH}_4)_2\text{SO}_4$	Ammonium sulphate
NLEACH	Nitrogen leaching and runoff
NFERT	Nitrogen input as fertilizer
NEX	Amount of nitrogen leached as excreta
n	number of moles
$\text{O}_2$	Oxygen
P	Pressure
Q	Water discharge rate
R	Universal gas constant
RR	Tracer solution release rate
Sc	Schmidt number
T	Temperature
t	time
U	water velocity
V	Volume
$X_{(\text{aq})}$	Dissolved gas concentration in a aqueous phase
$X_{(\text{g})}$	Equilibrium gas concentration in gas phase
$\eta^2$	Sum of squares between groups divided by the total sum of squares

## Appendix B

### Equations

$k'_{N_2O}$	=	$k'_{Tracer\ gas} * (SC_{N_2O} / SC_{Tracer\ gas})^{-n}$	2.1
$F_{N_2O}$	=	$h * k'_{N_2O} (X_{aq} - X_g)$	2.2
$k_{N_2O}$	=	$h * k'_{N_2O}$	2.3
$F_{N_2O}$	=	$k_{N_2O} * (X_{aq} - X_g)$	2.4
$k_{N_2O}$	=	$F_{N_2O} / (X_{aq} - X_g)$	2.5
$K_H$	=	$P_{X(g)} / X_{(aq)}$	2.6
$X_{(aq)}$	=	$F_{(g)} / K_H$	2.7
$X_{(aq)}$	=	$F / k$	2.8
$k_{water}$	=	$(D * U / h)^{0.5}$	2.9
$k$	=	$k_{(20)} * [1.0241]^{T-20} * 3.74 * [U^{0.5} / h^{1.5}]$	2.10
$NLEACH$	=	$[NFERT + NEX] * FRACLEACH$	2.11
$N_2O\ (L)$	=	$NLEACH * EF5$	2.12
$Q$	=	$Solution\ [Br^-] \times RR / Site\ [Br^-]$	3.1
$D$	=	$Q / U * W$	3.2
$M$	=	$Cg \times [V_g + (V_l \times \theta)]$	3.3
$n$	=	$PV / RT$	3.4
$dC / dt$	=	$k' (C_t - C_0)$	3.5
$C_t$	=	$C_0 - k' (t_1 - t_0)$	3.6
$\ln C_t / C_0$	=	$-k' (t_1 - t_0)$	3.7



$$Sc_{(C_3H_8)} = 1911.1 - 118.11 \cdot T + 3.4527 \cdot T^2 - 0.04132 \cdot T^3 \quad 3.8$$

$$Sc_{(N_2O)} = 2055.6 - 137.11 \cdot T + 4.3173 \cdot T^2 - 0.05435 \cdot T^3 \quad 3.9$$

$$k'_{N_2O} = (Sc_{N_2O} / Sc_{C_3H_8})^{-n} \cdot k'_{C_3H_8} \quad 3.10$$

$$k'_{2(N_2O)} = k'_{N_2O} (600 / Sc_{N_2O(T)})^{-n} \quad 3.11$$

$$F = (dC/dt) \cdot (V/A) \cdot (P/RT) \quad 3.12$$

$$k_{C_3H_8} = F_{C_3H_8} / (X_{aq} - X_g) \quad 3.13$$

$$k_{N_2O} = (Sc_{N_2O} / Sc_{C_3H_8})^{-n} \cdot k_{C_3H_8} \quad 3.14$$

$$k_{(N_2O)} = k_{N_2O} (600 / Sc_{N_2O(T)})^{-n} \quad 3.15$$

$$k_{N_2O} = (Sc_{N_2O} / Sc_{O_2})^{-n} \cdot k_{O_2} \quad 3.16$$

$$\text{Atom \% of } ^{15}N = [^{15}N / (^{15}N + ^{14}N)] \cdot 100 \quad 5.1$$

$$\delta^{15}N = [(^{15}N / ^{14}N \text{ sample}) / (^{15}N / ^{14}N \text{ air}) - 1] \cdot 1000 \quad 5.2$$

$$^{15}N \text{ recovered (\%)} = 100 \times \frac{p \times (c-b)}{f \times (a-b)} \quad 5.3$$

$$C_{(t)} = C_{(0)} e^{-kt} \quad 5.4$$

$$t^{1/2} = \ln(0.5) / -k \quad 5.5$$

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